

One-step synthesis of highly pure and well-crystallized vertically aligned carbon nanotubes

Emeline Charon, Mathieu Pinault, Martine Mayne-L'Hermite, Cécile Reynaud

▶ To cite this version:

Emeline Charon, Mathieu Pinault, Martine Mayne-L'Hermite, Cécile Reynaud. One-step synthesis of highly pure and well-crystallized vertically aligned carbon nanotubes. Carbon, 2020, 173, pp.758-768. 10.1016/j.carbon.2020.10.056 . cea-03002425

HAL Id: cea-03002425 https://cea.hal.science/cea-03002425

Submitted on 12 Nov 2020

HAL is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers. L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.

1 2	One-step synthesis of highly pure and well-crystallized vertically aligned carbon nanotubes
3	Emeline Charon [*] , Mathieu Pinault, Martine Mayne-L'Hermite, Cécile Reynaud
4	Université Paris-Saclay, CEA, CNRS, NIMBE, 91191 Gif sur Yvette Cedex, France
5	

^{*} Corresponding author. Tel: 33 1 69 08 53 05. E-mail: emeline.charon@cea.fr

6 Abstract (197 words)

7 The one-step aerosol-assisted catalytic chemical vapor deposition (CCVD) process, when 8 operated in a H₂-based carrier gas, is shown to be effective at an extremely low ferrocene 9 content (0.1wt.% in toluene), which enables to efficiently prepare forests of vertically aligned 10 multiwalled carbon nanotubes (VACNTs) with high purity and good crystalline level. The 11 resulting iron content in VACNT sample is only 0.5wt.% corresponding to a high catalytic yield 12 of 200 while the steady growth rate (20 µm/min) is maintained at a significant value. The iron 13 content in the sample is found proportional to the ferrocene concentration in the precursor, and 14 when it decreases, a noticeable reduction in the iron encapsulation frequency in the nanotube 15 channel is plainly observed. Lowering the ferrocene concentration generates a reduction in the 16 VACNT number density while the growth rate increases and CNT diameters and crystalline 17 structure remain similar. Such significant purity and crystalline levels involves a high oxidation 18 resistance of the VACNT forest. These results, together with the *in-situ* continuous growth 19 feature of the one-step aerosol assisted CCVD process, open up towards a new VACNT range 20 made of pure and well-crystallized multi-walled carbon nanotubes, which is of interest for 21 industrial production and commercial applications.

22

Keywords: vertically aligned carbon nanotubes; one-step catalytic chemical vapour deposition;
 iron content; purity; crystallinity; oxidation resistance.

26 1 Introduction

27 Vertically Aligned Carbon NanoTubes (VACNT) arrays have demonstrated outstanding 28 potentialities as a novel material to prepare nanostructured composite or multifunctional 29 materials. The carbon nanotube (CNT) alignment allows to take advantage of their anisotropic 30 properties. This is useful for many applications of high societal interest such as heat transfer [1], 31 energy storage [2,3], or high performance structural composites [4,5]. Efforts are currently 32 underway to develop efficient synthesis processes for the manufacture of VACNTs in order to 33 achieve mass production while reducing costs [6,7]. In particular, the process must be as simple 34 as possible and must be operated at atmospheric pressure. The most effective method for 35 synthesizing VACNT is catalytic chemical vapor deposition (CCVD) [8] which can be operated 36 at atmospheric pressure. However, it often involved several preliminary steps at low pressure to prepare the layer of catalytic nanoparticles from which the nanotubes will then grow. It is 37 38 why the aerosol-assisted version of the CCVD process has been developed [9-14], where 39 catalyst nanoparticles are produced in situ and continuously refreshed due to the simultaneous 40 injection of both metal and carbon precursors [15]. This process involves a base-growth 41 mechanism [16] enabling the continuous growth of VACNTs at steady growth rate over very 42 long synthesis duration, which allows VACNTs greater than 1mm to be achieved. Therefore, 43 aerosol-assisted CCVD is a versatile, cost-effective and scalable one-step process operated at 44 atmospheric pressure potentially applicable for a roll to roll production of multi-walled 45 VACNTs. The continuous supply of ferrocene, which is essential to sustain the growth through 46 the refreshment of the catalyst nanoparticles [16], induces the encapsulation of short nanowires 47 in the inner channel of the nanotubes [17,18]. As a consequence, the iron content of the pristine 48 VACNTs (Table 1) is typically around a few wt.% [15,19–21]. Such metallic by-products can 49 alter the intrinsic nanotube properties and be detrimental for several applications [22]. In 50 addition, it is also recognized that they can catalyze the oxidation of nanotubes and thus affect 51 their stability in air at moderate temperatures [23-25]. Therefore, these CNTs need to be 52 purified and several methods have been developed to remove metal by-products [22], either by 53 acid treatment [26], but their complete removal is difficult to achieve without altering the 54 nanotube structure [27,28], or by high temperature annealing which is the most effective 55 method for their removal while improving the nanotube crystallinity [22,29,30]. However, such 56 treatments complicate the CNT production process and are not always compatible with the 57 targeted application.

58 Therefore, efforts must be done directly on the aerosol-assisted CCVD production process in 59 order to reduce drastically the iron content in the pristine VACNTs. Recently and in the 60 meantime of our study, this issue was addressed by T. Kinoshita et al. [31] who reported a 61 modified floating catalyst CCVD method (similar to the aerosol-assisted one) enabling the 62 growth of CNT forests containing very low concentration of impurity (0.8 wt%). However, the 63 changes made to the process have turned it into a two-step process involving in the first step 64 the in-situ formation of the catalyst particles, then in the second step the CNT growth with carbon precursors only. Such experimental conditions do not allow the refreshment of the 65 66 catalyst particles so that the lifetime of their process is limited. Moreover the second step was 67 performed at low pressure which limits the industrial interest of the method.

68 In this context, the aim of our work is to reduce the Fe content of pristine VACNTs while 69 preserving their crystallinity, alignment and growth rate by increasing the catalytic yield of the 70 one-step aerosol-assisted CCVD process operated at atmospheric pressure. In the literature 71 (Table 1), few studies [15,19–21] report the measurement of iron content of VACNTs formed 72 by the one-step aerosol-assisted CCVD, but it is generally found that iron content increases 73 with ferrocene concentration in the precursor solution [19,21]. Cho et al. [20] studied the [0.2-74 9] wt.% ferrocene range at 760°C and obtained 1.9wt.% as the lowest iron content in CNT 75 samples for 1.5wt.% of ferrocene in toluene. However, they did not observe any growth of 76 VACNT forests at 0.2wt.% of ferrocene, in agreement with the result of Singh et al. [13]. 77 Similarly, Castro et al. [15] observed no growth of VACNT at 0.1 and 0.5wt.% when studying 78 the [0.1-5] wt.% range of ferrocene at 850°C and the lowest iron content obtained is 3wt.% at 79 2.5wt% ferrocene with a higher growth rate due to a higher synthesis temperature. To our 80 knowledge, for one-step aerosol-assisted CCVD process, the lowest concentration of ferrocene 81 responsible for the growth of VACNTs is 0.1wt.% [32] but the growth rate at 750°C is 82 particularly low (0.4 μ m/min) and the iron content in the resulting sample is not reported. The 83 highest growth rate obtained with a low ferrocene concentration (0.58wt.%) is 13.6 µm/min at 84 780°C [33] but the iron content is not indicated. The latter result was obtained with 15% H₂ 85 added to Ar as carrier gas.

- 86
- 87
- 88
- 89

91

92 Table 1 : Lowest ferrocene concentrations giving rise to VACNT growth reported in the 93 literature for the one-step aerosol-assisted CCVD synthesis. The most relevant 94 experimental parameters are reported, as well as, the growth rate and iron content of the 95 final product when available. Ferrocene concentrations in the precursor solution were 96 converted to wt.%. Note that 1wt.% of ferrocene in toluene corresponds to a Fe/C ratio 97 of 0.07at.%.

	Ferrocene concentration (wt.%)	Carbon source	Carrier gas	T (°C)	Substrate	Growth rate (µm/min)	Iron content (wt.%)	Raman ID/IG λ (nm)	
Bai 2005	0.58	vulono	Ar/H ₂	780	auartz	13.6		-	
[33]	1.14	xylelle	87/13	87/13	/ 00	quartz	20.4		-
	0.1	xylene	Ar	750	Sputtered Al Si wafer	0.4		0.49	
Ionescu								785 nm	
2011 [32]						17		0.68	
	1				water	4.7		785 nm	
Cho 2012	15	toluene	Δr	760	auartz	25	19	0.33*	
[20]	1.5 101	0]	toruene	IIC AI 700 0	quartz	2.5	1.7	633 nm	
McKee 2009 [19]	0.54	benzene	Ar	750	various	-	0.7 - 3	0.3 measured at 1.75 wt% Fe 514 nm	
Meysami 2013 [21]	1	toluene	Ar	800	quartz	16	2.5	0.29 532 nm	
Castro	ro 1.25	- toluene	Ar	850	quartz	11	3.5	0.52* 532 nm	
2010 [15]	2.5					20	3	0.33*	
								532 nm	
Castro	2.5	toluono	2.5 tolyana	Ar/H ₂	850	quartz	29	5.3	-
2013 [34]	2.3	toruene	80/20	800	quartz	23	6.2	-	

98 * Area ratio

99 Despite the wide disparity in the experimental conditions, the results of the literature highlight 100 the important role played by the synthesis temperature and the hydrogen presence in the carrier 101 gas to maintain a realistic growth rate while decreasing the ferrocene concentration in the 102 aerosol. In a previous paper [34], we studied the effect of adding hydrogen to Ar carrier gas and 103 showed that it has a major impact on the aerosol-assisted CCVD process. Increasing the 104 hydrogen content strongly shifts the CNT growth to the reactor inlet and reduces the CNT 105 diameters, while the CNT number density increases. Indeed, hydrogen demonstrably affects the

106 gas phase phenomena by lowering the decomposition temperature of ferrocene, promoting the 107 formation of a larger number of smaller iron nanoparticles in the gas phase and increasing the 108 nucleation site density of the catalytic nanoparticles. In addition, the optimal synthesis 109 temperature in terms of yield and homogeneity of growth is reduced to 800°C under hydrogen 110 (Table 1) [34]. In these previous experiments, the concentration of ferrocene in toluene was set 111 at 2.5wt.%, the optimal concentration determined at 850°C without H₂ [15]. It should be 112 reminded that without H₂, no growth of VACNTs is obtained below 1.25wt.% of ferrocene, neither at 850°C nor at 800°C. However, the situation may change in the presence of H₂ due to 113 114 the significant improvement in the ferrocene decomposition it induces. Therefore, our objective 115 is to determine, in the presence of H_2 , the lowest concentration of ferrocene in toluene allowing 116 the growth of a VACNT forest with low impurity level while maintaining a high growth rate 117 and a good structural quality.

118 In this paper, we investigate the role of ferrocene concentration in the precursor solution 119 (toluene/ferrocene) on the VACNT growth and characteristics (iron content, length, diameter, 120 density, structure, oxidation resistance as well as on growth efficiency (yields and growth rate). 121 As hydrogen was reported to be a determining chemical player in the decomposition rate of 122 ferrocene [34], all the synthesis of this study are performed by the one-step aerosol assisted 123 CCVD process with hydrogen diluted in argon as carrier gas. The approach combines global 124 analysis by Scanning Electron Microscopy (SEM), Thermogravimetric Analysis (TGA) and 125 Raman Spectrometry, with local analysis by Transmission Electron Microscopy (TEM). Since 126 in this one-step aerosol assisted CCVD process a continuous supply of ferrocene is essential to 127 sustain growth [35], our first objective is to determine the ferrocene concentration threshold 128 above which VACNT growth is maintained once the catalytic particles are formed. To this end, 129 we first carry out double injection experiments, by designing a specific set-up allowing to use 130 a solution containing 2.5wt.% ferrocene in a first short injection sequence to form the catalyst 131 particles, and then to use a second solution with a lower ferrocene concentration in a second 132 long injection sequence. These experiments demonstrate that a very low ferrocene 133 concentration (0.01wt.%) used in the second sequence can sustain the growth of VACNT forest, 134 which is considerably lower than the ones reported in the literature for this one-step aerosol 135 assisted CCVD process. Subsequently, by operating this process in a single injection mode with 136 a ferrocene concentration decreasing from 2.5 to 0.01wt.%, we show that it is possible to 137 determine conditions to synthesize a pristine VACNT carpet with unprecedented reported low 138 iron content (0.5 wt%) and high oxidation resistance.

139 2 Experimental

140 **2.1** Synthesis

141 The set-up (Fig. 1) and standard procedure used to synthesize VACNTs by the one-step aerosol-142 assisted CCVD process at atmospheric pressure are similar to those described by Castro et 143 al. [34]. Note that syntheses in the presence of H₂ cannot be done under the same conditions as 144 in its absence because the addition of H₂ considerably shifts the VACNT growth towards the 145 reactor inlet. The synthesis temperature must then be lowered to restore growth in the reactor 146 center. This is why all syntheses here are made in the presence of H₂ and at the optimal 147 temperature of 800°C [34]. The furnace exhibits an isothermal area larger than the previous 148 one. It is a 45 cm long tubular furnace equipped with a quartz reactor (16 mm inner diameter). 149 At 800°C, the isothermal area ($\pm 10^{\circ}$ C), is extended from 10 to 35 cm from the furnace inlet 150 (Fig. 1). A flat quartz substrate of 1.5×0.75 cm² is placed in the isothermal area at 14 cm from 151 the reactor inlet. The VACNTs grown on this substrate are analyzed together with the VACNTs 152 grown on the reactor walls. The VACNTs grown on the reactor walls are collected with a 153 stainless scraper, a procedure which keeps intact their morphology and structure. They are 154 weighed according to the location in the reactor, divided into 5 cm long sections with a surface 155 area of 25 cm² each, in order to assess the distribution of the VACNT deposit. All the 156 characterizations will be carried out on the VACNTs coming from the substrate of zone 2 and 157 the VACNT powder coming from zone 3. These zones were chosen because the yield is better 158 there. To perform double injection experiments, the present set-up is equipped with two liquid 159 precursor tanks. Solutions of ferrocene dissolved in toluene at different concentrations are 160 poured into these tanks connected to an injection system and an evaporator where they are 161 nebulized and carried to the reactor by a gas flow of 1 L/min at a rate about 0.8 g/min. The gas 162 flow is a mixture of Ar and 30 vol.% of H₂. A solution with 2.5wt.% of ferrocene is poured into 163 tank A (Fig. 1) while in tank B, the solution has variable concentrations. The solution in tank 164 A is injected for 1 min 40 s and then the solution in tank B for 13 min 20 s. The switch from 165 tank A to tank B is instantaneous, so that the process remains a one-step continuous process. In 166 single injection experiments, only the solution in tank B is injected for 15 min, with ferrocene 167 concentrations ranging from 0.01 to 2.5wt.%.



168

Fig. 1: Experimental set-up used for the one-step aerosol-assisted CCVD process operated
 at atmospheric pressure. Insert: temperature profile at 800°C measured with a

171 thermocouple moved along the quartz reactor.

172 **2.2 Characterizations**

Morphology and thickness of VACNT carpets grown on the substrate and on the walls in the center of the reactor are investigated by SEM (Carl Zeiss Ultra 55). CNT structure and statistical analysis of external and internal diameters are obtained from TEM (Philips CM12, 120 kV) after ultrasonic dispersion of CNTs in ethanol and deposition on standard TEM holder (copper grids). For high resolution TEM, we use a JEOL 2011 operating at 200 kV, equipped with a CCD camera (GATAN system ORIUS SC100, 4008×2672 pixels, pixel size: 0.014 nm).

179 TGA under air of products collected in the area in the center of the reactor is performed with a 180 92–16.18 SETARAM apparatus, at a temperature rate of 10°C/min in the 20-1000°C range, 181 which leads to the complete gasification of carbon. The rusty residue is used to determine the 182 iron content of the sample (weight percentage of iron in the collected products), as well as the 183 catalytic yield (ratio between the carbon and iron masses). This iron content is calculated 184 knowing that the residue consists of Fe₂O₃ as shown by X-ray diffraction [36]. In the unlikely 185 event that FeO contributes to the residue, the error would be small since the mass of iron in 186 Fe_2O_3 is 70%, while it is 78% in FeO. We will see in the following that this error would be 187 negligible given the magnitude of the variation in iron content in our experiments.

188 Raman spectra are acquired from the substrate samples in ambient conditions using a Renishaw

- 189 INVIA microspectrometer equipped with an Ar laser (514.5 nm wavelength), focused through
- 190 a Leica microscope. A very low incident power (2 mW) is used to avoid heating effects. Spectra

are recorded in the middle of the carpet cross-section in the 1000-3500 cm⁻¹ range. Pertinent quantitative Raman parameters are obtained by conventional fitting procedures [37] for the classical G, D, D' and 2D bands [38] and the corresponding position, full-width at half maximum (FWHM) and intensity (band height) relative to the G band are reported in Table S1 (Supplementary data).

196 **3 Results**

197 **3.1** Thickness and growth rate of the VACNT forests

Double injection experiments

199 Double injection syntheses are performed with a first injection sequence with 2.5wt.% ferrocene 200 in toluene during 1 min 40 s immediately followed by a long injection sequence of 13 min 20 s 201 with a ferrocene concentration varying between 0.01 and 1.5wt.%. In preliminary experiments, 202 we checked that the 1 min 40 s duration is long enough to initiate a VACNT carpet 203 representative of a VACNT growth with a ferrocene concentration of 2.5wt.% (See Fig. S1 in 204 supplementary data). SEM images of the products grown on quartz substrates placed in the 205 oven center (Fig. 2a) reveal VACNT forests of the same good quality as usually reported [34]. 206 The shortest carpet (170 µm) is obtained for 0.01wt.% of ferrocene in the second injection 207 sequence, but then, the thickness increases sharply to 330 µm for 0.05wt.% and up to 380 µm 208 for 0.1wt.%, after which it remains around 270 µm for higher concentrations. The 209 corresponding growth rate (Fig. 2b) exceeds 25 µm/min at 0.1wt.% of ferrocene and stabilizes 210 between 15 and 20 µm/min at higher concentrations.





Fig. 2: Double injection. (a): SEM images of the VACNT carpets grown on the central substrate (side-view) for increasing ferrocene concentration in the second long injection sequence. (b): mean carpet thickness and growth rate on the substrate (red dot) and on the reactor walls (blue triangle) as a function of ferrocene concentration. Dashed lines are added as eyes guide only. The thickness distribution was measured by SEM on the same samples with 20 measurement points for the CNTs on the walls of the reactor and 3 measurement points for the CNTs on the substrate.

- 219 The values on the substrate are slightly higher than those obtained on samples collected on the 220 reactor walls. (Fig. 2b). It is because the substrate is placed upstream along the reactor of the 221 zone where the samples used for the SEM analysis are collected and that, in aerosol-assisted 222 CCVD, the growth yield decreases along the reactor due to the dynamics of the catalytic 223 nanoparticles deposition as observed previously by us [15,34] and others [36]. This effect is 224 confirmed by the measurement of the mass distribution along the reactor displayed in Fig.S2. 225 As detailed in Supplementary Data, Fig.S2 shows that, whatever the ferrocene concentration, 226 the yield is optimal in zone 2 where the substrate is placed while the collected zone considered
- 227 in Fig.2 is zone 3 where the yield is slightly lower.
- The most striking result of these double injection experiments is that, in the presence of H_2 , a ferrocene concentration as low as 0.01wt.% in the second injection sequence is sufficient to sustain the growth, and a rate higher than 15 μ m/min is obtained for a concentration from
- 231 0.05wt.%.

232 Single injection experiments

233 Considering the very low ferrocene concentration (0.01 wt%) able to sustain the growth in 234 double injection synthesis, single injection synthesis with ferrocene concentration from 0.01 to 235 2.5wt.% are performed (Fig. 3a). For 0.01 and 0.05wt.% ferrocene, only a thin layer of entangled nanotubes is observed. However, as soon as the ferrocene concentration reaches 236 237 0.1wt.%, the growth of a well-defined VACNT forest becomes effective with a growth rate as 238 high as 20 µm/min, close to its maximum of 22 µm/min obtained with 0.25wt.% (Fig. 3b). For 239 higher concentrations, the growth rate decreases to values in the 10-15 µm/min range. The 240 trends are the same on the substrate located at the center of the furnace and on the reactor walls, 241 with still mean values slightly lower for samples collected on the walls, due to variation along 242 the reactor (Fig. S2). The VACNT carpet thickness increases linearly with the synthesis 243 duration in the tested duration range up to 420 min, with a growth rate of 11.4 µm/min at 244 1.25wt.% and 2.5wt.% ferrocene (Fig. S3 in supplementary data).



Fig. 3: Single injection. (a): SEM images of the VACNT carpets grown on the central substrate for increasing ferrocene concentration. (b): mean carpet thickness and growth rate on the central substrate (red dot) and on the reactor walls (blue triangle) as a function of ferrocene concentration. Dashed lines are added as eyes guide only. The thickness distribution was measured by SEM on the same samples with 20 measurement points for

251 the CNTs on the walls of the reactor and 3 measurement points for the CNTs on the 252 substrate.

Therefore for this one-step aerosol assisted CCVD process operated at 800°C with hydrogen in the gas phase, the ferrocene concentration threshold allowing an efficient growth of VACNTs is as low as 0.1wt.%, while no growth at all was observed without hydrogen at 850°C for ferrocene concentration equal to 0.1 or 0.5wt% [15]. More generally, the present results represent a great improvement as compared to the state of the art related to the one-step CCVD process (Table 1) in terms of growth rate at very low ferrocene concentration.

259 **3.2** Purity, diameter and structure of carbon nanotubes

The main characteristics of the VACNTs are similar regardless of the injection mode and depend only on the ferrocene concentration. Results obtained for the single injection mode will be discussed here and the ones regarding the double injection reported in Supplementary data.

263 Let's focus on single injection samples and compare SEM and TEM images of the formed 264 nanotubes with 0.1wt.% and 2.5wt.% of ferrocene respectively (Fig. 4). The striking difference 265 between both samples is in terms of cleanliness. At 0.1wt.%, the forest is very clean and no 266 parasitic particles can be observed outside the nanotubes at the resolutions used for the 267 observations. There are very few iron-based nanowires inside the nanotubes (Fig. 4a and 4c). 268 The number of embedded Fe nanoparticles has been drastically reduced as compared to our 269 previous results. Indeed, TEM micrographs on figure 4c) clearly indicate a high purity of CNT 270 at low ferrocene concentration. On the contrary, at 2.5wt.% numerous iron-based particles 271 exhibiting a nanowire shape are located inside the nanotubes (see also Fig. S4). In addition, a 272 considerable amount of nanoparticles are located on CNT surface (Fig. 4b and 4d), as observed 273 by others when the ferrocene concentration is high [19,21,33]. They are of varying sizes, some 274 of them being encapsulated into carbon shells and some others giving rise to the growth of 275 nanotubes of very small diameter which represent a low fraction of the sample mass and are not 276 considered in the diameter distributions reported below. Such iron nanoparticles located on the 277 CNT surface and the thin nanotubes observed on samples prepared with 2.5wt.% of ferrocene (Fig. 4d) cannot be detected in the sample obtained with 0.1wt.% of ferrocene (Fig. 4c). 278 279 Therefore, lowering the ferrocene concentration induces a drastically reduction of the iron 280 impurities inside the VACNT samples.

A detailed HRTEM analysis of a few individual nanotubes over their length (see Fig. S4) is used to characterize the iron-based nanowires found in the inner channel of the tubes. Their 283 average length and number density decrease significantly as the ferrocene concentration 284 decreases. This detailed TEM analysis at higher magnification (Fig S4) shows also a highly 285 reduced frequency of incorporation of nanowires into the tubes as well as a much lower mean 286 size of these nanoparticles when the ferrocene concentration is reduced. Therefore, the amount 287 of embedded nanoparticles is really low, and it is a great improvement for a one-step CCVD 288 process. For 0.1wt.% ferrocene, only 2% of the length of the nanotube inner channel is occupied 289 by iron nanowires, while it is 24% for 2.5wt.%. On average, it can be estimated that there is 1 290 nanowire every 2 µm at 0.1wt.% ferrocene while there is one nanowire every 0.4 µm at 2.5wt.% 291 (See Table S2). An analysis of structural defects (corking) in the inner channel also shows a 292 decrease in their occurrence for 0.1wt.% as compared to 2.5wt.%, but not in the same proportion 293 as nanowires (Table S2).



Fig. 4: Comparison in single injection between samples obtained with ferrocene
concentration of 0.1 and 2.5wt.%. a) SEM image of 0.1%; b) SEM image of 2.5%; c) TEM
image of 0.1%; and d) TEM image of 2.5%.

The iron content of VACNT forests is determined by TGA analysis under air (Fig. 5a) on samples taken in the same central area of the reactor as the ones used for the SEM and TEM

300 analysis above. In single injection, the iron content varies greatly and linearly with the ferrocene 301 concentration, from 0.5wt.% at 0.1wt.% ferrocene up to 9wt.% at 2.5wt.% ferrocene. This value 302 of 0.5 wt% of iron in VACNT sample is a remarkably low value as compared to the literature 303 (see Table 1 and references herein) and is even lower than that of 0.56 recently published in a 304 paper related to a two-step floating CCVD process[31]. It confirmed the great increase in the 305 VACNT purity at low ferrocene concentration as observed by TEM above. In double injection, 306 iron content variations are less pronounced as compared to single injection (Fig. 5a) due to the 307 first injection sequence at 2.5wt.%. To verify that the variation in iron content with the ferrocene 308 concentration is not due to a similar variation in iron chemical yield, we estimate the proportion 309 of injected iron found in the final product. In single injection, the incorporated iron represents 310 40% of the injected iron at 0.1wt.% ferrocene and 50% at 2.5wt.%. Therefore, the incorporation 311 rate of iron remains similar regardless of the ferrocene concentration and cannot be responsible 312 for the high difference in iron content.

The catalytic yield (Fig. 5b) scales as the inverse of the ferrocene concentration for single injection. A very high and maximum catalytic yield about 200 (200g of carbon produced by iron gram) is obtained for the lowest concentration of ferrocene (0.1wt.%) and then decreases rapidly down to 10 when the ferrocene concentration increases. For double injection, the catalytic yield is varying in a slighter range, between 16 and 35, for the whole ferrocene concentration range.



Fig. 5: Ferrocene concentration effect on a) iron content and b) catalytic yield, for single
(full dot) and double (open dot) injection (in this last case, it is the ferrocene concentration
of the second long injection sequence). Dashed lines are added as eyes guide only.

323 Regarding the CNT diameter, the distribution does not change with the ferrocene concentration 324 (Fig. 6a), with external and internal average diameters around 35 nm and 9 nm respectively. 325 Similar results are found in the case of double injection (Fig.S5). In terms of structural quality, 326 the Raman spectra of the samples obtained with 0.1 and 2.5 w.t% ferrocene are compared in Fig. 6b (see Fig. S6 for double injection): G, D and D' bands at 1580 cm⁻¹, 1350 cm⁻¹ and 327 328 1615 cm⁻¹ respectively, as well as the 2D band at 2700 cm⁻¹ are occurring. In multi-walled 329 carbon nanotubes, the D band is associated with defects and disorder and is influenced by the 330 curvature of the walls, while the G band is inherent to in plane tangential stretching of carbon-331 carbon bonds. The ratio between the D and G band intensities (I_D/I_G) is commonly used as a 332 qualitative measure of the defect density in defective tubes: the higher this ratio, the lower the 333 crystalline level [38,39]. This ratio is dependent on the excitation wavelength. The analysis of 334 the Raman spectra recorded at 514 nm on the samples obtained in the current study gives rise 335 to a I_D/I_G ratio remaining similar whatever the injection mode and the ferrocene concentration. 336 This ratio is around 0.3 and the lowest value of 0.28 is obtained at 0.25wt.% ferrocene 337 concentration in single injection (Table S1). Such values are low for multi-walled carbon 338 nanotubes produced by CVD and are related to a low defect density as discussed by Meysami 339 et al. [21]. These values compare well with those reported in Table 1 obtained with similar 340 Raman wavelengths (514 or 532 nm) for samples formed in similar conditions in terms of 341 carbon precursors and synthesis temperatures (750-850°C) [15,19,21]. By contrast, they are 342 much lower than those reported in the range [0.56-0.79] by Kinoshita et al. [31] from synthesis 343 at 700°C with acetylene as carbon source. However, it has been shown that the G band in CNT 344 can be affected by defects [39], therefore as the 2D band does not represent a disorder-induced 345 mode, the relative intensity of the D and 2D bands (I_D/I_{2D}) is also used as a qualitative measure 346 of the defect density. Kinoshita el al. [31] found a I_D/I_{2D} ratio between 0.8 and 2. In the present 347 work, this ratio is around 0.3 for almost all the ferrocene concentrations, apart for 2.5wt.% of 348 ferrocene which gives rise to a ratio of 0.36. Such low I_D/I_{2D} ratio indicates a really good 349 structural quality of the CNT forest that is well preserved and even slightly improved at low 350 ferrocene concentration. This result corroborates the same trend observed by Cho et al. [20] 351 and McKee et al. [19] with a similar one-step aerosol-assisted process.



Fig. 6: Comparison in single injection between samples obtained with ferrocene concentration of 2.5 (red) and 0.1wt.% (blue), respectively. a) Nanotube external diameter distributions from the TEM analysis of more than 100 CNTs; b) Raman spectra acquired at 514 nm at the center of forest cross-sections.

357 3.3 VACNT forest density

358 The mass per unit area of VACNTs collected on the reactor walls in the oven center (Fig. 7a) 359 increases with ferrocene concentration for both single and double injection experiments, 360 meaning that the chemical yield improves in both cases. In single injection, the areal mass is close to 2mg/cm² at 0.1wt.% and then increases gradually up to 4 mg/cm². In double injection, 361 the areal mass is already equal to 3 mg/cm² at 0.01wt.% ferrocene in the second injection and 362 then rises up to more than 6 mg/cm^2 , with values systematically higher than in single injection. 363 364 The gap between the two curves remains approximately constant around 2.5 mg/cm² in excess in double injection as compared to single injection. This difference can be attributed to the 365 366 effect of the first injection sequence with 2.5wt.% in the double injection mode. Reproducibility 367 has been tested for experiments performed with ferrocene concentration of 0.1, 0.25 and 2.5 368 wt.% in single injection and 0.1, 0.25 and 0.5 wt.% in double injection. The observed deviations 369 do not affect the general trends, particularly for single injection experiments (Fig. S6 in 370 supplementary information).

From measurements of areal masses (Fig. 7a) and forest thicknesses (Fig. 2b and Fig. 3b), the forest density can be determined and increases with the ferrocene concentration, especially in single injection (Fig. 7b). Since nanotube diameters are similar whatever the ferrocene concentration, this density increase must be related to an increase in N, the number density of nanotubes (CNTs/cm²). N can be estimated knowing the mean external diameter of the nanotubes and taking 1.8 g/cm^3 for the intrinsic carbon nanotube density as estimated by helium 377 picnometry. N is found about ~5 10^9 CNT/cm² at low ferrocene concentration, but reaches 378 ~1.7 10^{10} CNT/cm² at 1wt.%. This result suggests that the number density of catalytic 379 nanoparticles increases as well.



Fig. 7 – Ferrocene concentration effect on a) mass per unit area of carbon collected on the
reactor walls in the center zone, and b) measured mass density, for single (full dot) and
double (open dot) injection (in this last case, it is the ferrocene concentration of the second
long injection sequence). Dashed lines are added as eyes guide only.

385 **3.4 Oxidation resistance**

380

386 The TGA mass-loss profiles are very dependent on the ferrocene concentration (Fig. 8a; see 387 also Fig. S8). In single injection, the profile is strongly shifted towards the high temperatures 388 when the ferrocene concentration decreases. The oxidation temperature (Tox), taken as the 389 temperature of the peak in the TGA graph derivatives (Fig. 8b and Fig. S8), decreases quasi-390 linearly from 685°C down to 550°C when ferrocene increases from 0.1 to 2.5wt.%. Since in 391 single injection the iron content of the sample was previously found to be a linear function of 392 the ferrocene concentration (Fig 5a), T_{ox} appears to be a linear function of the iron content as 393 well (Fig. 8c and Fig. S9). In the case of double injection, the TGA profile exhibits a remarkable 394 shoulder on the high temperature side when the ferrocene concentration in the second injection 395 sequence is lower than 0.5wt.%, so that two T_{ox} (labelled Double1 and Double2) can be 396 identified at low ferrocene concentrations (Fig. 8c and S9). The difference between both values 397 is really significant (nearly 100°C) which points to the existence of two distinct components in 398 the samples as discussed below.



Fig. 8: a) TGA graphs obtained at a temperature rate of 10°C/min and b) their derivatives
for single injection samples (blue dashed lines labelled from S_0.1 to S_2.5 according to
the ferrocene concentration) compared to the double injection with 0.01wt.% ferrocene
in the second injection sequence (orange solid line labelled D_0.01). c) Oxidation
temperature as a function of iron content. In double injection the label "Double2"
corresponds to the second peak at high temperature when observed in the dTG graph.
See also Fig. S8.

407 **4 Discussion**

The present results show that the one-step aerosol-assisted CCVD process can be operated at very low ferrocene concentration (0.1 wt.%) using an Ar/H2 gas mixture as carrier gas. Using these conditions and a synthesis temperature of 800°C, we demonstrate that this one-step 411 process enables the formation with a high catalytic yield (200) of VACNT forests exhibiting 412 low impurity level (0.5 wt.% of Fe). Such low ferrocene concentration does not involve any 413 reduction of CNT growth rate since it remains higher than 20 μ m/min. Compared to the 414 literature (Table 1), it is, to our knowledge, the lowest concentration of ferrocene reported so 415 far for aerosol-assisted CCVD process leading to such growth rates and impressive catalytic 416 efficiency, thus involving the formation of high purity VACNT forests. The growth of a 417 VACNT forest becomes impossible only when the ferrocene concentration falls below 0.1wt.%.

418 When it increases up to 1wt.%, the growth rate decreases by a factor of 2, while the number

419 density N is multiplied by more than 3 going from 5 10^9 to 1.7 10^{10} cm⁻².

420 Regarding the mechanisms at play, hydrogen plays a significant role in the process of ferrocene 421 decomposition. Indeed, our previous results obtained at 850°C with 2.5wt.% ferrocene [34] 422 have shown that including 30% of H_2 in the Ar gas flow induces an increase of N from 5 10^9 to 2 10¹⁰ CNT.cm⁻² as well as a decrease of the mean CNT external diameter. These results were 423 424 attributed to the hydrogen induced enhancement of the dissociation rate of ferrocene. As a 425 consequence, there is a fast rise of the iron partial pressure in the reactor and a high level of 426 supersaturation which affects the homogeneous nucleation process of the iron nanoparticles. A 427 much higher number of smaller nuclei forms, which leads to a higher number density of 428 catalytic nanoparticles deposited on the substrate and therefore to a higher density of growing 429 CNTs. Such very efficient effect of hydrogen on the catalytic particles density is responsible 430 for the remarkable decrease in the ferrocene concentration allowing to reach the threshold in 431 density of CNTs needed to form a self-supporting forest structure [40]. Interestingly, in the present work at 0.1wt.% ferrocene in single injection mode, N is equal to 5 10⁹CNT.cm⁻², a 432 433 value similar to the one obtained without hydrogen at 2.5wt.% ferrocene with the same one-434 step aerosol assisted CCVD process [18]. This number allowing the vertical self-organization of the interacting CNTs is comparable to the value of about 2 10⁹ CNTs/cm² reported by 435 Bedewy et al. [40]. This threshold is obviously not reached below 0.1wt.%, explaining the 436 437 absence of VACNT growth at such low concentration. This threshold was also not reached 438 without hydrogen for ferrocene concentration below 1.25wt.%, explaining why no VACNTs 439 were observed at 0.1 and 0.5wt.% by Castro et al. [15].

440 In double injection synthesis, the first injection sequence with 2.5wt.% ferrocene determines 441 the density of catalytic nanoparticles. So N is higher from the beginning of the precursor 442 injection and its evolution is less pronounced with the ferrocene concentration increase in the second injection sequence, where a ferrocene concentration as low as 0.05wt.% is sufficient tosustain the growth.

445 The existence of a clear threshold in the ferrocene concentration allowing the self-organization 446 of VACNTs is responsible for the sharp increase in the growth rate with ferrocene concentration observed for single injection experiments (Fig. 3b). The slow decrease observed after the 447 448 maximum (Fig. 3b), as also observed by others [32,33], is generally attributed to an increase in 449 VACNT density. Call et al. [41] show that ferrocene concentration dictates forest density but 450 that forest thickness is limited by density presumably due to diffusion-limited precursor supply. 451 However, in our case, the forest thickness is found proportional to the synthesis duration at least up to 90 min even at 1.25 wt.% ferrocene where the forest density is above 10¹⁰ CNT/cm² (Fig. 452 453 S3). Indeed, the flow rate is too high and the average inter-tube distance too large (between 60 454 and 150 nm) to encounter feedstock resistance [42]. Same conclusion was reported by Cho et 455 al. [20] leading them to invoke, as Bai et al. [33], a weaker activity of the catalytic nanoparticles 456 due to their size increasing with ferrocene concentration [8]. However, in our study, the CNT 457 diameter remains similar whatever the ferrocene concentration, which implies that the catalytic 458 particle size remains also the same [8]. In the present range of ferrocene concentration, this size 459 is mainly governed by temperature, H_2 content and nature of the substrate, all these parameters 460 being constant here. On the other hand, when the number density of nanotubes increases, the 461 amount of precursors available per nanotube decreases, in principle in inverse proportion to the 462 density. This is not exactly what we are observing here since the mass per unit area that is the 463 product of the two is not constant, but increases. Such result could be rationalized considering 464 that at very low forest density, not all the carbon precursors impinging the substrate area around 465 a given CNT (intertube distance is 150 nm) are able to interact with the catalyst particle, but 466 their proportion increases when the intertube distance decreases. Such effect could explain the 467 observed variation of growth rate.

468 Regarding the iron content of the VACNT forest, it increases linearly from 0.48 to 8.75 wt.% 469 with the ferrocene concentration in single injection, and the atomic ratio Fe/C in the forest 470 appears to be 10 times the Fe/C ratio in the precursors (Fig. S10). It means that the iron 471 conversion is 10 times higher than the carbon conversion. It should be noted that the 472 contribution of the catalyst nanoparticles themselves to the iron content is very low as is out of 473 principle the case for any VACNT forest (see its estimation in Supplementary Data). The iron 474 incorporated in the material is predominantly found as nanowires encapsulated in the inner 475 channel as a consequence of the continuous refreshment of the catalyst nanoparticles from the

iron-based nanoparticles continuously nucleated in the gas phase [18] in the one-step aerosol-476 477 assisted CCVD process. When the ferrocene concentration is decreased, the percentage of the 478 CNT inner channel length occupied by the nanowires (Fig. S4 and Table S2) drastically 479 decreases: it is estimated to be 10 times lower for the optimal concentration of 0.1wt.% 480 ferrocene as compared to 2.5wt.%, which corresponds to an encapsulation frequency which is 481 3 times lower.. Since the CNT growth rate is two-fold higher at 0.1wt.% than at 2.5 wt.%, it 482 means that the acceleration in the refreshment at high ferrocene concentration does not allow 483 to increase the growth rate but only leads to an increase of the iron content.

- 484 Iron can be incorporated in the forest also as nanoparticles found outside the nanotubes. This 485 contribution increases a lot when the ferrocene concentration increases, as observed by SEM and TEM (Fig. 4) and by others [21,33]. Since TEM observations show that the amount of 486 487 external nanoparticles is negligible in the sample obtained at 0.1wt.% ferrocene, then we can 488 estimate from the TEM analysis of the inner channel (Table S2) that the iron inside the tubes 489 represents about 2/3 of the total iron content for the sample formed with 2.5wt% ferrocene. 490 Therefore, external nanoparticles contain at most a third of the iron content. Their presence in 491 large quantities is due to the large increase, with the ferrocene concentration, of the number 492 density of iron nanoparticles in the precursor gas flow going towards the substrate through the 493 carpet. To avoid the formation of such large proportion of by-products in the presence of H₂, 494 the ferrocene concentration must be kept lower than 1wt.%.
- 495 Regarding now the size and crystalline structure of the nanotubes, both TEM and Raman 496 analysis show that their structure and diameter depend only slightly on the concentration of 497 ferrocene in the range studied here. The ID/IG ratio of 0.3 indicates a good structural quality 498 with a low defect density for MWCNTs as observed previously [15,21]. That is why it is not 499 possible to interpret the large variation in the oxidation temperature with the ferrocene 500 concentration in terms of variation of the structural properties. Even considering the position of 501 the G-band, which was found to correlate with T_{ox} in the literature [43], it is not possible to 502 invoke such structure evolution, since here, the G-band position is very stable (Table S1). 503 Alternatively, the catalytic activity of the iron-based compounds inside the forests during the 504 TGA was also considered in the literature since it is able to change the kinetic parameters of 505 the oxidation [19,21,23–25]. In the present case, this second interpretation is strongly supported by the strong correlation found between Tox and iron content in single injection synthesis 506 507 (Fig.8c). Also, the highest oxidation temperature (680°C) obtained for the sample with the 508 lowest iron content is found very similar to the one of VACNT sample freed from iron after a

509 heat-treatment at 2000°C [29]. Moreover, in double injection, the catalytic activity of the iron-510 based compounds allows to understand directly the presence of two components in the TGA 511 graphs. When the ferrocene concentration is very different between the two injection sequences, 512 two layers are formed with very different iron contents and different oxidation temperatures. 513 The highest oxidation temperature is close to those obtained with single injection with a similar 514 low ferrocene concentration. The large variation in oxidation temperature under dry air can be 515 correlated to the iron content and the double peak observed for sample synthesized by double 516 injection underlines the localized catalytic role of iron compounds in the oxidation reaction as 517 mentioned in [25]. It could be used to perform selective oxidation of the carpet top in order to 518 suppress the layer where the CNTs are entangled and to open the tubes. Also, double injection 519 experiments offer the possibility to control independently forest density and growth rate while 520 limiting the iron content. The forest density is determined by the ferrocene concentration in the 521 first injection sequence while the growth rate depends mostly on the ferrocene concentration in 522 the second injection sequence.

523 **5** Conclusion

524 Our results show that, in the aerosol-assisted CCVD process, the addition of H_2 in the carrier 525 gas results in a significant increase in the number density of catalytic nanoparticles, due to its 526 strong influence on the decomposition kinetics of the ferrocene. As a result, the formation of a 527 self-organized VACNT forest occurs at a much lower ferrocene concentration than without 528 hydrogen and a pristine forest of high purity is formed with high catalytic yield at a performing 529 growth rate. At 800°C, with 30% H₂ in Ar, VACNT forest is formed with only 0.1wt.% 530 ferrocene (Fe/C=0.007at%), a value 25 times lower than the usual one of 2.5% optimized 531 without hydrogen. The iron content falls down to 0.5wt.%, so that the catalytic yield is strongly 532 enhanced by a factor of 20, while the growth rate is improved by a factor of 2 and the crystalline structure remains of high quality. A forest density of 5 10⁹ CNTs/cm² appears to be the 533 534 threshold for the self-organization of the nanotubes to occur. This number density increases 535 with the ferrocene concentration, due to the increase in the number density of catalytic 536 nanoparticles. The iron content of the forest is directly proportional to the ferrocene 537 concentration. When it decreases, the frequency of encapsulation of iron nanowires in the inner 538 channel of the tubes decreases significantly and the oxidation resistance of the samples is 539 greatly improved, with an increase in oxidation temperature equal to 100°C. Finally, double 540 injection experiments appear to be an attractive approach in order to optimize independently 541 the density and the growth rate of the forest, since the density is fixed by the initial ferrocene

543	3 the	the concentration in the second injection sequence.							
544	4 Ack	Acknowledgement							
54: 540 54	5 The 6 Poly 7 Ran	The authors would like to thank M. Paternostre (CEA Saclay), PE. Coulon (LSI, Ecole Polytechnique Palaiseau) and J. N. Rouzaud (ENS Paris) for access to TEM, HRTEM and Raman analysis facilities, respectively.							
548	8								
549	9 App	Appendix A. Supplementary data							
55(55)	0 Sup 1	Supplementary data associated with this article can be found, in the online version, at							
552	2 Ref	References							
553 554 555	3 [1] 4 5	A.M. Marconnet, N. Yamamoto, M.A. Panzer, B.L. Wardle, K.E. Goodson, Thermal Conduction in Aligned Carbon Nanotube- Polymer Nanocomposites with High Packing Density, ACS Nano. 5 (2011) 4818–4825. doi:10.1021/nn200847u.							
550 557 558 559 560	6 [2] 7 8 9 0	 S. Lagoutte, PH. Aubert, M. Pinault, F.O. Tran-Van, M. Mayne-L 'hermite, C. Chevrot, Poly(3-methylthiophene)/Vertically Aligned Multi-walled Carbon Nanotubes: Electrochemical Synthesis, Characterizations and Electrochemical Storage Properties in Ionic Liquids, Electrochim. Acta. 130 (2014) 754–765. doi:10.1016/j.electacta.2014.03.097. 							
562 562 563	1 [3] 2 3	K. Evanoff, J. Khan, A.A. Balandin, A. Magasinski, W.J. Ready, T.F. Fuller, G. Yushin, Towards ultrathick battery electrodes: Aligned carbon nanotube-enabled architecture, Adv. Mater. 24 (2012) 533–537. doi:10.1002/adma.201103044.							
564 565 560	4 [4] 5 6	H. Cebeci, I.Y. Stein, B.L. Wardle, Effect of nanofiber proximity on the mechanical behavior of high volume fraction aligned carbon nanotube arrays, Appl. Phys. Lett. 104 (2014). doi:10.1063/1.4862273.							
56 568 569	7 [5] 8 9	[5] J.R. Raney, F. Fraternali, C. Daraio, Rate-independent dissipation and loading direction effects in compressed carbon nanotube arrays, Nanotechnology. 24 (2013) 255707 doi:10.1088/0957-4484/24/25/255707.							
57(57)	0 [6] 1	M. Kumar, Y. Ando, Chemical Vapor Deposition of Carbon Nanotubes: A Review on Growth Mechanism and Mass Production, J. Nanosci. Nanotechnol. 10 (2010) 3739–							

concentration in the first short injection sequence while the growth rate can be controlled by

542

- 572 3758. doi:10.1166/jnn.2010.2939.
- [7] R. Guzmán de Villoria, S.L. Figueredo, A.J. Hart, S.A.I. Steiner, A.H. Slocum, B.L.
 Wardle, High-yield growth of vertically aligned carbon nanotubes on a continuously
 moving substrate, Nanotechnology. 20 (2009) 405611. doi:10.1088/09574484/20/40/405611.
- 577 [8] V. Jourdain, C. Bichara, Current understanding of the growth of carbon nanotubes in
 578 catalytic chemical vapour deposition, Carbon N. Y. 58 (2013) 2–39.
 579 doi:10.1016/j.carbon.2013.02.046.
- [9] R. Andrews, D. Jacques, a. M. Rao, F. Derbyshire, D. Qian, X. Fan, E.C. Dickey, J.
 Chen, Continuous production of aligned carbon nanotubes: a step closer to commercial
 realization, Chem. Phys. Lett. 303 (1999) 467–474. doi:10.1016/S0009-2614(99)002821.
- [10] M. Mayne, N. Grobert, M. Terrones, R. Kamalakaran, M. Rühle, H.W. Kroto, D.R.M.
 Walton, Pyrolytic production of aligned carbon nanotubes from homogeneously
 dispersed benzene-based aerosols, Chem. Phys. Lett. 338 (2001) 101–107.
 doi:10.1016/S0009-2614(01)00278-0.
- 588 [11] X. Zhang, a Cao, B. Wei, Y. Li, J. Wei, C. Xu, D. Wu, Rapid growth of well-aligned
 589 carbon nanotube arrays, Chem. Phys. Lett. 362 (2002) 285–290. doi:10.1016/S0009590 2614(02)01025-4.
- 591 [12] R.A. Afre, T. Soga, T. Jimbo, M. Kumar, Y. Ando, M. Sharon, Growth of vertically 592 aligned carbon nanotubes on silicon and quartz substrate by spray pyrolysis of a natural 593 precursor: Turpentine oil, Chem. Phys. Lett. 414 (2005)6–10. 594 doi:10.1016/j.cplett.2005.08.040.
- 595 [13] C. Singh, M.S.P. Shaffer, A.H. Windle, Production of controlled architectures of aligned
 596 carbon nanotubes by an injection chemical vapour deposition method, Carbon N. Y. 41
 597 (2003) 359–368.
- 598 [14] P. Boulanger, L. Belkadi, J. Descarpentries, D. Porterat, E. Hibert, A. Brouzes, M. Mille,
 599 S. Patel, M. Pinault, C. Reynaud, M. Mayne-L'Hermite, J.M.M. Decamps, Towards
 600 large scale aligned carbon nanotube composites: an industrial safe-by-design and
 601 sustainable approach, J. Phys. Conf. Ser. 429 (2013) 012050. doi:10.1088/1742602 6596/429/1/012050.

- 603 [15] C. Castro, M. Pinault, S. Coste-Leconte, D. Porterat, N. Bendiab, C. Reynaud, M.
 604 Mayne-L'Hermite, Dynamics of catalyst particle formation and multi-walled carbon
 605 nanotube growth in aerosol-assisted catalytic chemical vapor deposition, Carbon N. Y.
 606 48 (2010) 3807–3816. doi:10.1016/j.carbon.2010.06.045.
- M. Pinault, M. Mayne-L'Hermite, C. Reynaud, V. Pichot, P. Launois, D. Ballutaud, M.
 Mayne-L'Hermite, C. Reynaud, V. Pichot, P. Launois, D. Ballutaud, Growth of
 multiwalled carbon nanotubes during the initial stages of aerosol-assisted CCVD,
 Carbon N. Y. 43 (2005) 2968–2976. doi:10.1016/j.carbon.2005.06.011.
- [17] R. Xiang, G. Luo, W. Qian, Q. Zhang, Y. Wang, F. Wei, Q. Li, A. Cao, Encapsulation,
 compensation, and substitution of catalyst particles during continuous growth of carbon
 nanotubes, Adv. Mater. 19 (2007) 2360–2363. doi:10.1002/adma.200602468.
- [18] P. Landois, M. Pinault, S. Rouzière, D. Porterat, C. Mocuta, E. Elkaim, M. MayneL'Hermite, P. Launois, In situ time resolved wide angle X-ray diffraction study of
 nanotube carpet growth: Nature of catalyst particles and progressive nanotube alignment,
 Carbon N. Y. 87 (2015) 246–256. doi:10.1016/j.carbon.2015.01.046.
- 618 [19] G.S.B. McKee, C.P. Deck, K.S. Vecchio, Dimensional control of multi-walled carbon
 619 nanotubes in floating-catalyst CVD synthesis, Carbon N. Y. 47 (2009) 2085–2094.
 620 doi:10.1016/j.carbon.2009.03.060.
- [20] J. Cho, A.R. Boccaccini, M.S.P. Shaffer, The influence of reagent stoichiometry on the
 yield and aspect ratio of acid-oxidised injection CVD-grown multi-walled carbon
 nanotubes, Carbon N. Y. 50 (2012) 3967–3976. doi:10.1016/j.carbon.2012.03.049.
- 624 [21] S.S. Meysami, A. a. Koós, F. Dillon, N. Grobert, Aerosol-assisted chemical vapour
 625 deposition synthesis of multi-wall carbon nanotubes: II. An analytical study, Carbon N.
 626 Y. 58 (2013) 151–158. doi:10.1016/j.carbon.2013.02.041.
- 627 [22] P.X. Hou, C. Liu, H.M. Cheng, Purification of carbon nanotubes, Carbon N. Y. 46 (2008)
 628 2003–2025. doi:10.1016/j.carbon.2008.09.009.
- [23] I.W. Chiang, B.E. Brinson, R.E. Smalley, J.L. Margrave, R.H. Hauge, Purification and
 Characterization of Single-Wall Carbon Nanotubes, J. Phys. Chem. B. 105 (2001) 1157–
 1161. doi:10.1021/jp003453z.
- 632 [24] A.-R. Leino, M. Mohl, J. Kukkola, P. Mäki-Arvela, T. Kokkonen, A. Shchukarev, K.
 633 Kordas, Low-temperature catalytic oxidation of multi-walled carbon nanotubes, Carbon

- 634 N. Y. 57 (2013) 99–107. doi:10.1016/j.carbon.2013.01.040.
- 635 [25] C. Wang, S. Guo, X. Pan, W. Chen, X. Bao, Tailored cutting of carbon nanotubes and
 636 controlled dispersion of metal nanoparticles inside their channels, J. Mater. Chem. 18
 637 (2008) 5782. doi:10.1039/b811560e.
- E.R. Edwards, E.F. Antunes, E.C. Botelho, M.R. Baldan, E.J. Corat, Evaluation of
 residual iron in carbon nanotubes purified by acid treatments, Appl. Surf. Sci. 258 (2011)
 641–648. doi:10.1016/j.apsusc.2011.07.032.
- 641 [27] B.H.R. Suryanto, T. Fang, S. Cheong, R.D. Tilley, C. Zhao, From the inside-out:
 642 Leached metal impurities in multiwall carbon nanotubes for purification or
 643 electrocatalysis, J. Mater. Chem. A. 6 (2018) 4686–4694. doi:10.1039/c7ta11257b.
- K. Yang, M. Yang, H. Zhang, J. Zhao, X. Zhang, Q. Li, Electro-purification of carbon
 nanotube networks without damaging the assembly structure and crystallinity, Appl.
 Surf. Sci. 442 (2018) 232–238. doi:10.1016/j.apsusc.2018.02.169.
- 647 M. Pinault, M. Mayne-L'Hermite, C. Reynaud, O. Beyssac, J.N. Rouzaud, C. Clinard, [29] 648 Carbon nanotubes produced by aerosol pyrolysis: growth mechanisms and post-649 annealing effects, Diam. Relat. Mater. 13 (2004)1266-1269. 650 doi:10.1016/j.diamond.2003.12.015.
- [30] W. Huang, Y. Wang, G. Luo, F. Wei, 99.9% Purity Multi-Walled Carbon Nanotubes By
 Vacuum High-Temperature Annealing, Carbon N. Y. 41 (2003) 2585–2590.
 doi:10.1016/S0008-6223(03)00330-0.
- [31] T. Kinoshita, M. Karita, T. Nakano, Y. Inoue, Two step floating catalyst chemical vapor
 deposition including in situ fabrication of catalyst nanoparticles and carbon nanotube
 forest growth with low impurity level, Carbon N. Y. 144 (2019) 152–160.
 doi:10.1016/j.carbon.2018.12.019.
- 658 M.I. Ionescu, Y. Zhang, R. Li, X. Sun, H. Abou-Rachid, L.S. Lussier, Hydrogen-free [32] 659 spray pyrolysis chemical vapor deposition method for the carbon nanotube growth: 660 Parametric studies, Surf. Sci. 257 (2011)6843-6849. Appl. 661 doi:10.1016/j.apsusc.2011.03.011.
- [33] X. Bai, D. Li, Y. Wang, J. Liang, Effects of temperature and catalyst concentration on
 the growth of aligned carbon nanotubes, Tsinghua Sci. Technol. 10 (2005) 729–735.
 doi:10.1016/S1007-0214(05)70142-5.

- 665 [34] C. Castro, M. Pinault, D. Porterat, C. Reynaud, M. Mayne-L'Hermite, The role of
 666 hydrogen in the aerosol-assisted chemical vapor deposition process in producing thin
 667 and densely packed vertically aligned carbon nanotubes, Carbon N. Y. 61 (2013) 585–
 668 594. doi:10.1016/j.carbon.2013.05.040.
- 669 [35] M. Pinault, V. Pichot, H. Khodja, P. Launois, C. Reynaud, M. Mayne-L'Hermite,
 670 Evidence of sequential lift in growth of aligned multiwalled carbon nanotube
 671 multilayers, Nano Lett. 5 (2005) 2394–2398. doi:10.1021/nl051472k.
- [36] S.S. Meysami, F. Dillon, A. a. Koós, Z. Aslam, N. Grobert, Aerosol-assisted chemical
 vapour deposition synthesis of multi-wall carbon nanotubes: I. Mapping the reactor,
 Carbon N. Y. 58 (2013) 159–169. doi:10.1016/j.carbon.2013.02.044.
- E. Charon, J.-N. Rouzaud, J. Aléon, Graphitization at low temperatures (600-1200°C) in
 the presence of iron implications in planetology, Carbon N. Y. 66 (2014) 178–190.
 doi:10.1016/j.carbon.2013.08.056.
- [38] M.A. Pimenta, G. Dresselhaus, M.S. Dresselhaus, L.G. Cancado, A. Jorio, R. Saito,
 Studying disorder in graphite-based systems by Raman spectroscopy, Phys. Chem.
 Chem. Phys. 9 (2007) 1276–1291.
- [39] J. Maultzsch, S. Reich, C. Thomsen, S. Webster, R. Czerw, D.L. Carroll, S.M.C. Vieira,
 P.R. Birkett, C.A. Rego, Raman characterization of boron-doped multiwalled carbon
 nanotubes, Appl. Phys. Lett. 81 (2002) 2647–2649. doi:10.1063/1.1512330.
- [40] M. Bedewy, E.R. Meshot, H. Guo, E.A. Verploegen, W. Lu, A.J. Hart, Collective
 mechanism for the evolution and self-termination of vertically aligned carbon nanotube
 growth, J. Phys. Chem. C. 113 (2009) 20576–20582. doi:10.1021/jp904152v.
- [41] R.W. Call, C.G. Read, C. Mart, T.C. Shen, The density factor in the synthesis of carbon
 nanotube forest by injection chemical vapor deposition, J. Appl. Phys. 112 (2012).
 doi:10.1063/1.4768928.
- [42] R. Xiang, Z. Yang, Q. Zhang, G. Luo, W. Qian, F. Wei, M. Kadowaki, E. Einarsson, S.
 Maruyama, Growth deceleration of vertically aligned carbon nanotube arrays: Catalyst
 deactivation or feedstock diffusion controlled?, J. Phys. Chem. C. 112 (2008) 4892–
 4896. doi:10.1021/jp710730x.
- 694 [43] S. Santangelo, G. Messina, G. Faggio, M. Lanza, C. Milone, Evaluation of crystalline
 695 perfection degree of multi-walled carbon nanotubes: Correlations between thermal

- 696 kinetic analysis and micro-Raman spectroscopy, J. Raman Spectrosc. 42 (2011) 593–
- 697 602. doi:10.1002/jrs.2766.