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*SACSESS meeting
Warsaw, April 2015*

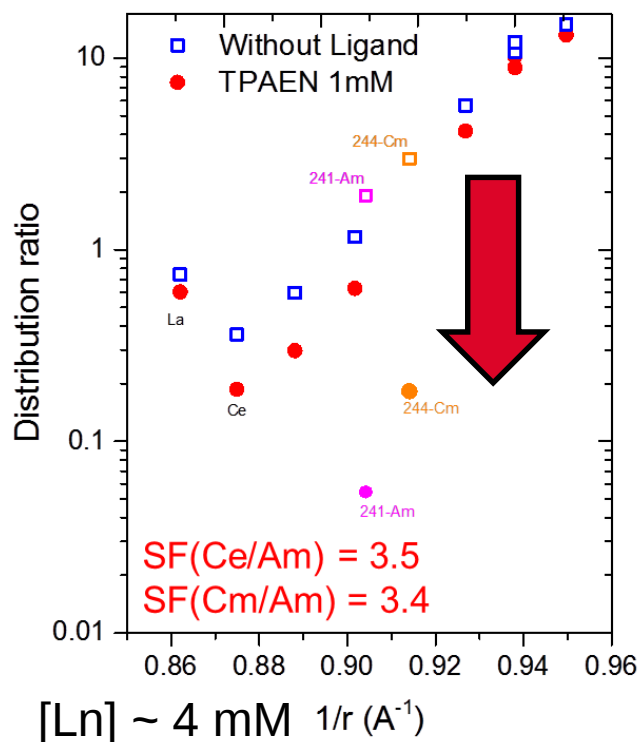
Modelling of Am stripping step with TODGA - TPAEN

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- Discuss the feasibility of a flowsheet compared to performances, based on two approaches : theoretical stages and a first model implemented in the PAREX code
- Make a progress report on modelling and identify a list of experiments to strengthen the model
- Suggest a first flowsheet



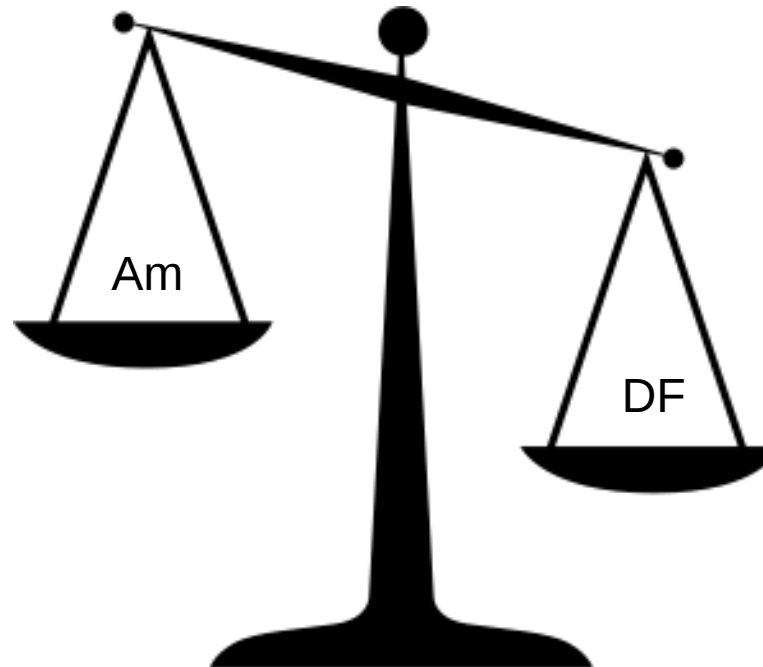
Feed (mg/L)	
[La]	350
[Ce]	750
[Pr]	400
[Nd]	1400
[Am]	420

$[Ln] \sim 25 \text{ mM}$

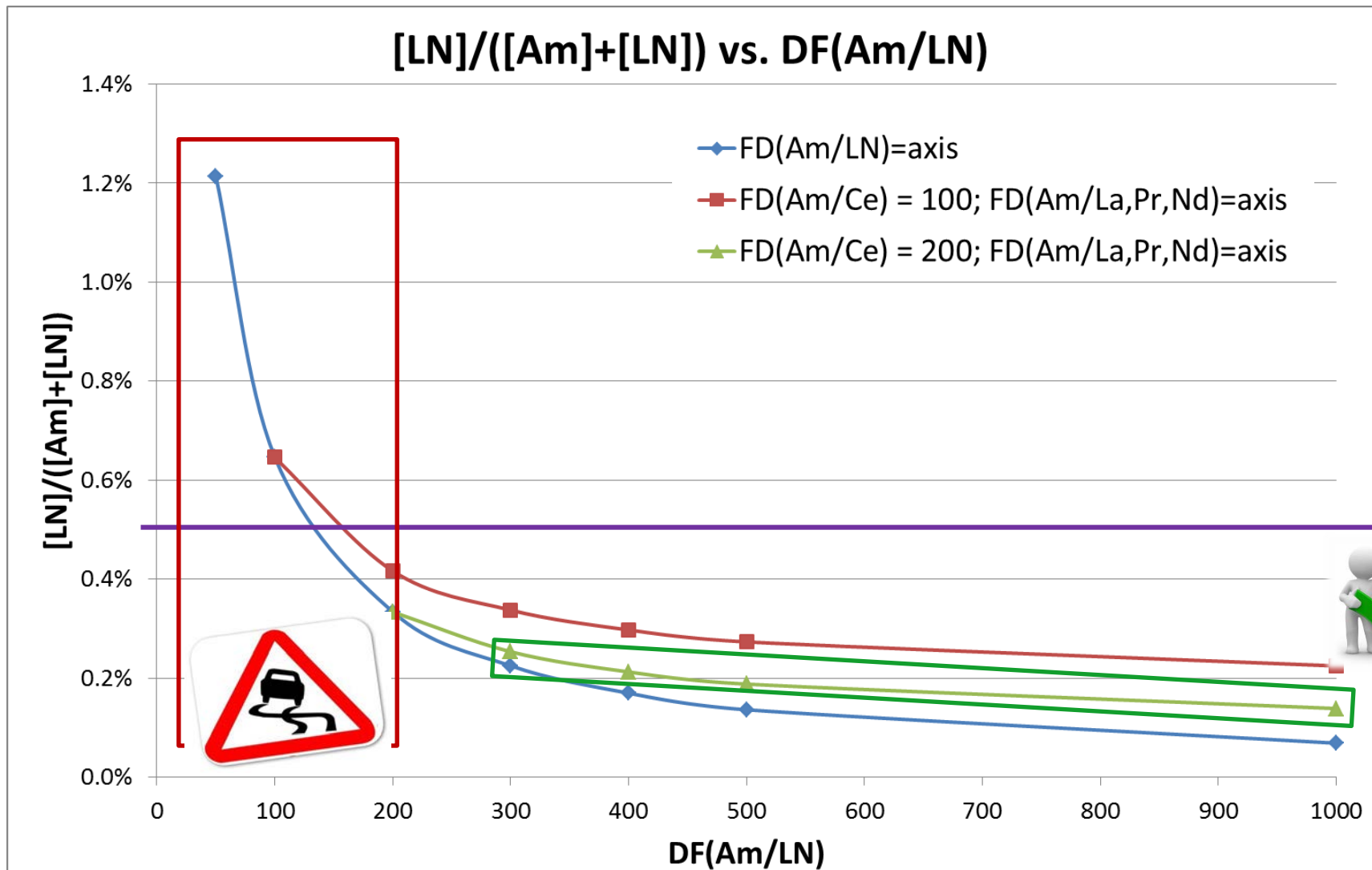
Target performances

- Am recovery rate : $> 90\%?$, $> 95\%?$, $> 99\%?$
- $DF(Am/Cm) > 500$?
- $Ln / (Am + Ln) < 5\%$?
- Number of stages

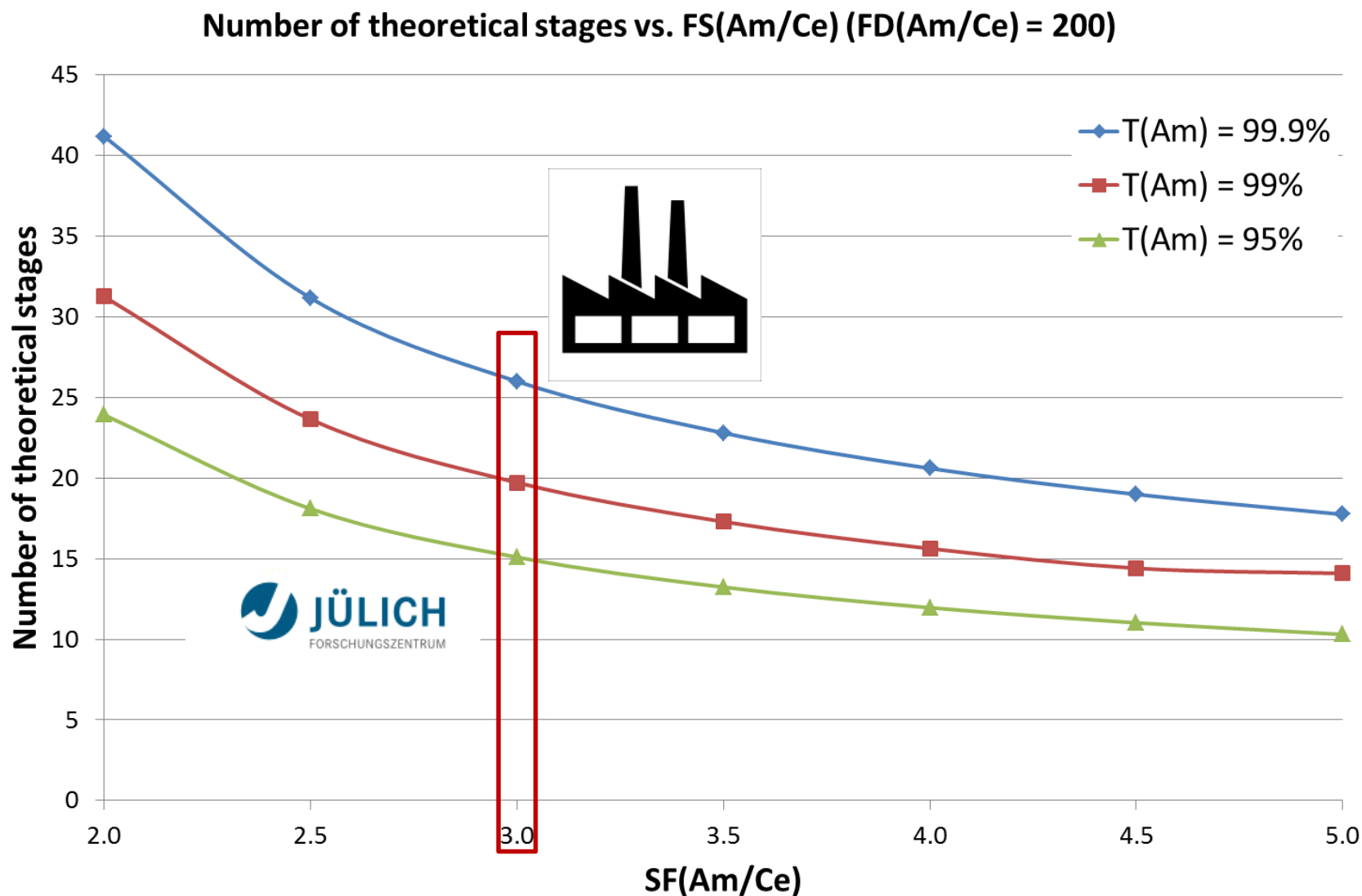
Number of stages
hot test $\neq$ industrial process



Which DF(Am/Ln) ?

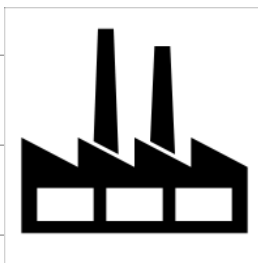
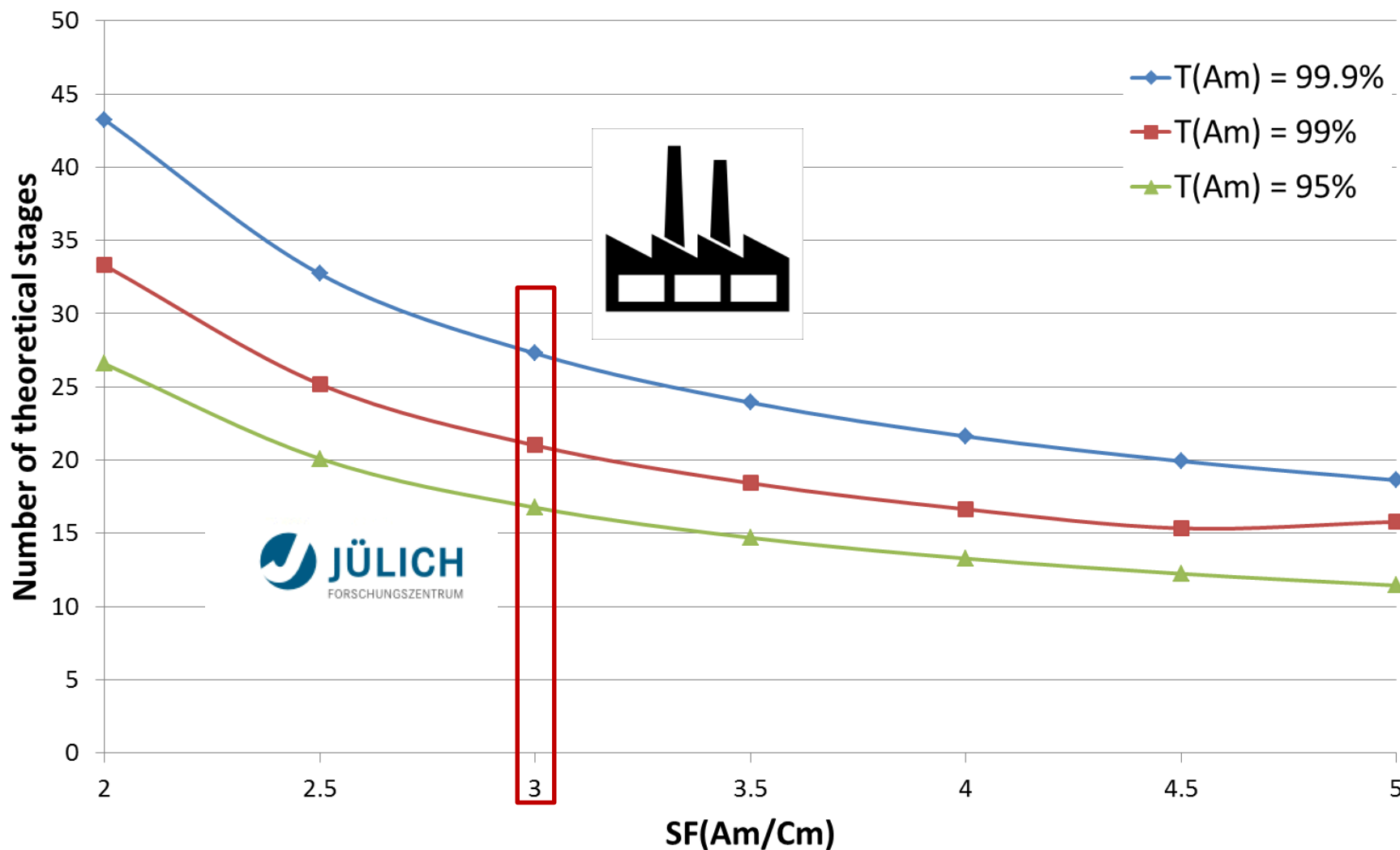


Am recovery vs. number of theoretical stages and SF(Am/Ce)



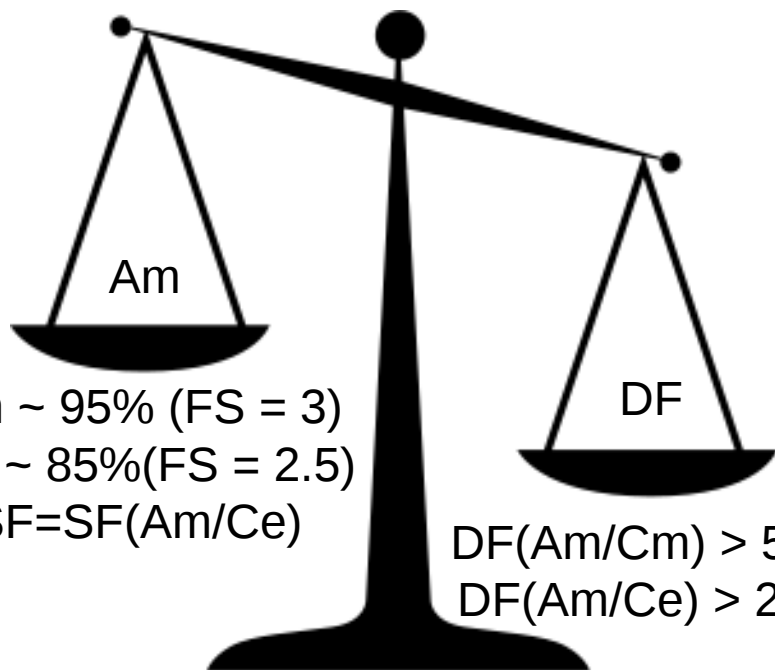
Am recovery vs. number of theoretical stages and SF(Am/Cm)

Number of theoretical stages vs. FS(Am/Cm) (FD(Am/Cm) = 500)



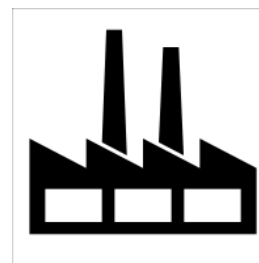


Number of stages = 16

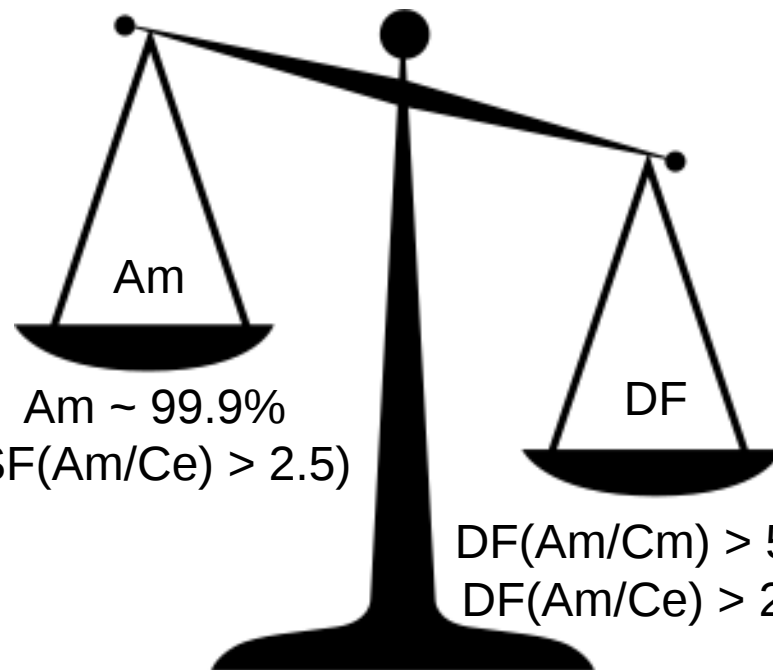


Am ~ 95% (FS = 3)
Am ~ 85% (FS = 2.5)
SF = SF(Am/Ce)

DF(Am/Cm) > 500
DF(Am/Ce) > 200



Number of stages = 32

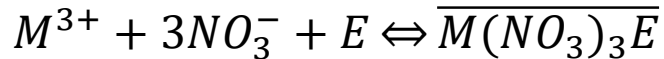


Am ~ 99.9%
(SF(Am/Ce) > 2.5)

DF(Am/Cm) > 500
DF(Am/Ce) > 200

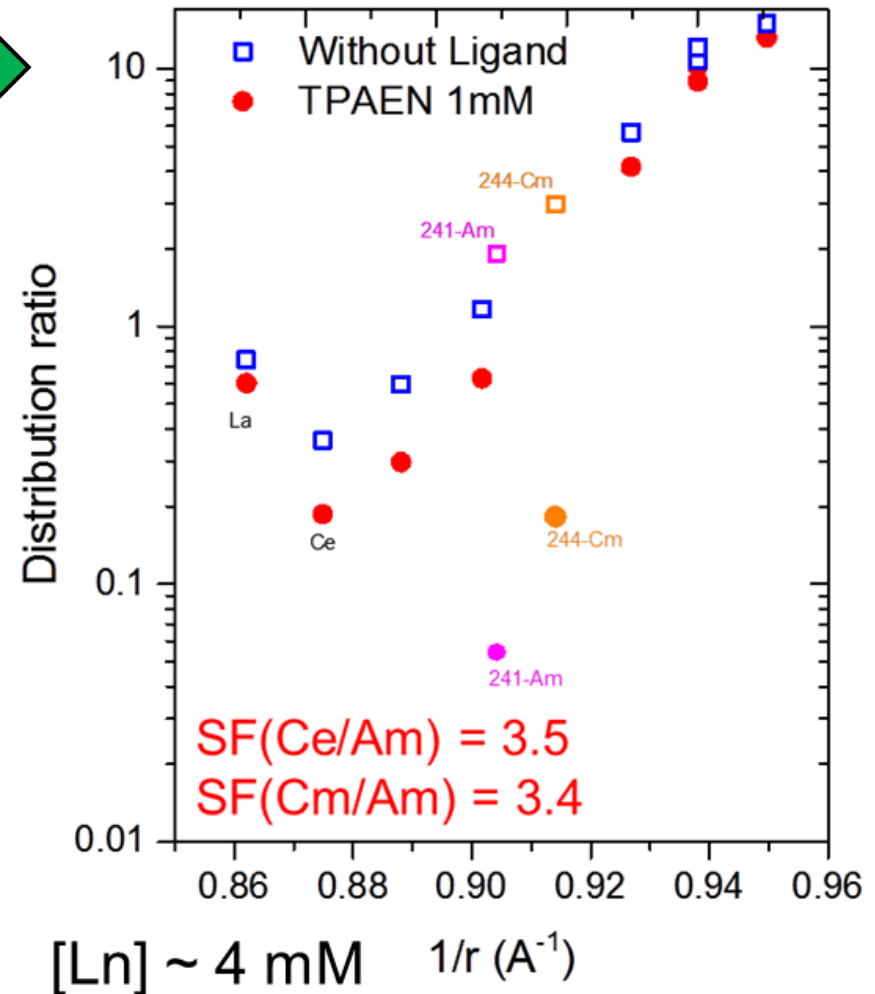
- Experiments used (2+2) 
- Assumption : diluted solutions (no salt, no high nitric acid concentration) => not necessary to take into account the deviation from ideality (chemical activities)

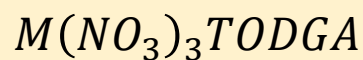
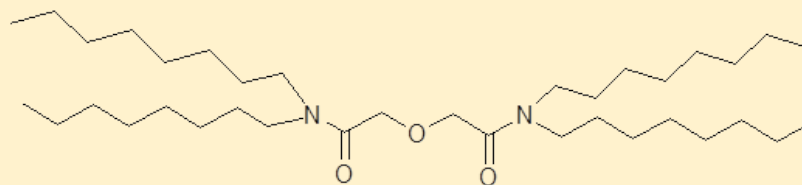
- Phenomenological model



$$[\overline{M(NO_3)_3E}] = K[M^{3+}][NO_3^-]^3[\bar{E}]$$

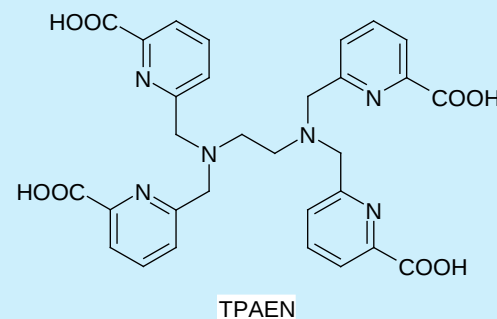
- First model = a lot of improvements to be made but a good way to determine a list of further experiments



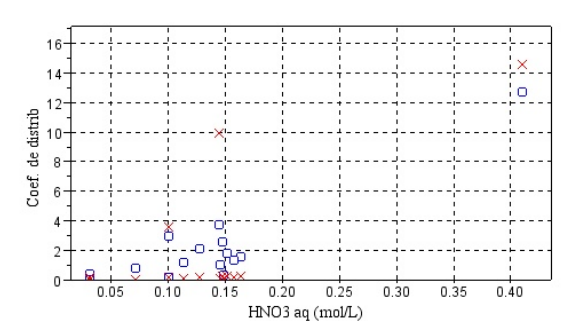
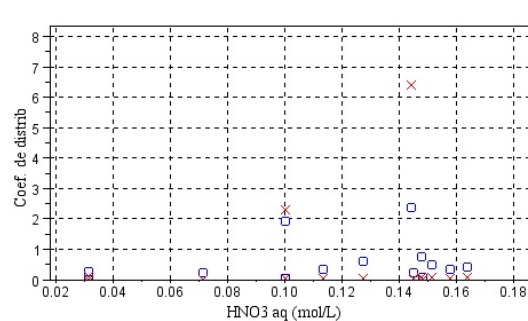
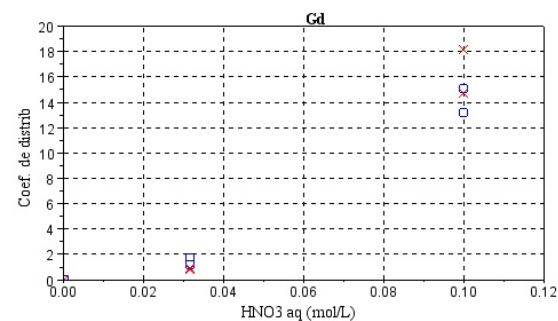
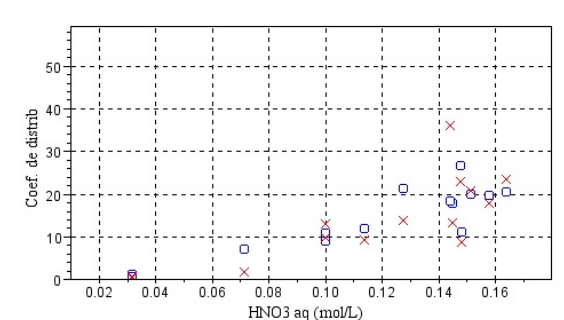
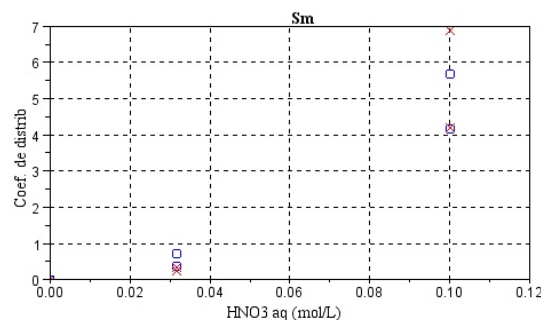
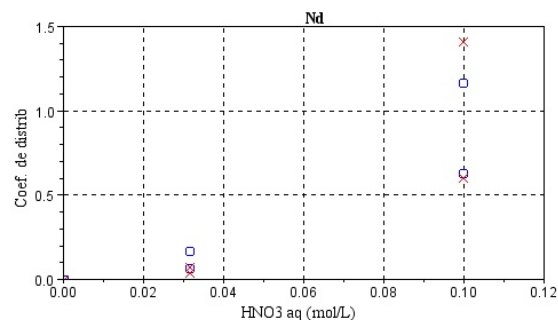
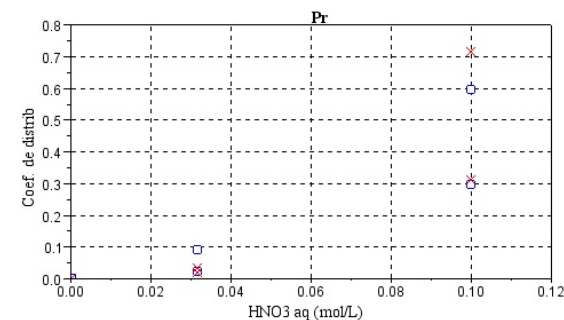
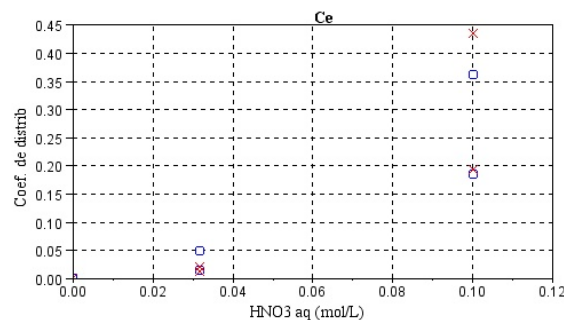
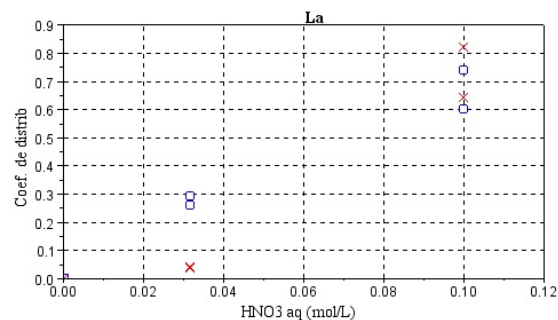


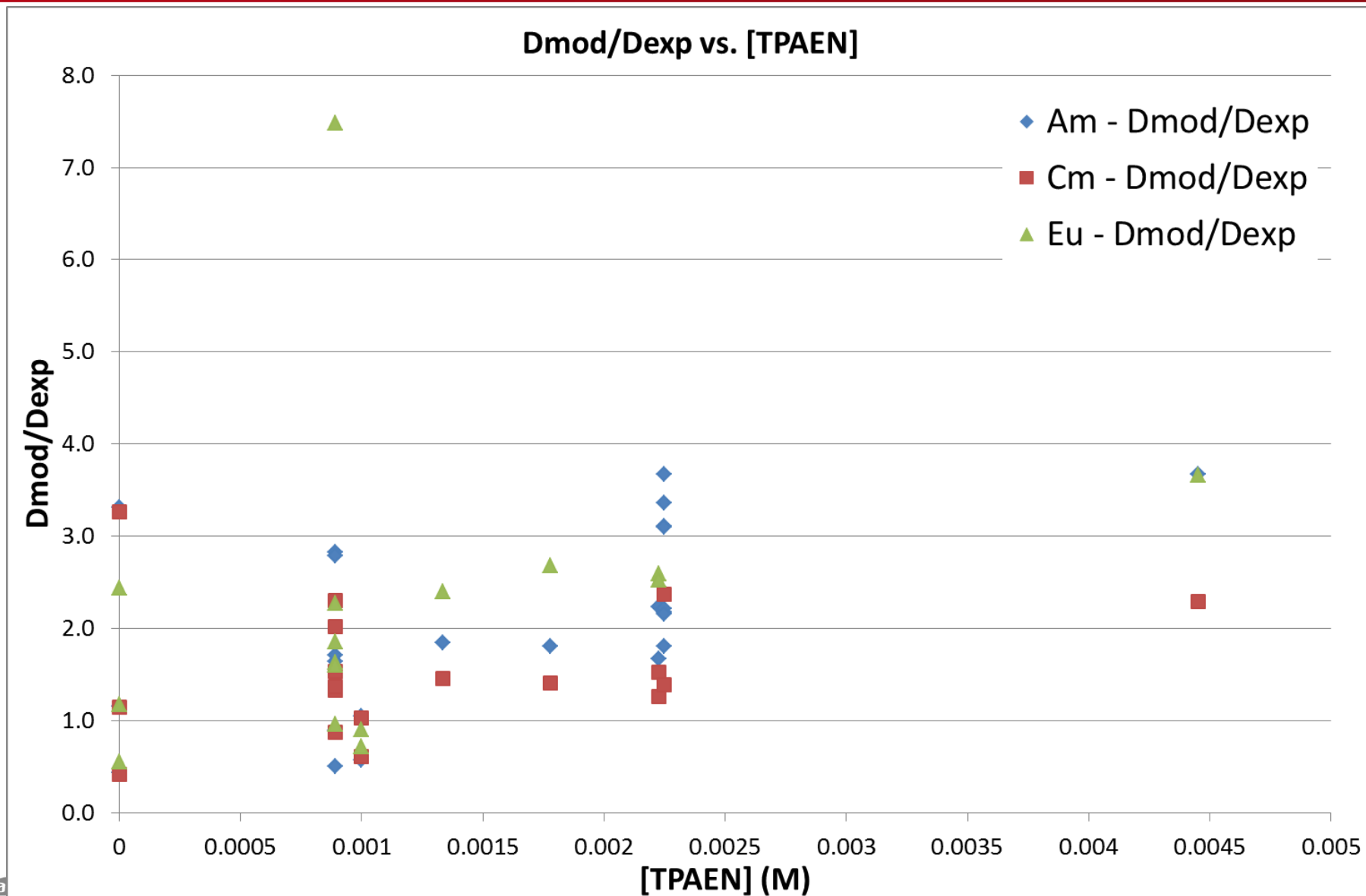
MH_4TPAEN (1:1)

H_6TPAEN
 H_4TPAEN
 H_3TPAEN^-
 H_2TPAEN^{-2}
 $HTPAEN^{-3}$
 $TPAEN^{-4}$

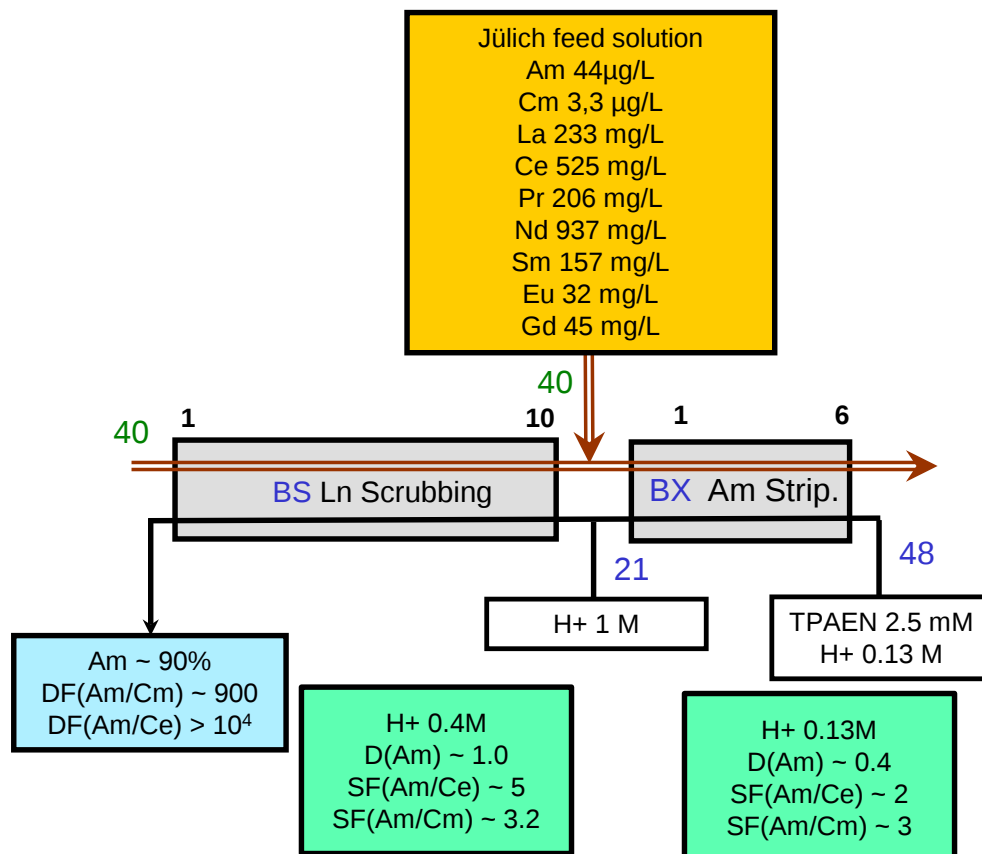


Log(K)	H _n	Am	Cm	La	Ce	Pr	Nd	Sm	Eu	Gd
M(NO ₃) ₃ TODGA (modelling) (2 experiments)	n=1: -0.27 n=2: -1.8 n=3: -3.82	4.0	4.2	3.6	3.3	3.5	3.8	4.5	4.8	4.9
M(H ₄ TPAEN) (modelling) (2 experiments)	n=6: 2.8 n=4: 3.2 n=3: 3.9 n=2: 5.1 n=1: 7.8	6.9	6.6	4.8	5.4	5.4	5.4	5.1	4.9	4.7
M(H ₄ TPAEN) (experimental)	n=6: 2.8 n=4: 3.2 n=3: 3.9 n=2: 5.1 n=1: 7.8	6.1	4.3	2.79	2.57	3.19	3.26	2.97	2.75	-

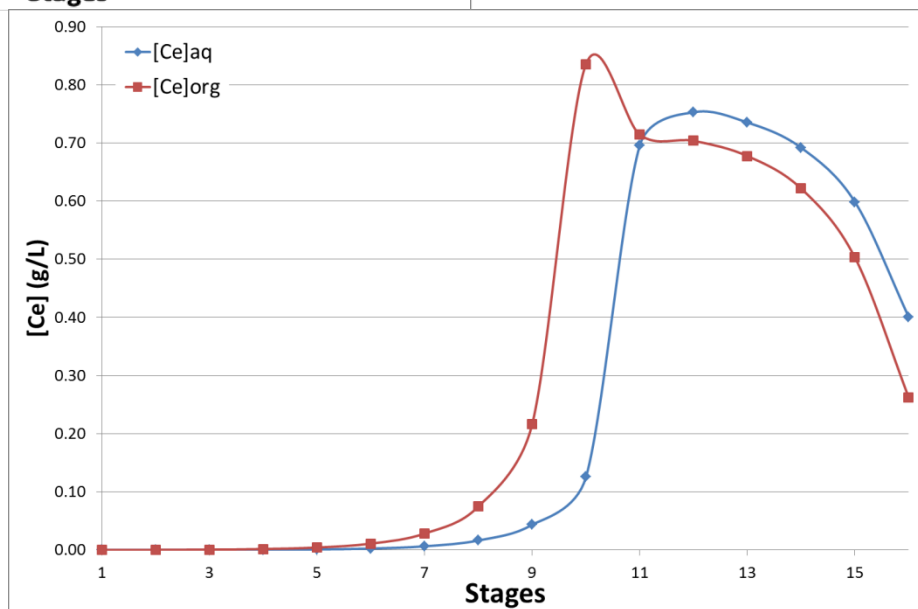
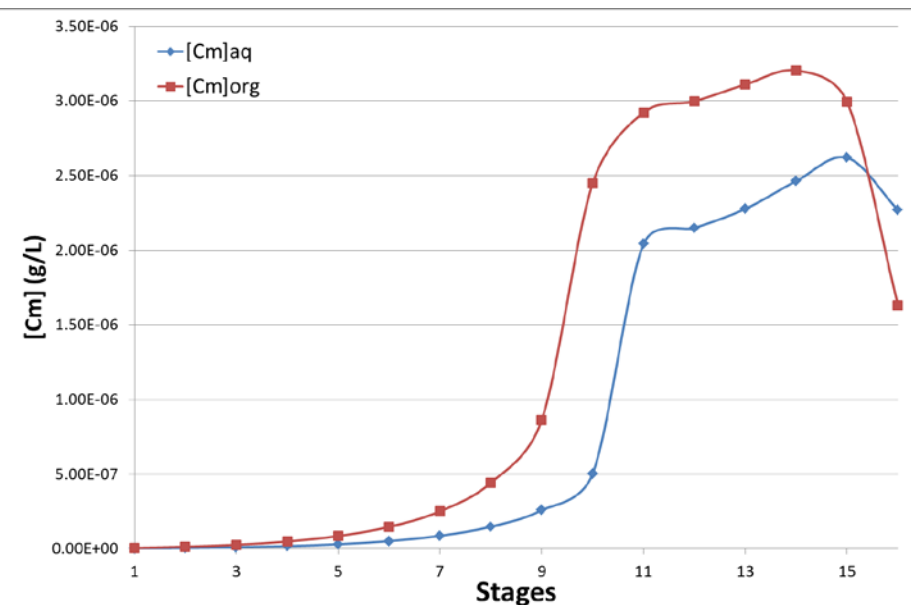
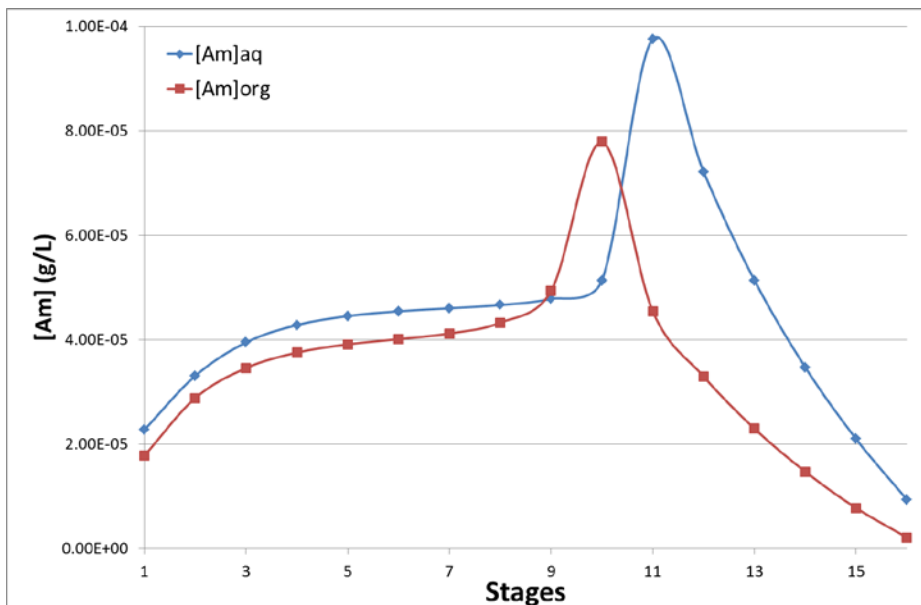




- Use $D(M) = f([H^+])$: BX lower D / BS higher D



Suggestion of a flowsheet



Conclusions

- Difficulties to simulate the last experimental data with macroconcentrations of Ln.
- A first flowsheet made, but necessary to improve this model with new experimental data :
 - Data at equilibrium : $D(M)$, $[M]_{\text{total}}$, $([M]_{\text{aq}}, [M]_{\text{org}})$
 - 2 families of Ln : La $\rightarrow$ Nd and Sm $\rightarrow$ Gd. Experiments with one representative from each family (Ce and Eu?) and then with all elements (Am, Cm, Ln)
 - $[Ln]$: 1-5 mM (BS) to 25 mM (BX)
 - $[H^+]$: 0,1M (BX) to 0.5 M (BS)
 - TPAEN : determine the solubility limit (2.5 mM?)
 - $[TPAEN]$: 0mM (extraction by TODGA alone) to solubility limit of TPAEN

TPAEN = 0 mM	$[Ln] = 1$ mM	$[Ln] = 5$ mM	$[Ln] = 15$ mM	$[Ln] = 20$ mM	$[Ln] = 25$ mM
$[H^+] = 0.1 \text{ M}$					
$[H^+] = 0.15 \text{ M}$					
...					
0.5 M					

- Implementation of kinetics aspects and temperature
- Suggestion of a consolidated flowsheet for Jülich hot test
- Sensitivity studies
- Study to reduce concentrations of La and Ce in loaded solvent (optimization with Am recovery rate) ?



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