



# Modelling approach to the evolution of physicochemical conditions in deep geological repository: alteration of engineered materials and redox control

Olivier Bildstein, P. Thouvenot, J. E. Lartigue, B. Cochepin, I. Munier

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DE LA RECHERCHE À L'INDUSTRIE



# MODELLING APPROACH TO THE EVOLUTION OF PHYSICOCHEMICAL CONDITIONS IN DEEP GEOLOGICAL REPOSITORY: ALTERATION OF ENGINEERED MATERIALS AND CLAYSTONES - REDOX CONTROL

O. Bildstein, P. Thouvenot, J.E. Lartigue

CEA (French Alternative Energies and Atomic Energy Commission)

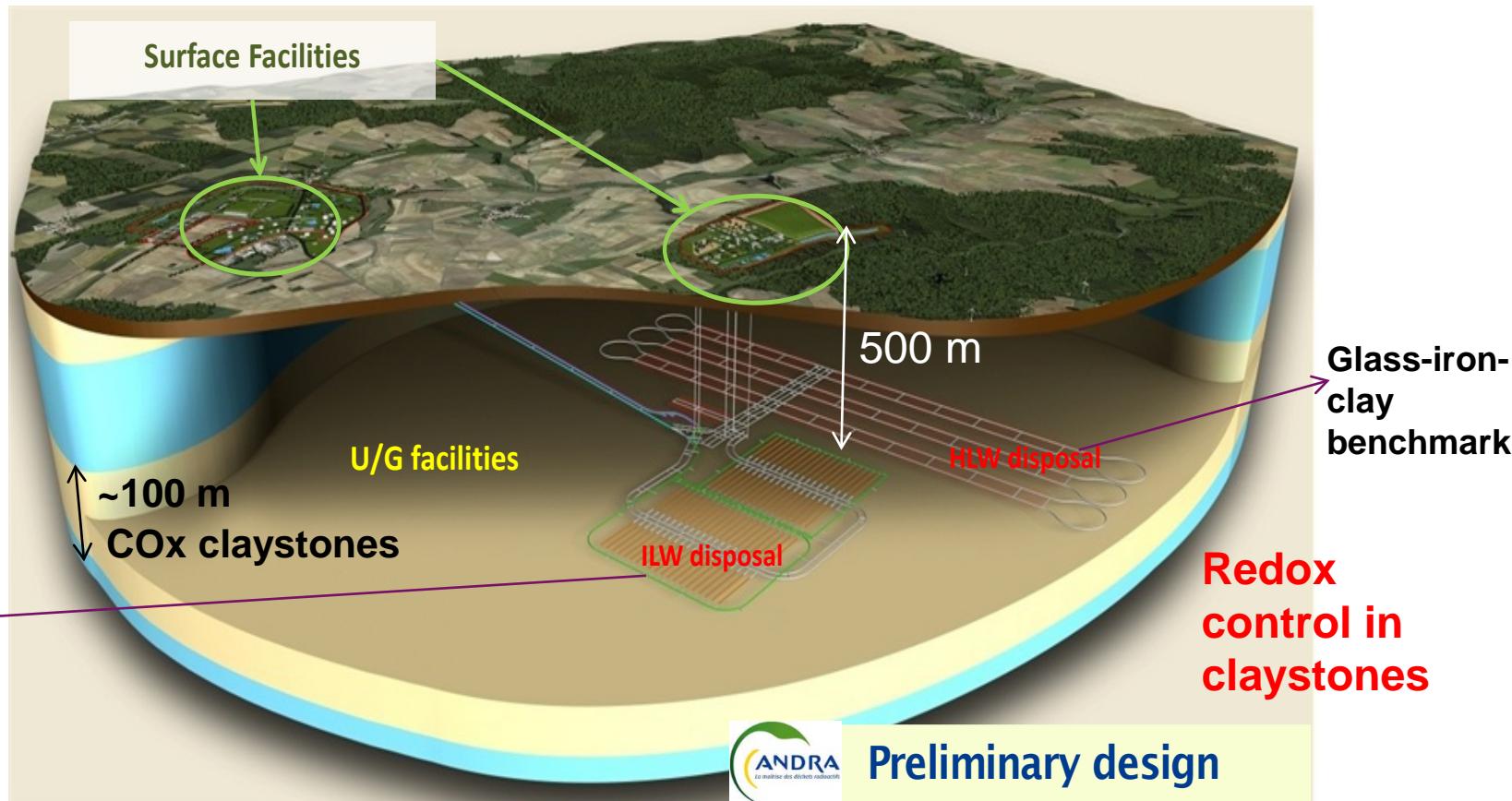
B. Cochebin, I. Munier

Andra (French Radioactive Waste Management Agency)



# DISPOSAL CONCEPT IN A CLAYSTONE FORMATION

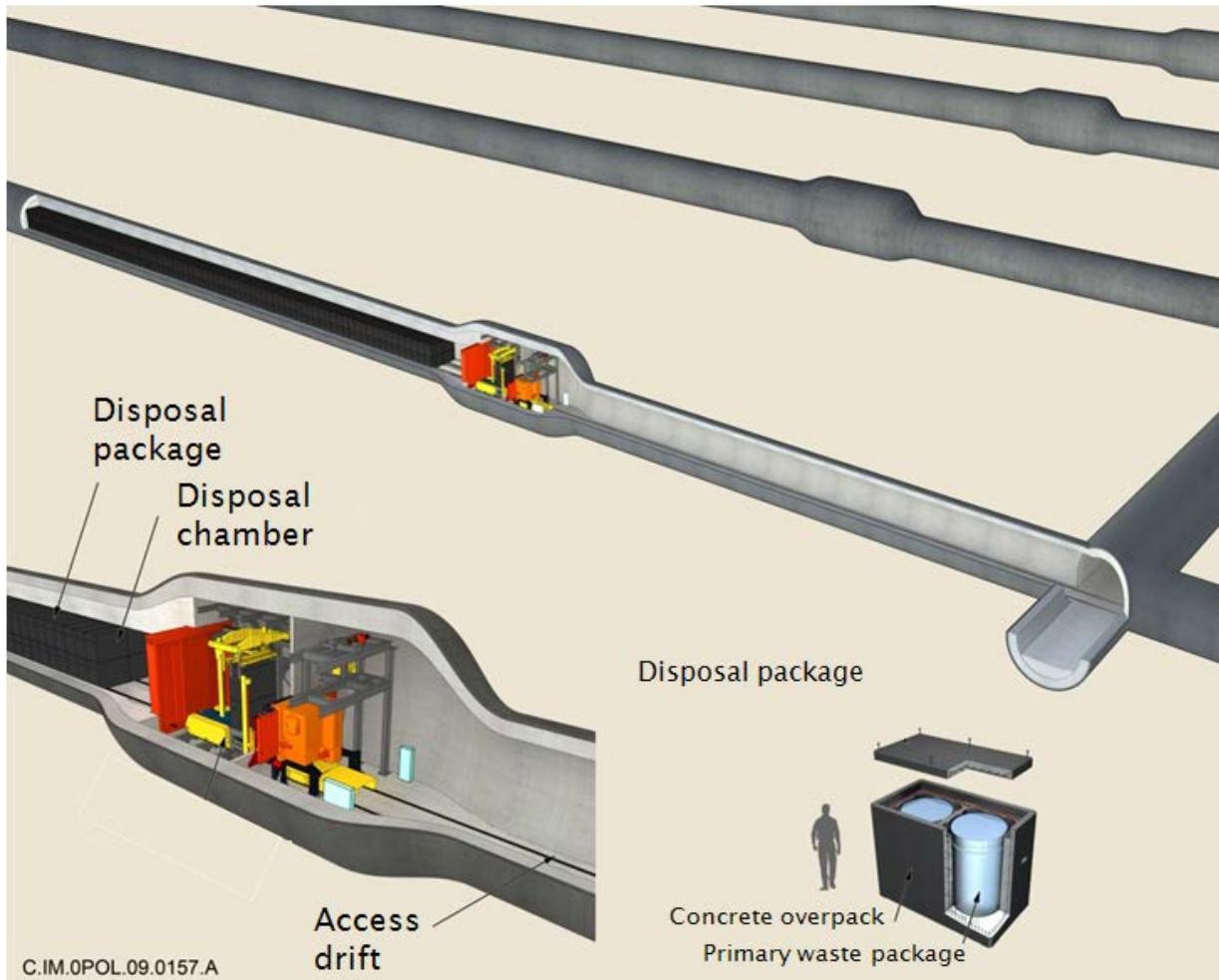
Current design of deep underground repository for high and intermediate level long-lived waste



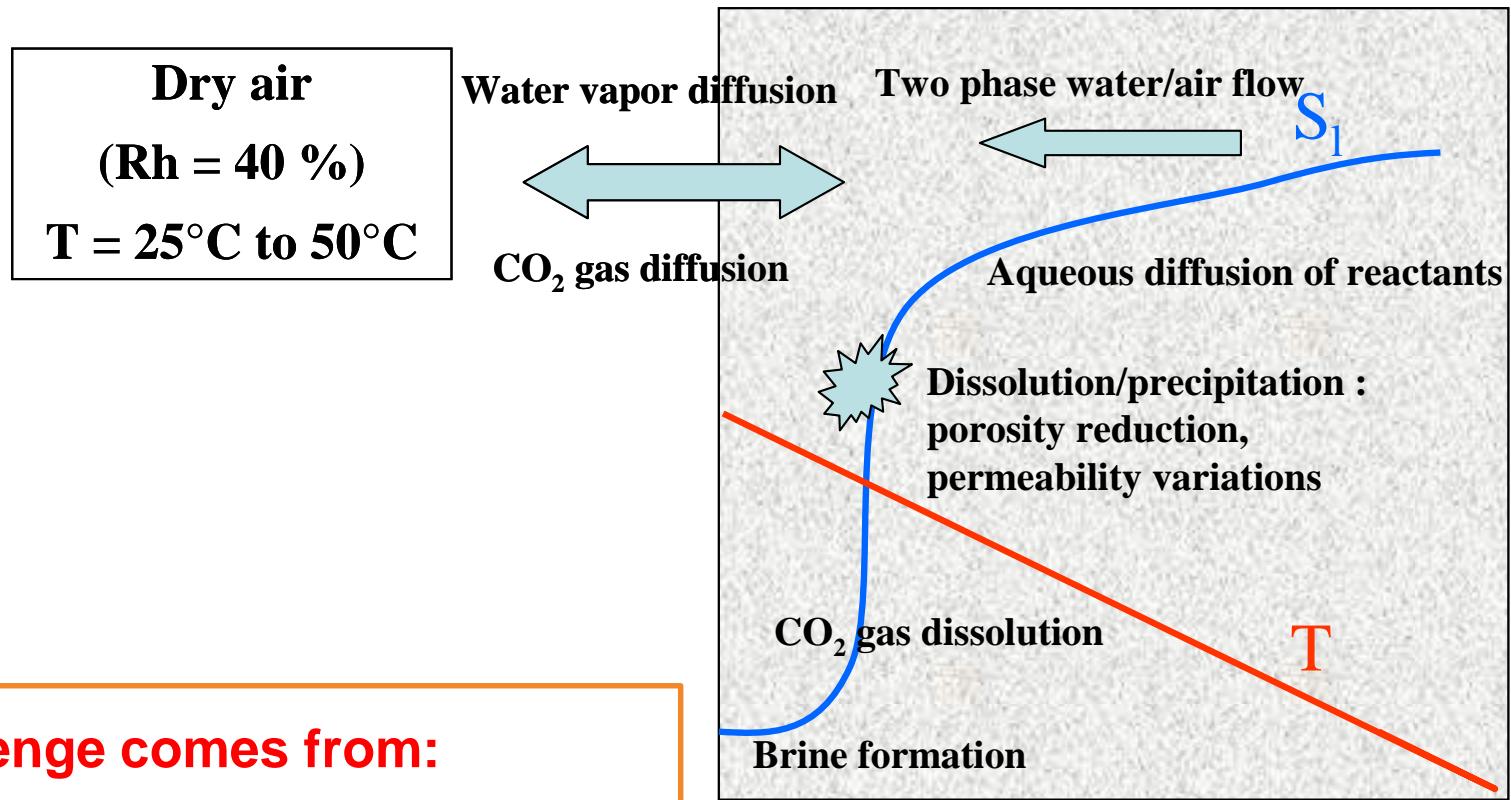
# **Update of the atmospheric concrete carbonation benchmark**

# DESIGN: ILLW CELLS, SHAFTS (AND SEALS), ILLW DISPOSAL OVERPACK

Atmospheric carbonation of overpack during the operating period



# DRYING AND CARBONATION PROCESSES OF ILLW OVERPACK

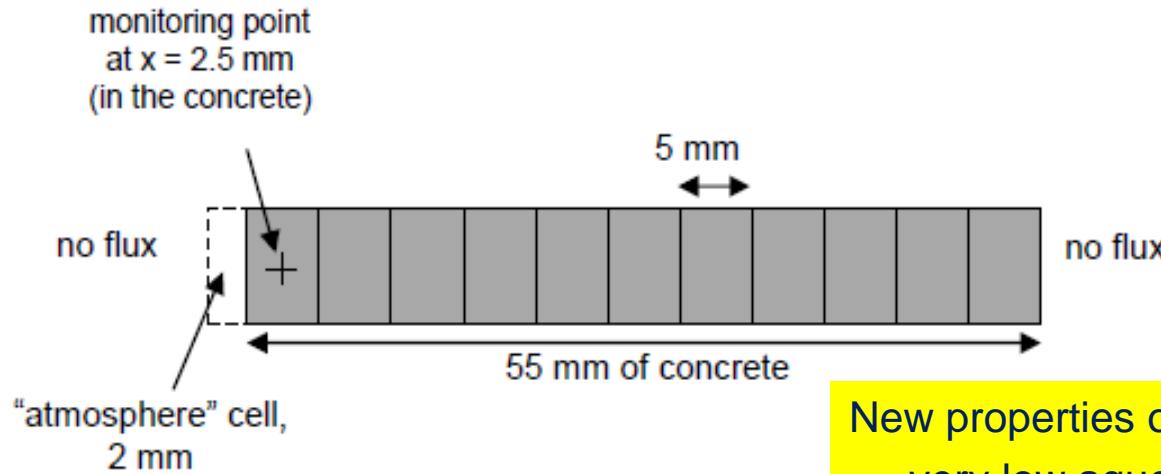


**Major challenge comes from:**

- **$\text{CO}_2$  fast gaseous transport and high reactivity with portlandite and CSH**
- **Coupling capability with « multiphase » flow and transport**

# GEOMETRY + BOUNDARY CONDITIONS

1D Cartesian – 5.5 cm divided in 11 cells (5 mm) for concrete  
1 extra cell for “atmosphere”



New properties of « atmosphere cell » :  

- very low aqueous diffusivity
- $k_{rl} = 0$ ;  $k_{rg} = 1$

## Full multiphase codes :

Toughreact (CEA + T. Xu, JLU)

iCORE (J. Samper, UDC)

HYTEC ??

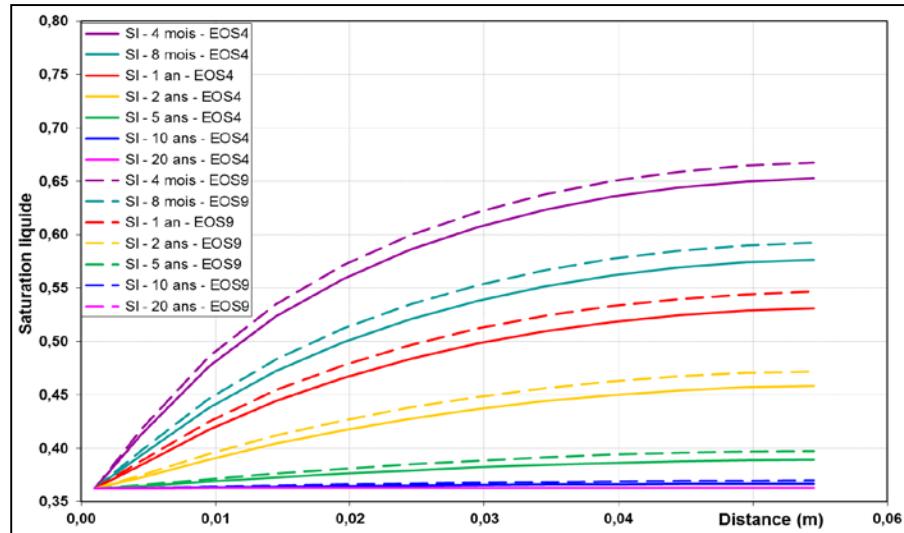
## Drying with Richards' equation :

MIN3P (S. Béa, CONICET ; U. Mayer, UBC)

HYTEC (J. Corvisier, Mines Paristech)

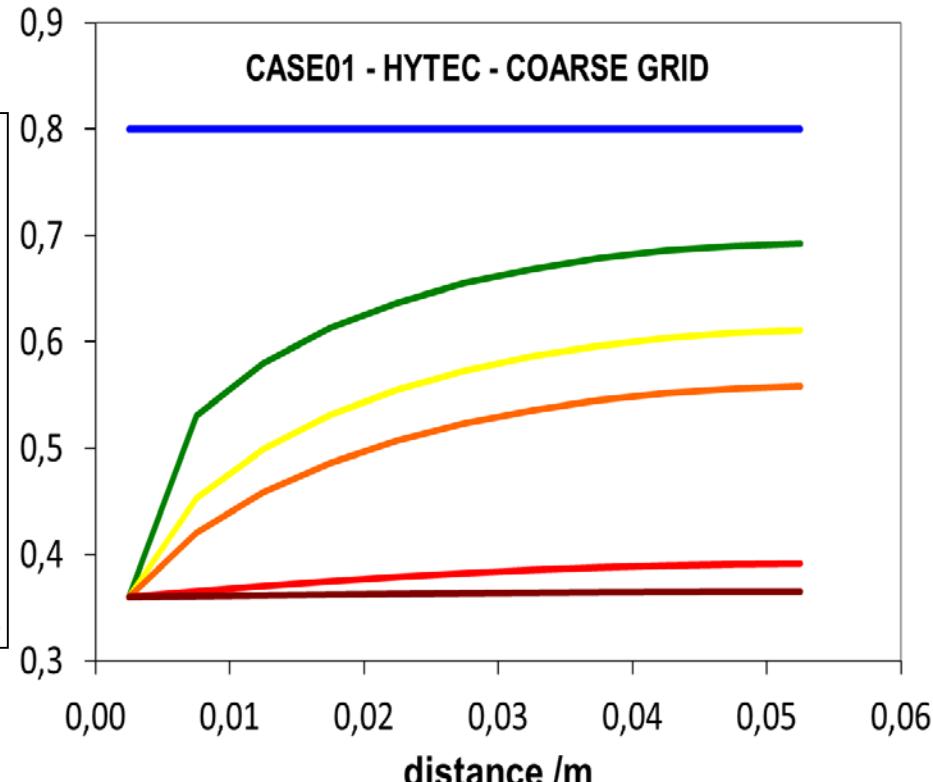
Crunchflow (CEA + C. Steefel, LBNL)

# COMPONENT 1: DRYING RESULTS



**TOUGH2**  
**Full multiphase (EOS4)**  
**Richards (EOS9)**

→ OK to use Richards' equation for benchmarking exercise



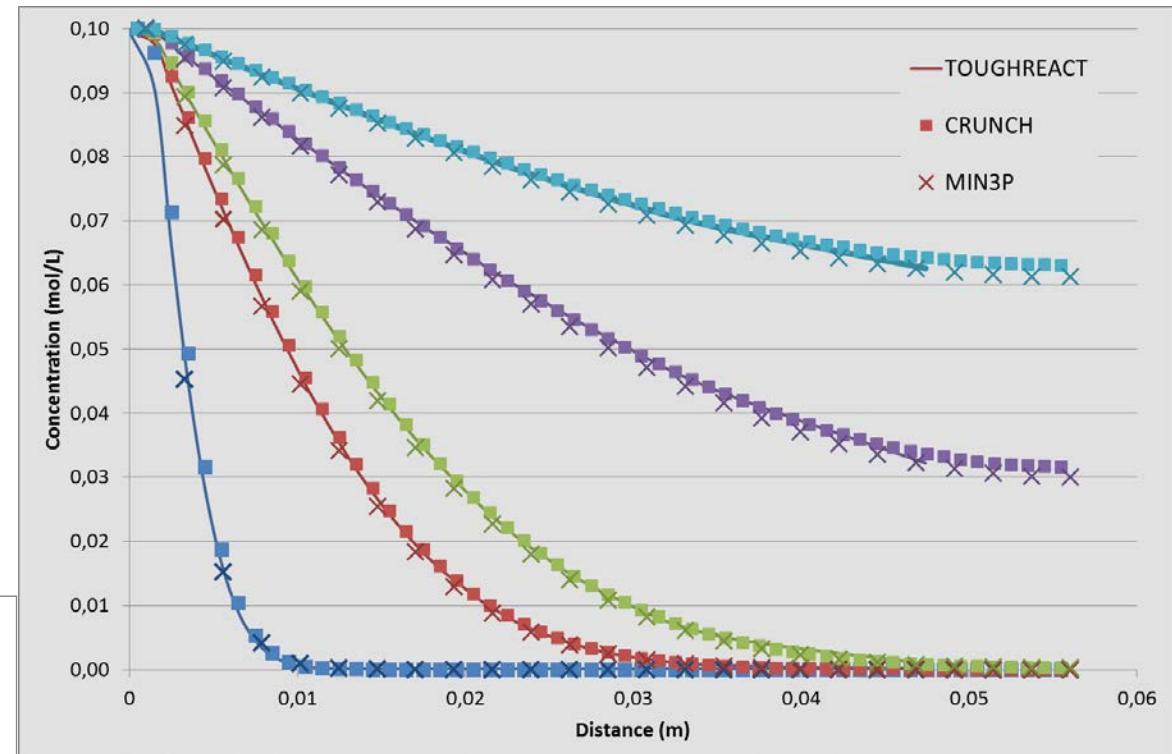
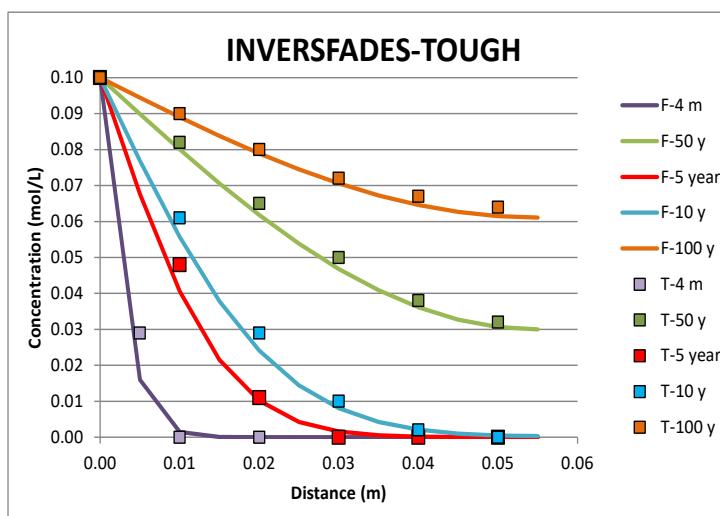
**Hytec (Richards' equation)**

## COMPONENT 2: REACTION TRANSPORT RESULTS AT CONSTANT S<sub>L</sub>

Making sure the same effective diffusion coefficient is used...

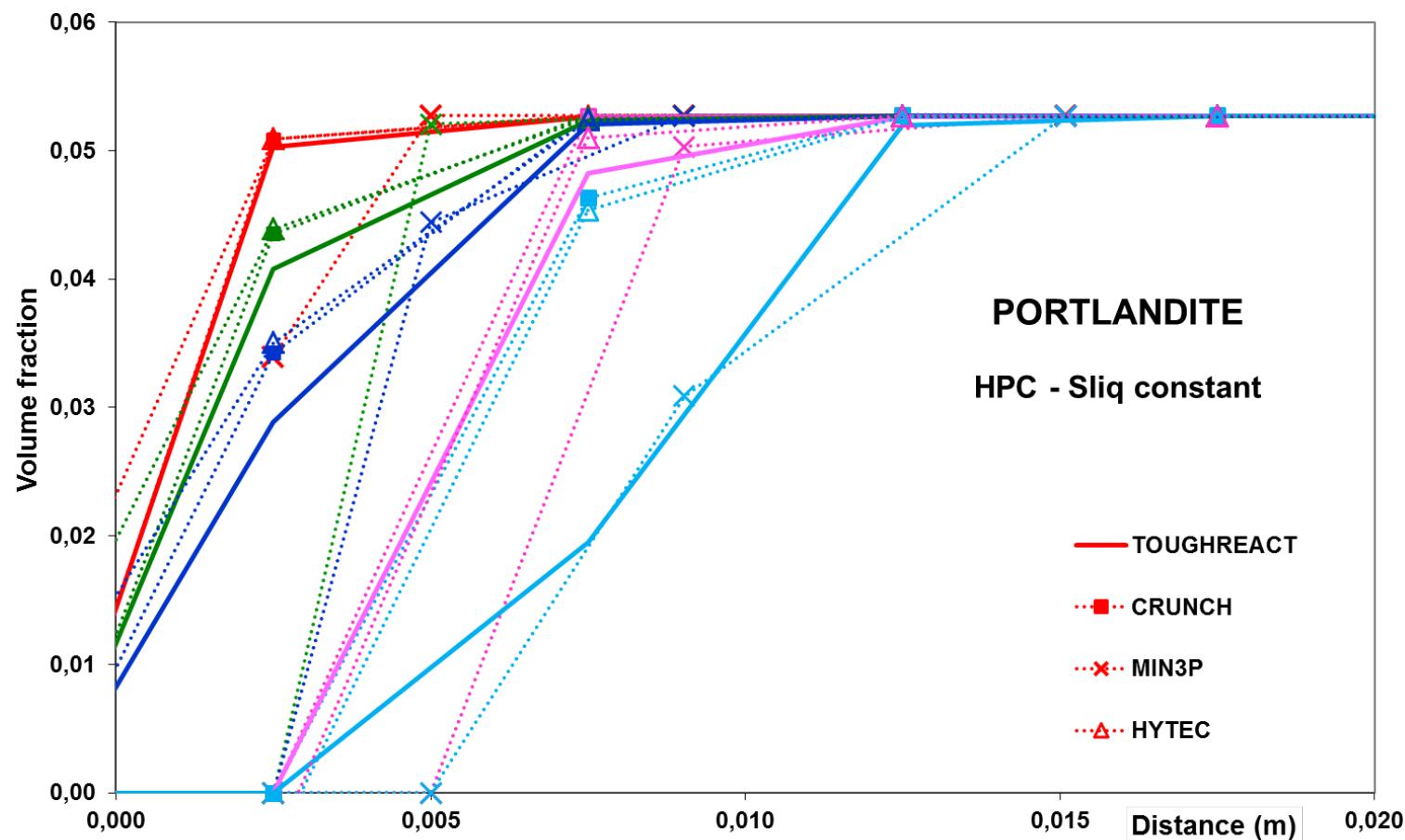
**coupling equation**  
 (Millington-Quirk  
 relationship):

$$D_{eff} = D_0 \omega^a S_l^b$$



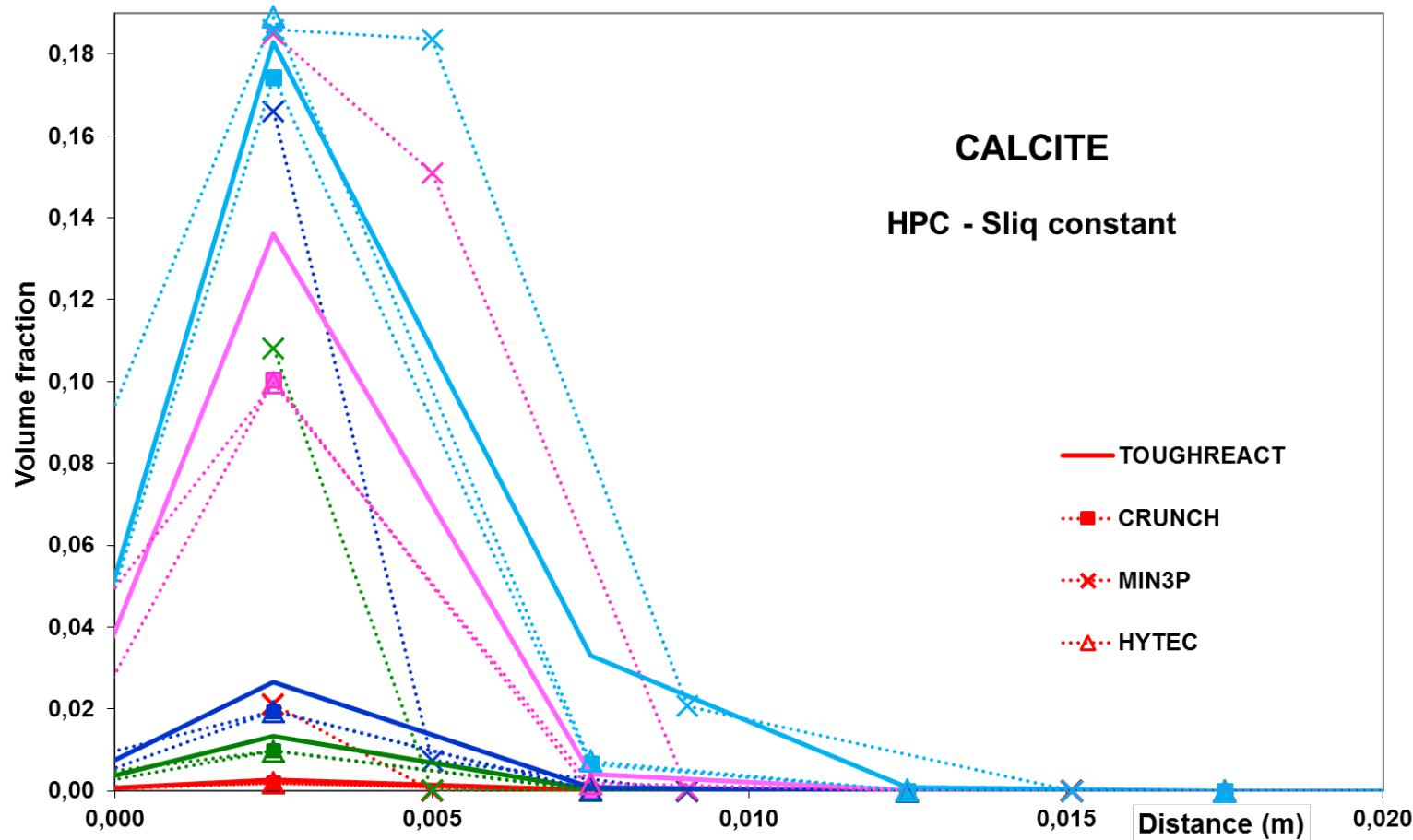
For Crunchflow, b = 3.2 has to be used  
 (instead of b = 4.2 for Toughreact)

# COMPONENT 2B: CONCRETE CARBONATION AT CONSTANT $S_L$



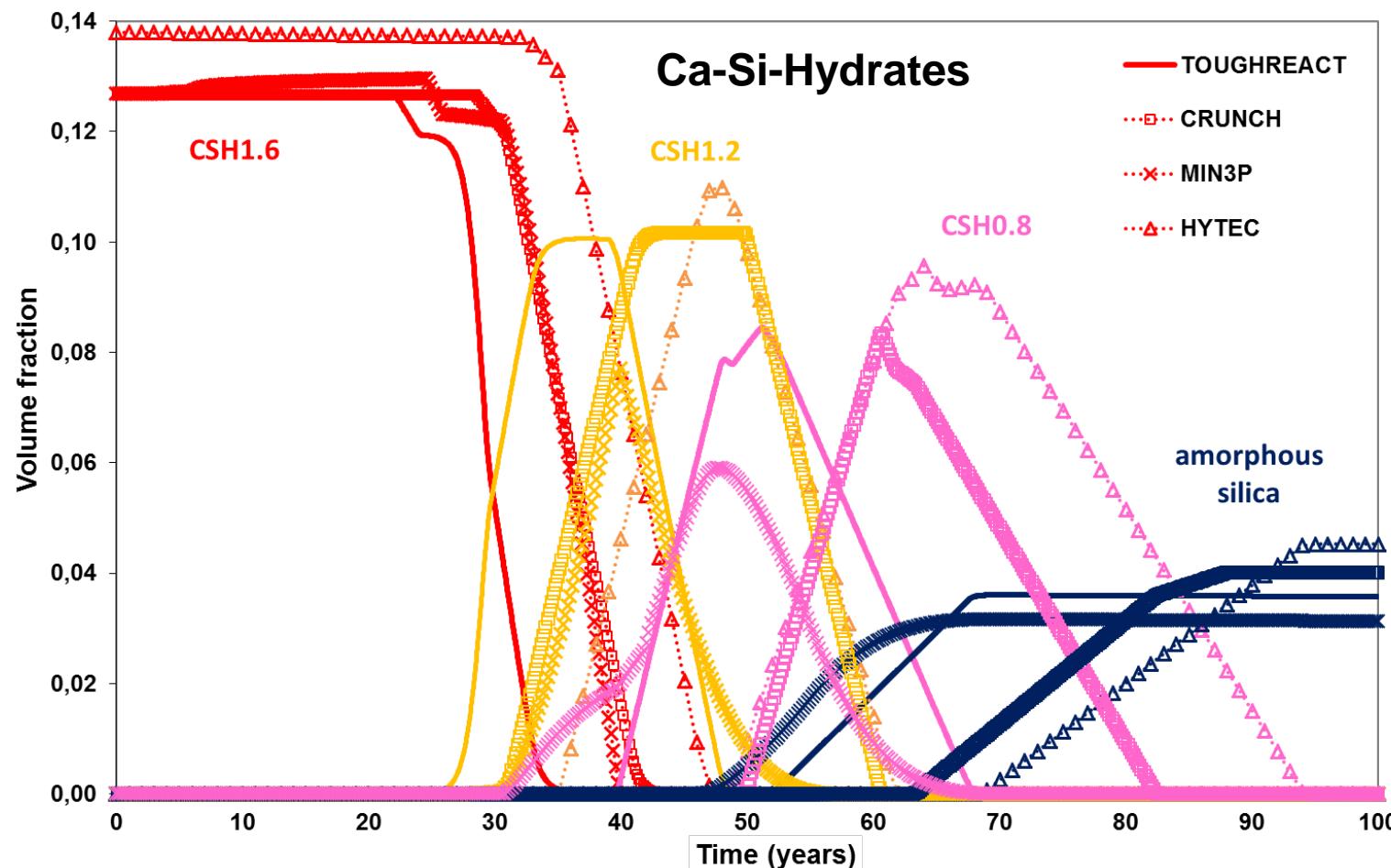
Carbonation front is similar, but the size of grid cells limits precise comparison

# COMPONENT 2B: CONCRETE CARBONATION AT CONSTANT $S_L$



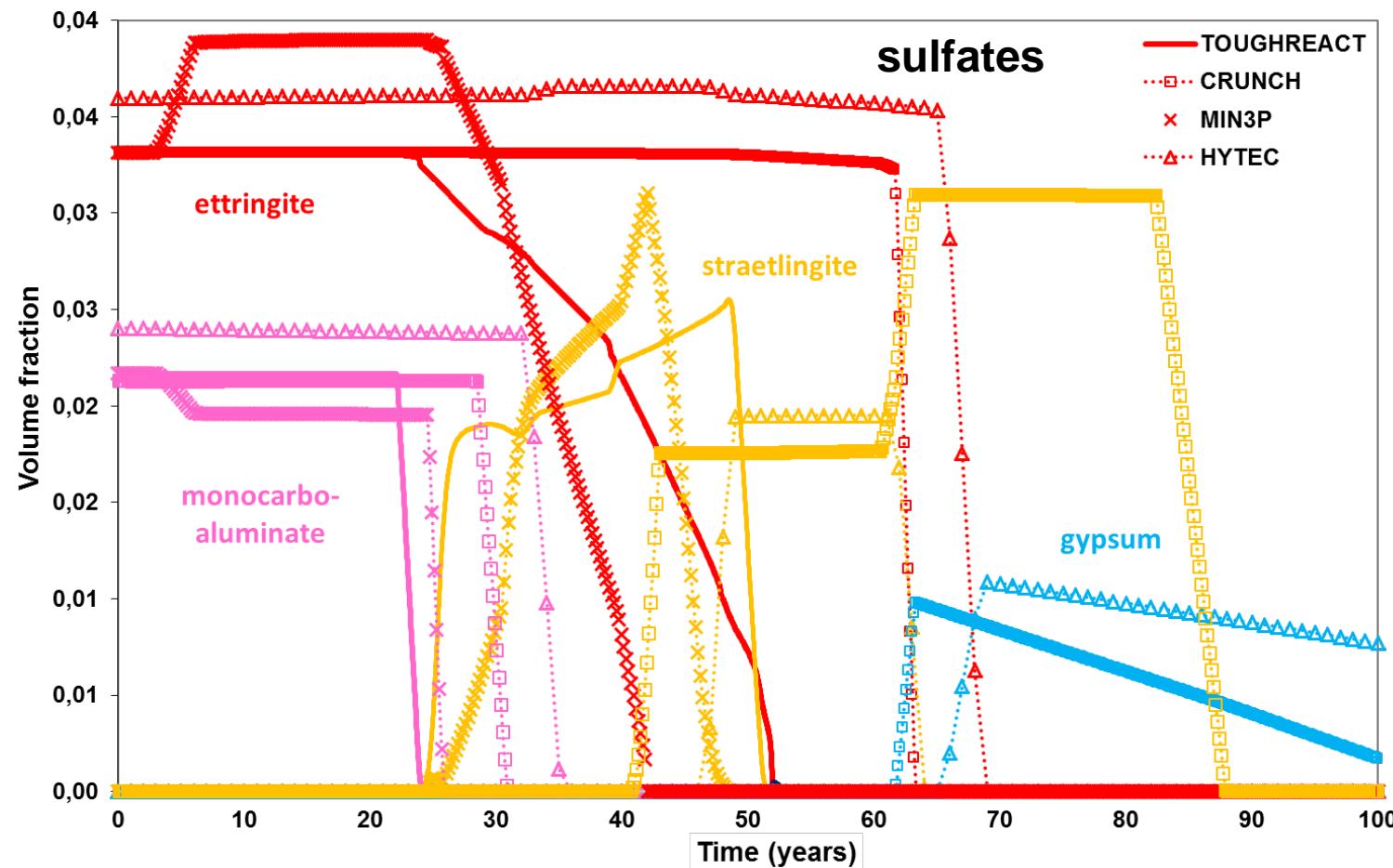
Calcite precipitation front is similar (MIN3P a little ahead of time/distance)

# COMPONENT 2B: CONCRETE CARBONATION AT CONSTANT S<sub>L</sub>



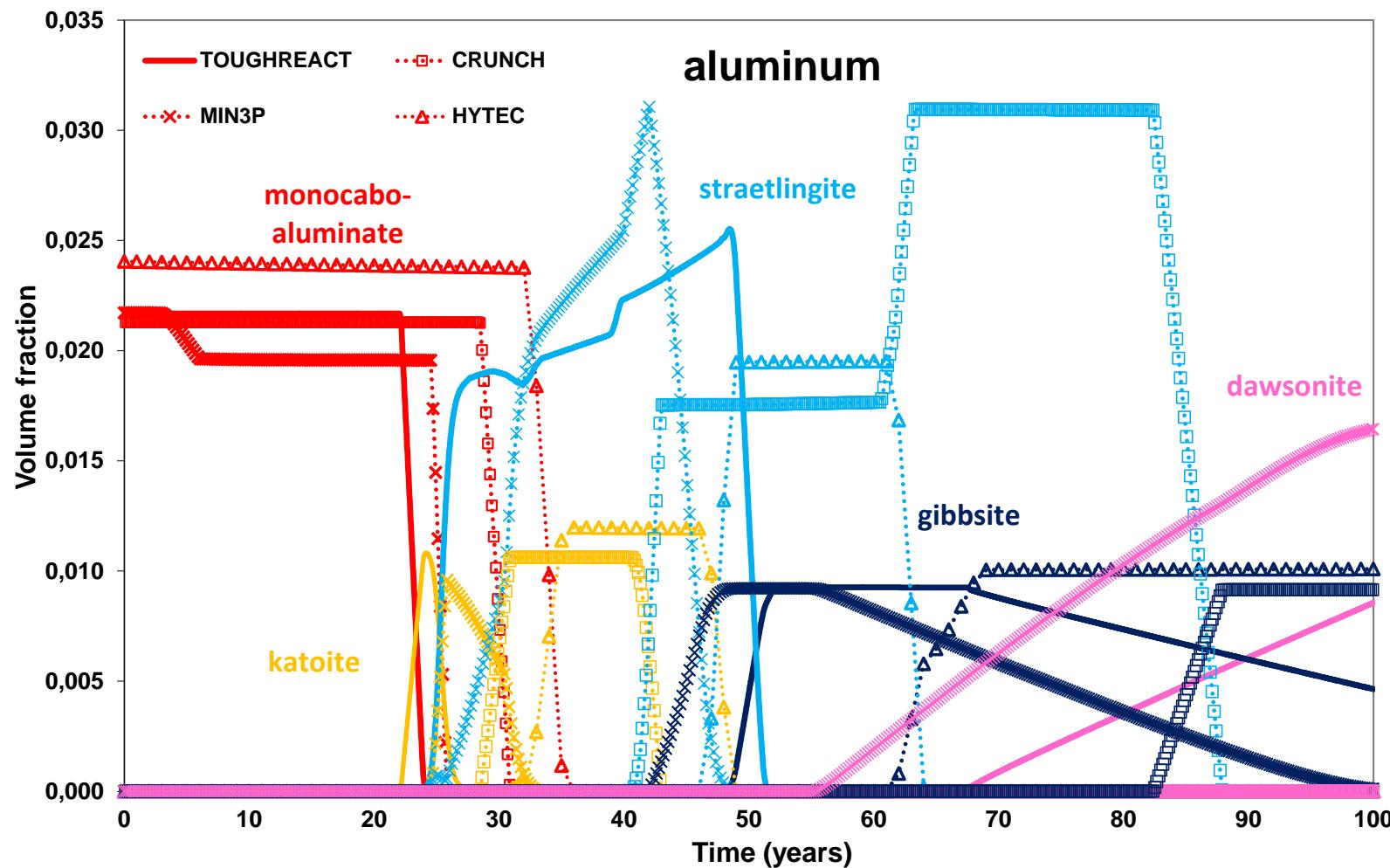
Same mineral paragenesis but timing not exactly the same for all codes

# COMPONENT 2B: CONCRETE CARBONATION AT CONSTANT S<sub>L</sub>



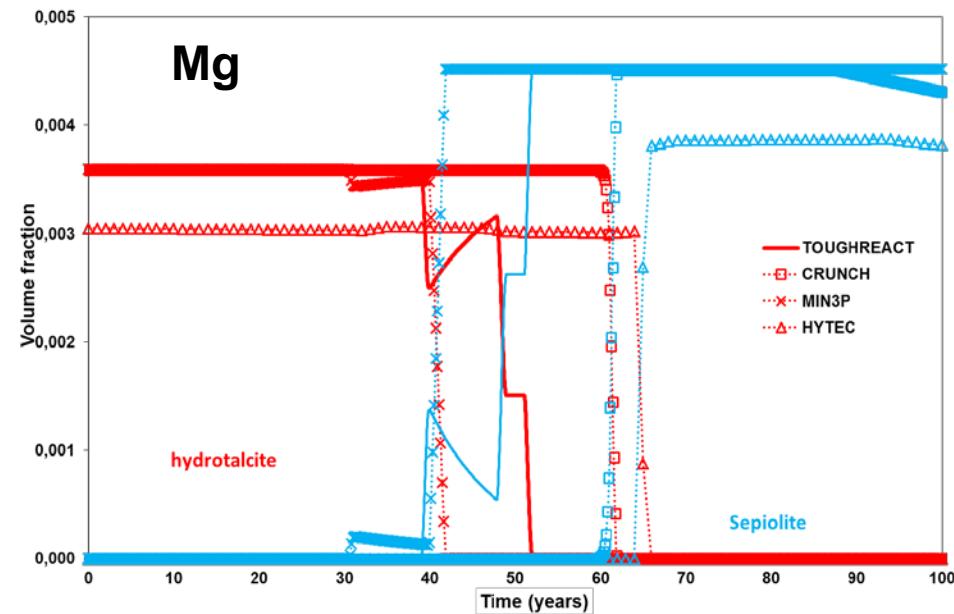
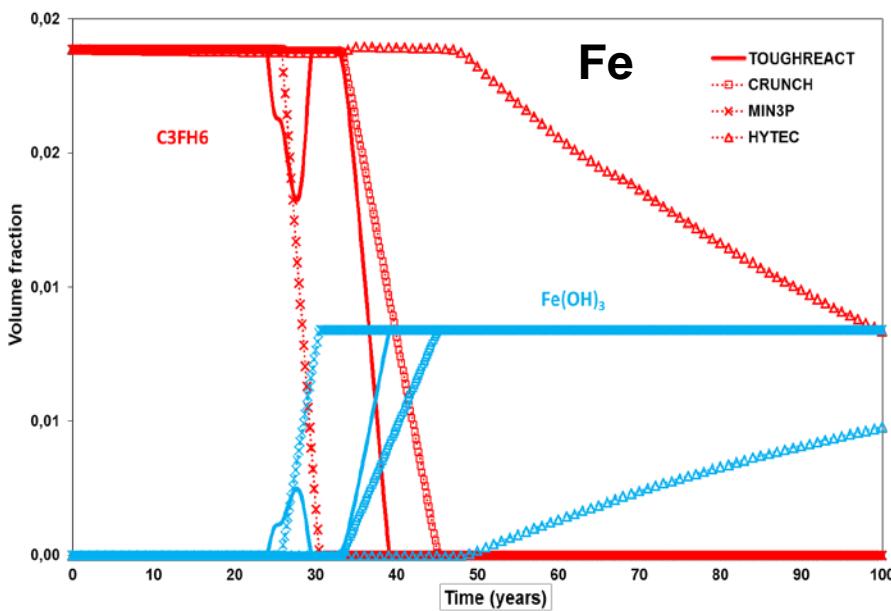
Precipitation of gypsum in the simulation with Crunchflow and Hytec

# COMPONENT 2B: CONCRETE CARBONATION AT CONSTANT S<sub>L</sub>



Dawsonite does not precipitate with Crunchflow and Hytec  
 Straetlingite more persistent with Crunchflow

# COMPONENT 2B: CONCRETE CARBONATION AT CONSTANT S<sub>L</sub>

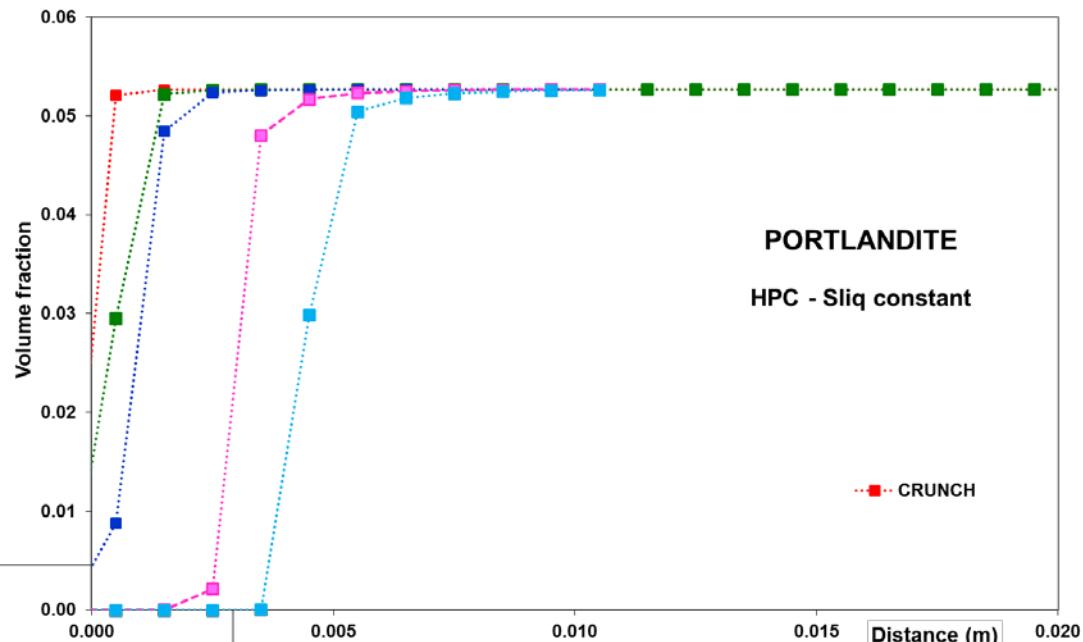
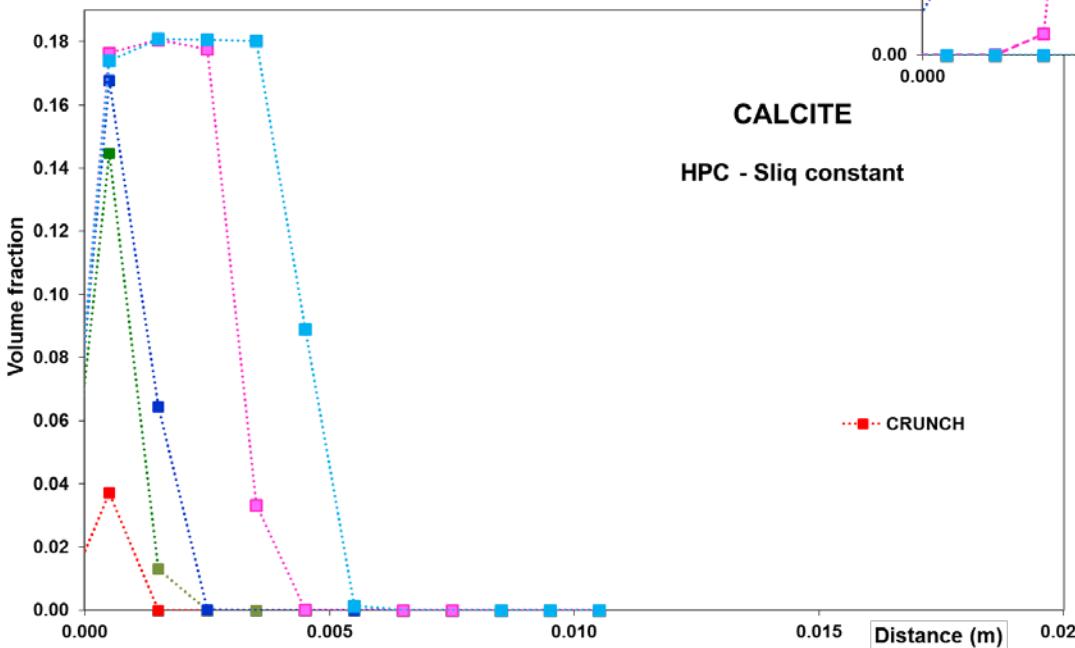


Same mineral paragenesis but timing not exactly the same for all codes

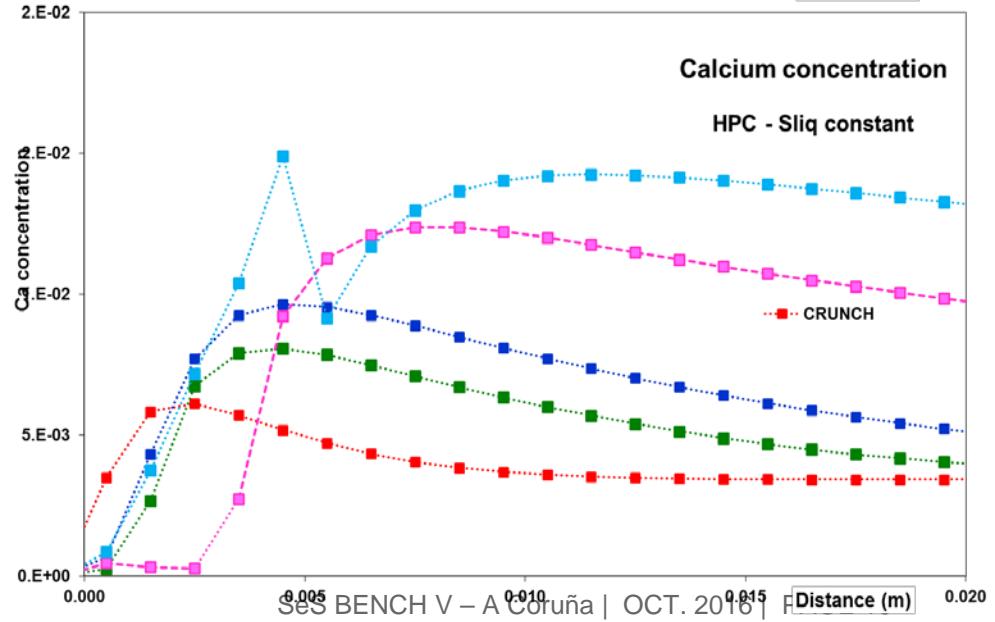
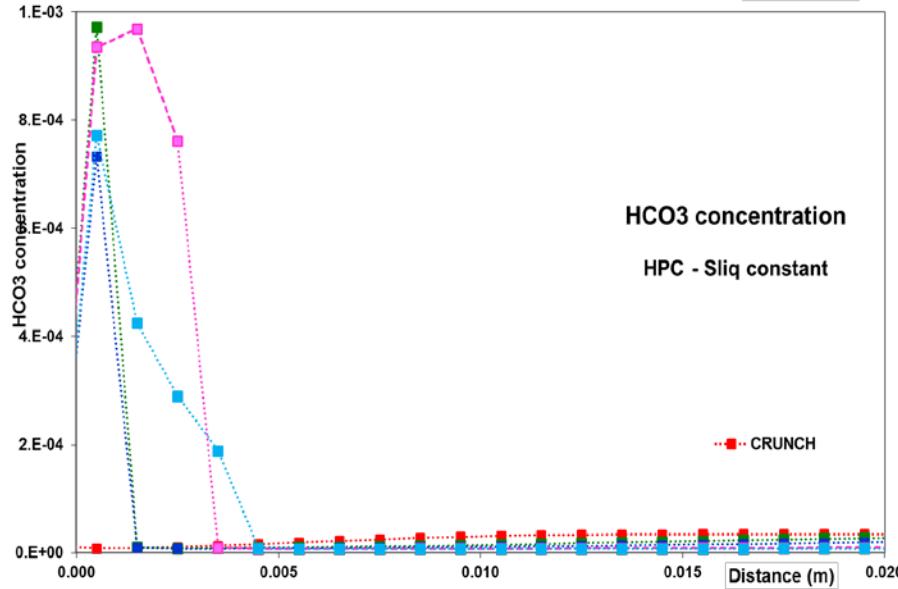
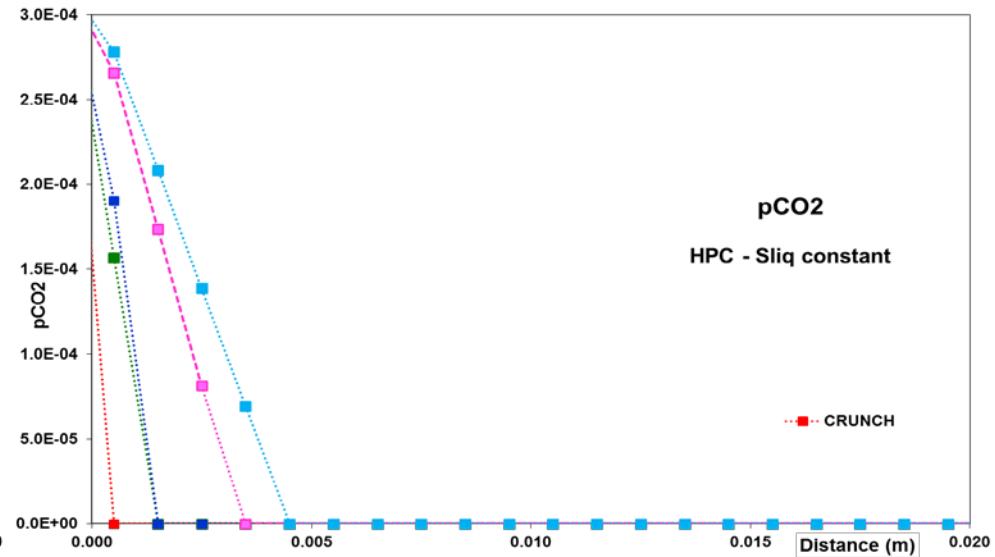
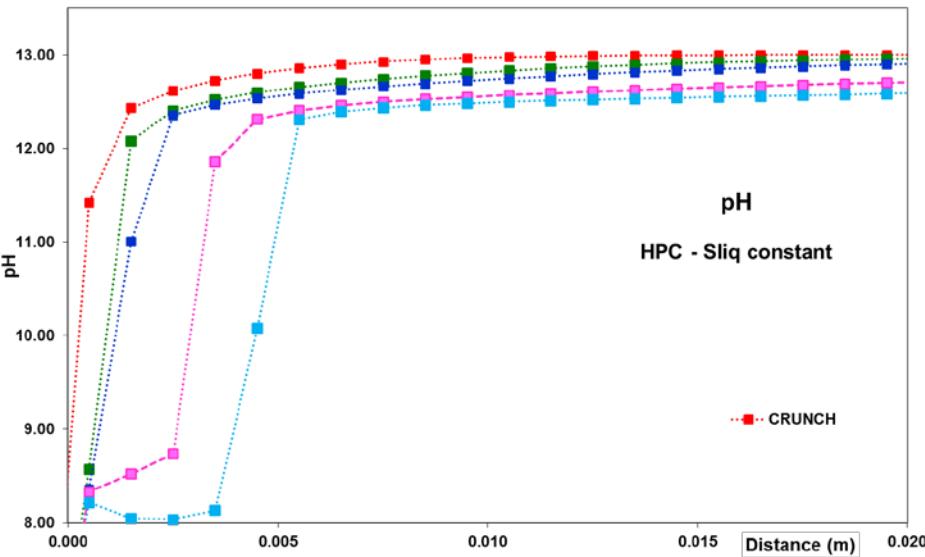
# COMPONENT 2A: PORTLANDITE-CALCITE SYSTEM AT CONSTANT S<sub>L</sub>

The discrepancies observed in the complex prompted a simpler simulation case (component 2A) with only

Portlandite and Calcite



# COMPONENT 2A: PORTLANDITE-CALCITE SYSTEM AT CONSTANT S<sub>L</sub>



# CONCRETE CARBONATION SUMMARY

## ✓ Concrete carbonation exercise

- ✓ differences between codes do not seem to be linked to the grid size or coupling method
- ✓ differences in results attributable to transport in the gas phase?
- ✓ CPU concerns: no SIA → small time steps → CPU times go up !

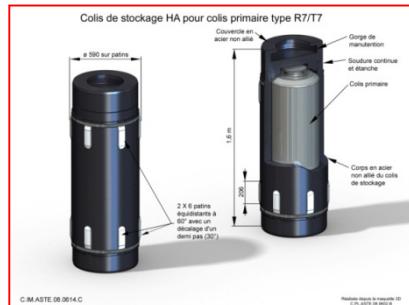
## ✓ Component 2a with simplified chemistry

## ✓ Component 3 with fully coupled drying+carbonation only with Toughreact

## ✓ New component : variable porosity?

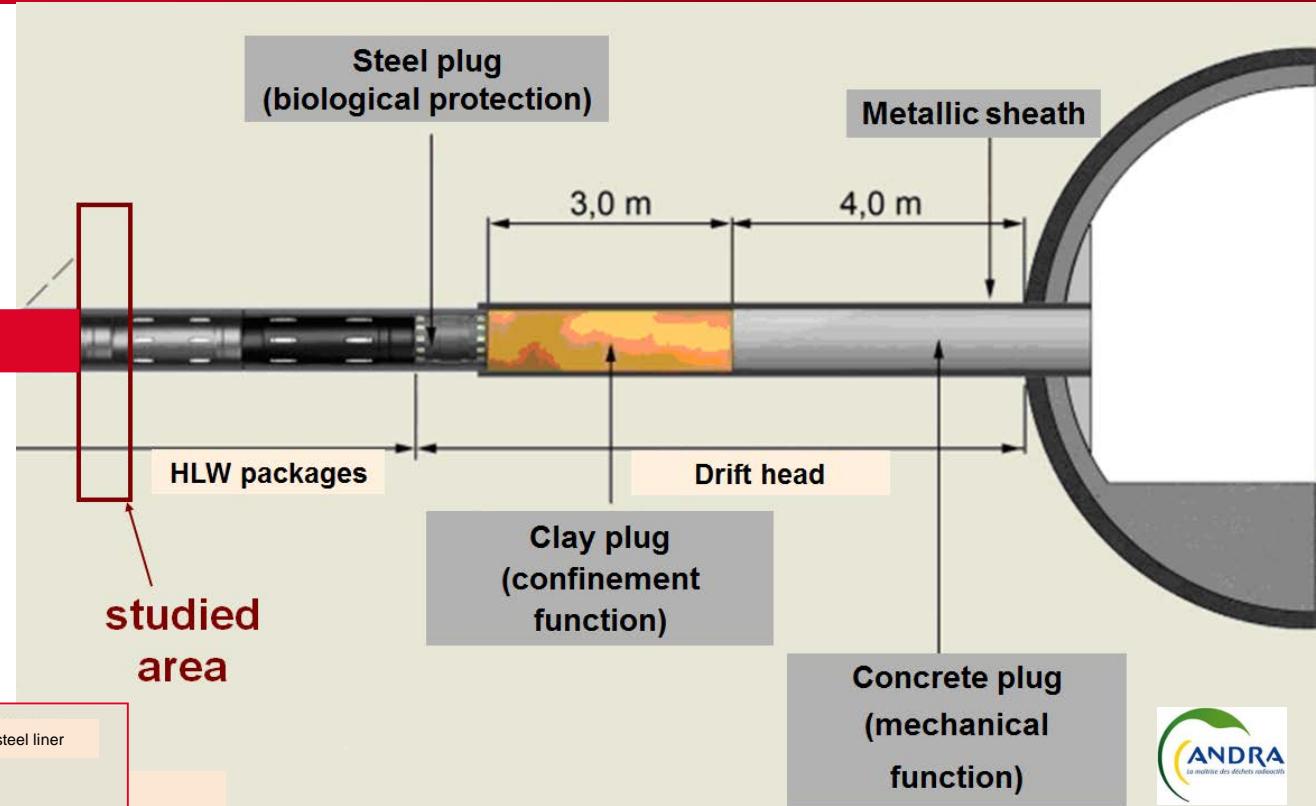
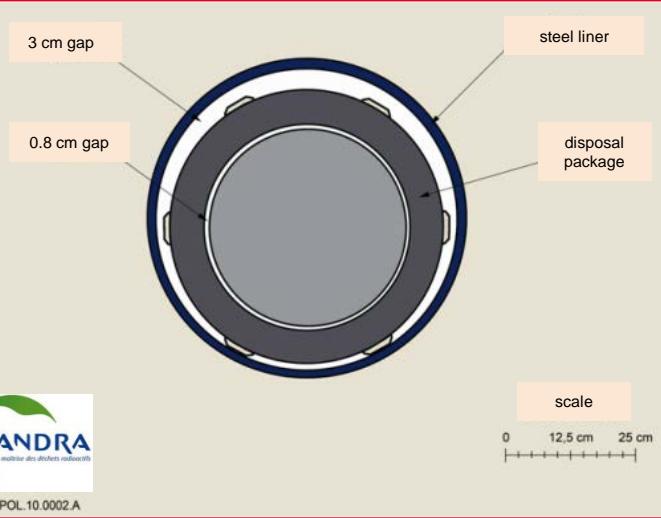
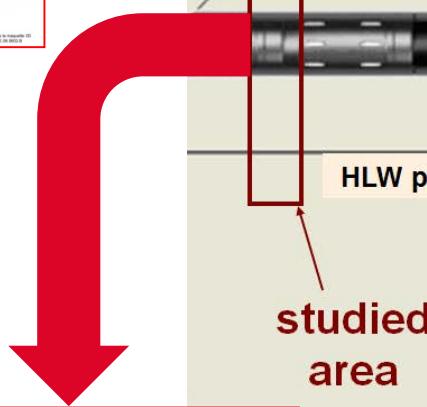
# Glass & steel corrosion and redox control in claystones

# HLW DISPOSAL CELL



Vitrified waste packages

Cross section



- different types of material in physical contact, technological gaps
- long term calculations of geochemical evolution (100 000 years)

# GEOMETRY AND TRANSPORT PROPERTIES

- 1D radial domain
- transport: diffusion only
- water saturated, constant porosity
- isothermal conditions
- $\text{H}_2(\text{g})$  from anoxic corrosion
- $\text{pH}_{2(\text{max})} = 60 \text{ bar}$

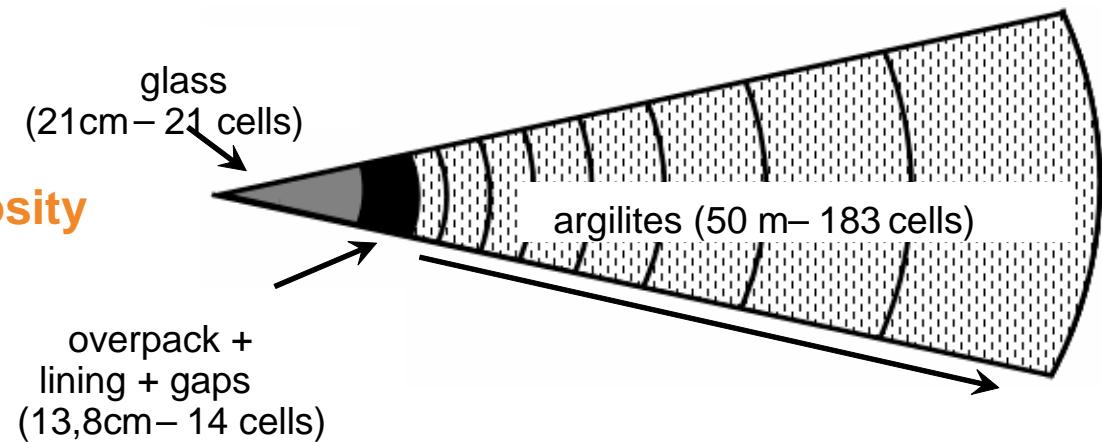
- glass
 

$\Phi = 0.42 \text{ m}, H = 1 \text{ m}$   
porosity = 0.12
- metallic components
 

total thickness = 0,095 m,  
porosity = 0.25
- connected fractured zone
 

$0.4 * \text{excavation diameter} = 0.268 \text{ m}$   
porosity = 0.20;  $D_{\text{eff}}(25^\circ\text{C}) = 5.2 \cdot 10^{-11} \text{ m}^2/\text{s}$
- undisturbed claystone (50 m)
 

porosity = 0.18;  $D_{\text{eff}}(25^\circ\text{C}) = 2.6 \cdot 10^{-11} \text{ m}^2/\text{s}$



**Major challenge comes from:**

- **highly reactive system  
(strong pH and redox perturbation)**
- **complex geochemical system  
(15 chemical elements, 80 aqueous species, 60 minerals)**

# EXISTING BENCHMARK SUB-COMPONENTS

## Component 1: iron corrosion only (45 000 yrs)

- magnetite, Ca-siderite, and greenalite dominate  
(oxide) (carbonate) (silicate)
- also smaller amounts of aluminosilicates  
(nontronites and saponites)
- **POROSITY CLOGGING (not taken explicitly into account)**

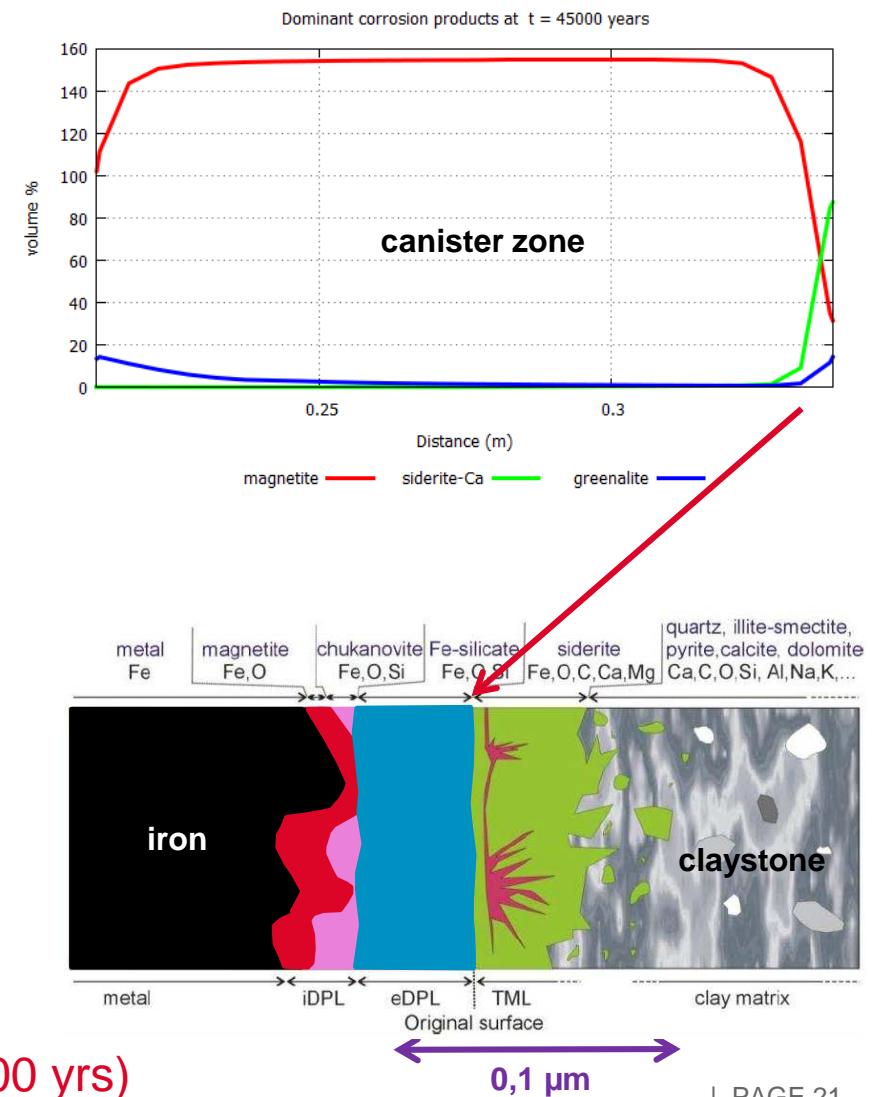
### modeling vs. experimental results

iron/claystone at 90°C for 1 year

- small amount of magnetite
- siderite(-Ca), Fe-silicates

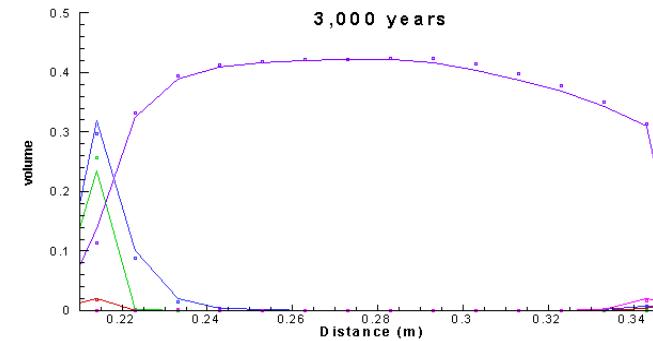
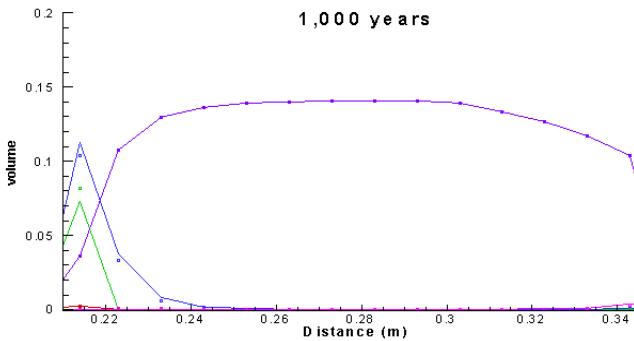
→ more phenomenological model for corrosion

## Component 2: iron corrosion + glass alteration (100 000 yrs)

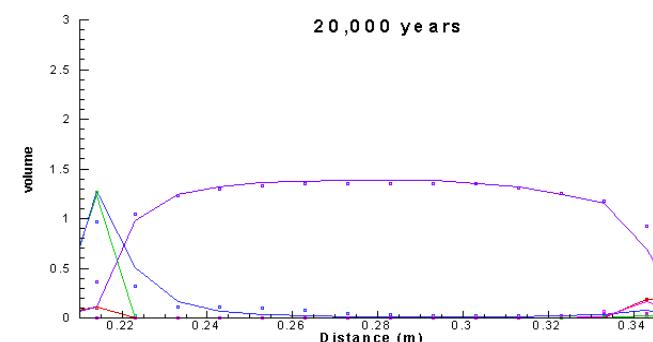
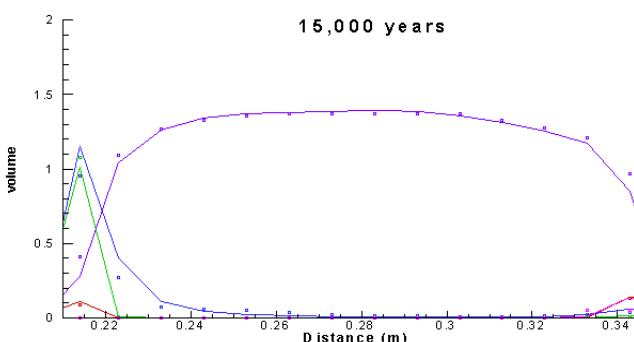
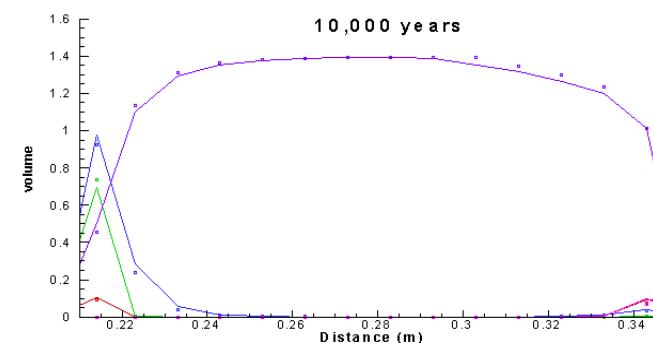
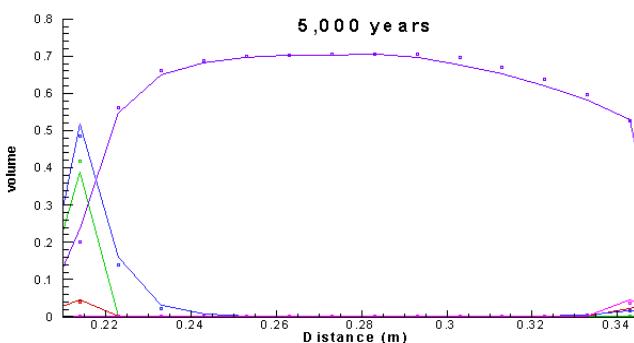


# COMPONENT 1: RESULTS IN THE BASE CASE

ONLY 2 CODES : MIN3P-Crunchflow (a very good agreement is obtained!) ...



**in the iron zone**

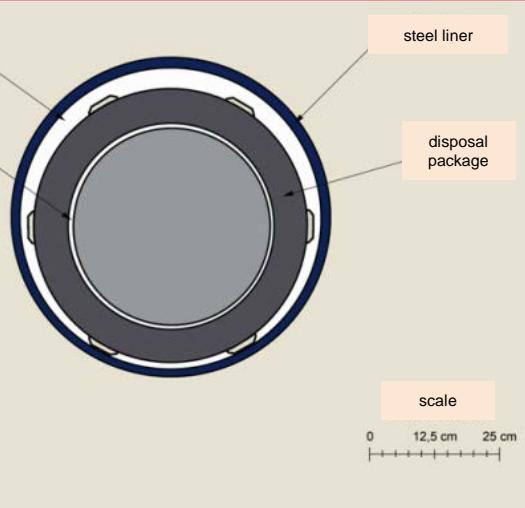
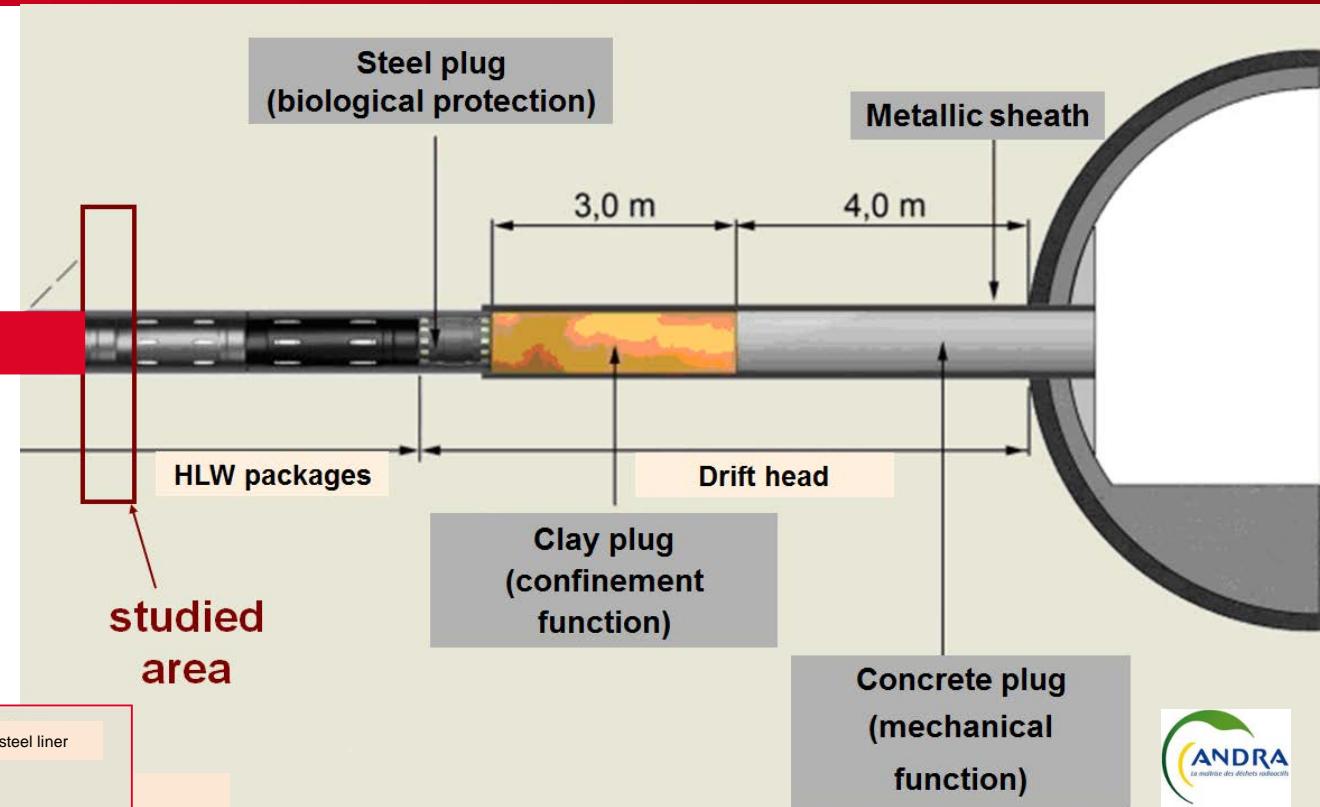


- Daphnite\_14A - crunchflow
- Fe-Saponite-Na - crunchflow
- Greenalite - crunchflow
- Magnetite,beta - crunchflow
- Pyrrohite-alpha - crunchflow
- Daphnite\_14A - MIN3P
- Greenalite - MIN3P
- Fe-Saponite-Na - MIN3P
- Pyrrohite-alpha - MIN3P
- Magnetite,beta - MIN3P

# CORROSION IN HLW DISPOSAL CELL



Vitrified waste packages



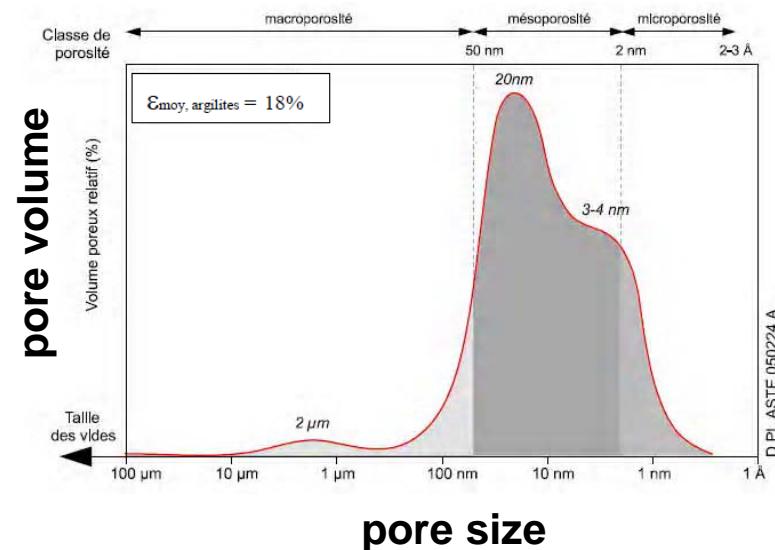
## RELATED TOPICS

- production of hydrogen: how reactive is it?
- redox in claystones: who is in control?
- how is corrosion represented in reactive transport codes?

➤ reactivity of H<sub>2</sub> in claystones  
(in tiny 20 nm connected pores)

- only at interfaces in repository
- redox control in claystones?
- RN sorption/migration?
- porosity clogging

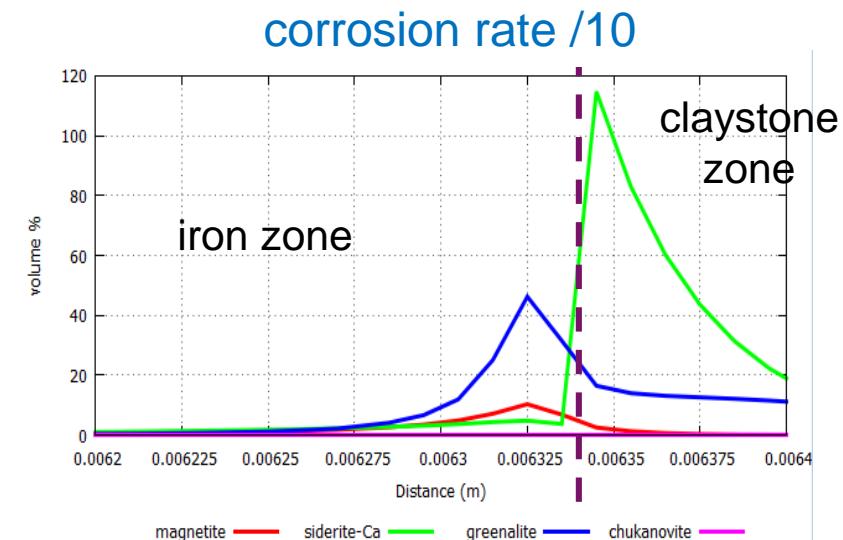
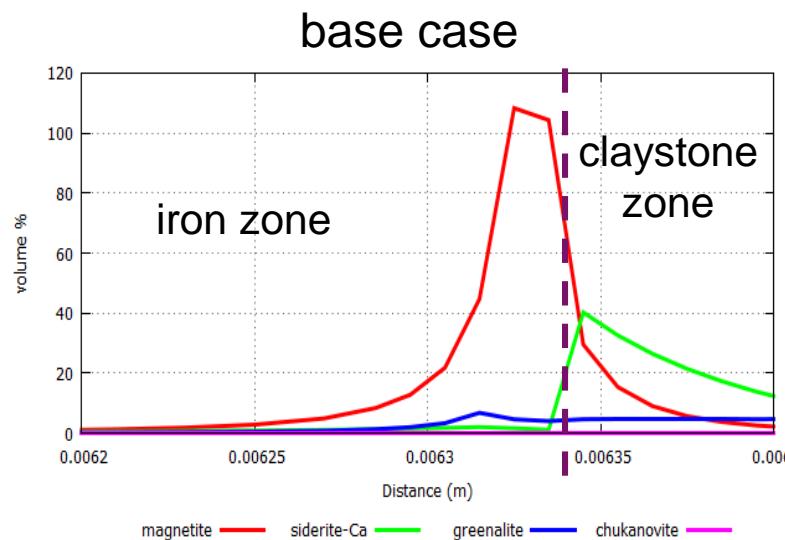
➤ discussion: coupling of electrochemical corrosion reactions with reactive transport codes



# STEEL CORROSION “GEOCHEMICAL” REACTION

## ✓ Corrosion in reactive transport codes

- ✓ changes in pH and Eh occur through:

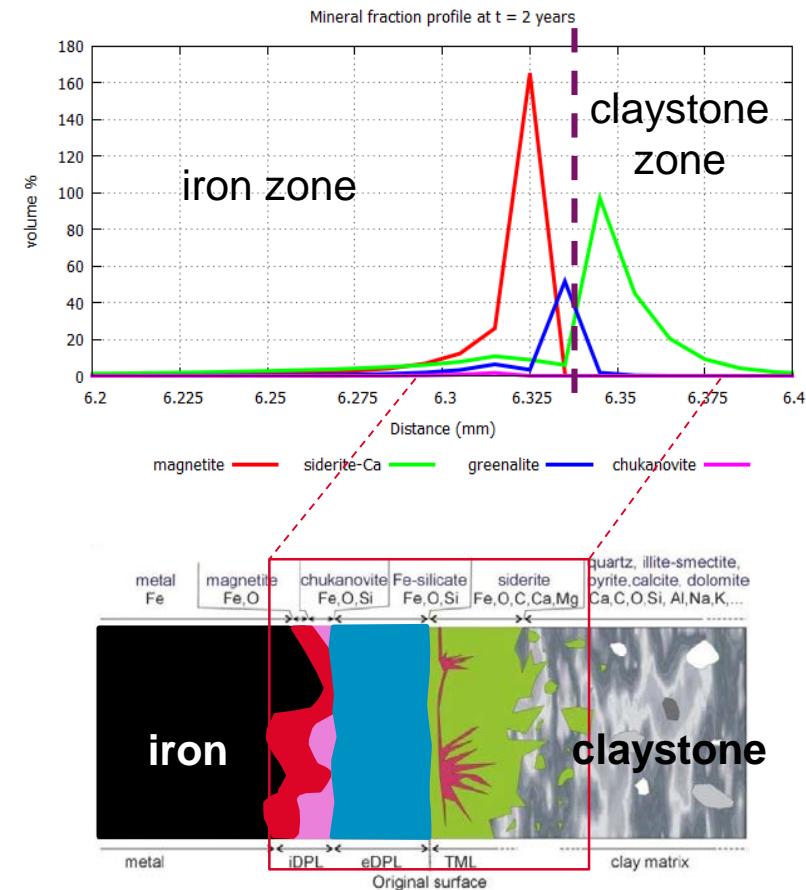


# STEEL CORROSION “GEOCHEMICAL” REACTION

... but the paragenesis of secondary minerals is not predicted correctly

To match the mineralogical paragenesis, we have to modify:

- (very low) diffusional properties in the corroded layer
- (high) magnetite precipitation rate



from Schlegel et al. 2014

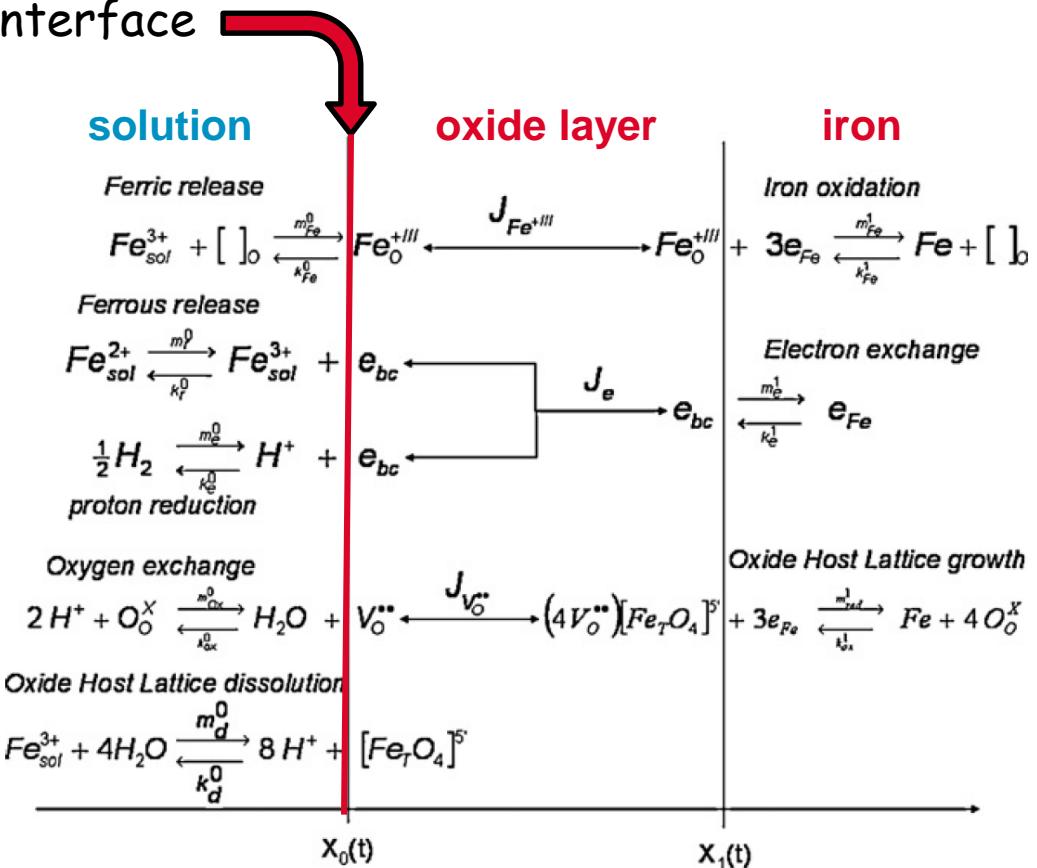
# CORROSION: ELECTROCHEMICAL REACTIONS

## Corrosion: an electrochemical model

✓ redox reactions occurring at the interface

✓ non-equilibrium reactions involving electrons in the conduction band

✓ corrosion generates fluxes of  $\text{Fe}^{2+}$ ,  $\text{Fe}^{3+}$ ,  $\text{H}_2$ ,  $\text{H}^+$ , ...



Diffusion Poisson Coupled Model (DPCM)  
from Bataillon et al. *Electrochim. Acta* 2010

# CONCLUSIONS

✓ Coupling of electrochemical corrosion reactions with reactive transport codes:

- ✓ use elemental fluxes ( $\text{Fe}$ ,  $\text{H}_2$ )?
- ✓ use mineral reaction rates (corrosion and oxide layer precipitation/dissolution)?
- ✓ use fluxes for  $\text{Fe}^{2+}$  and  $\text{Fe}^{3+}$  and aqueous kinetics?

# THANK YOU FOR YOUR ATTENTION

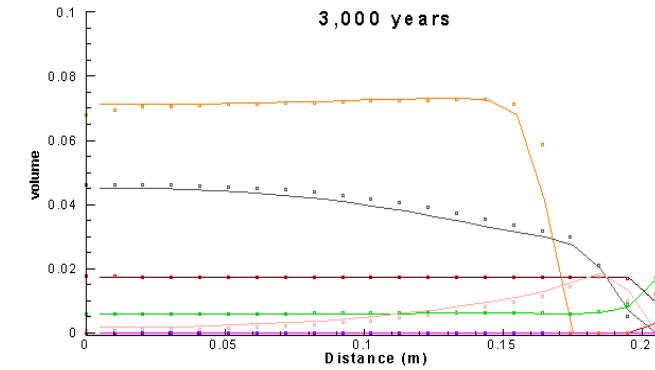
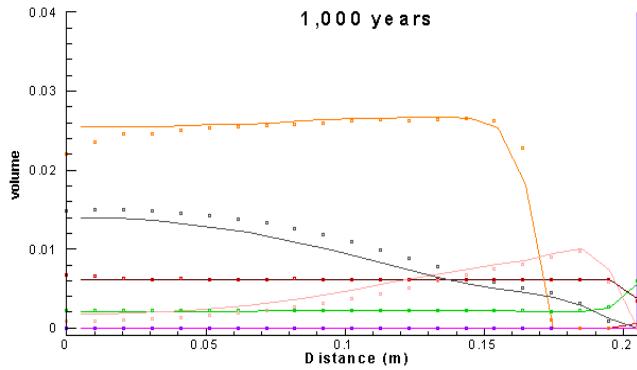
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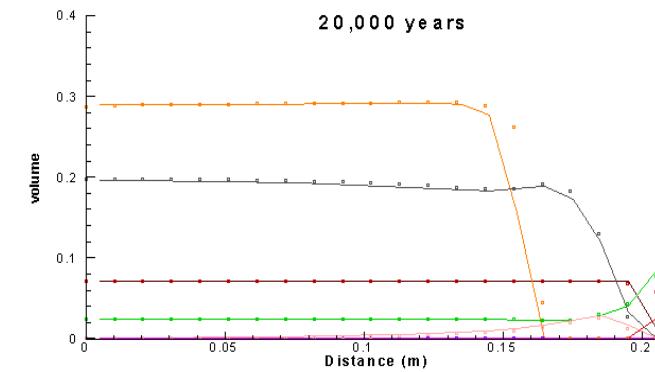
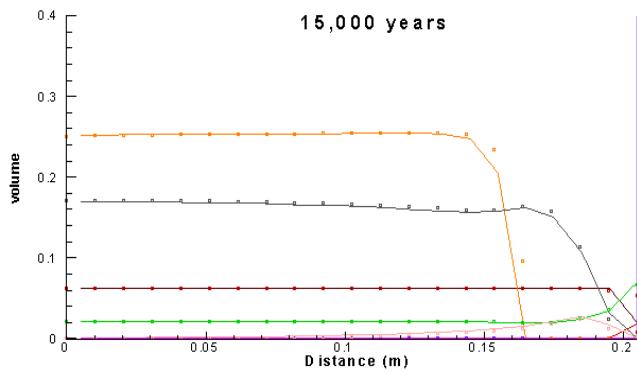
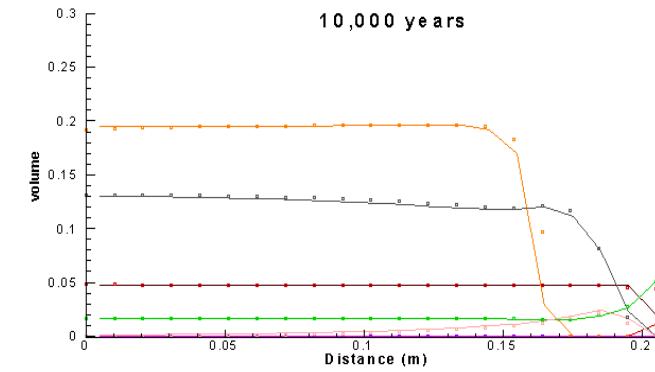
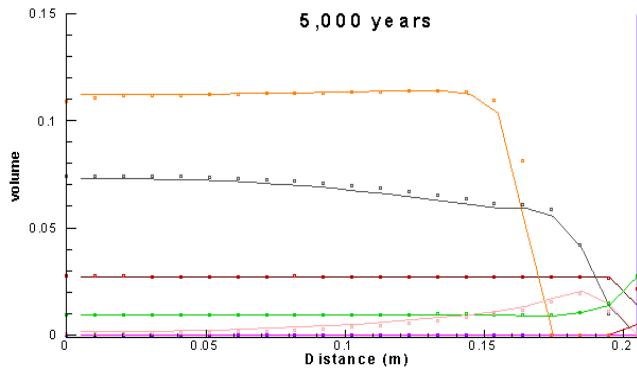
Direction de l'Energie Nucléaire  
Département des Technologies  
Nucléaires  
Service de Modélisation des Transferts  
et de Mesures Nucléaires

# Update on glass/iron/clay benchmark

# RESULTS IN THE BASE CASE (3)

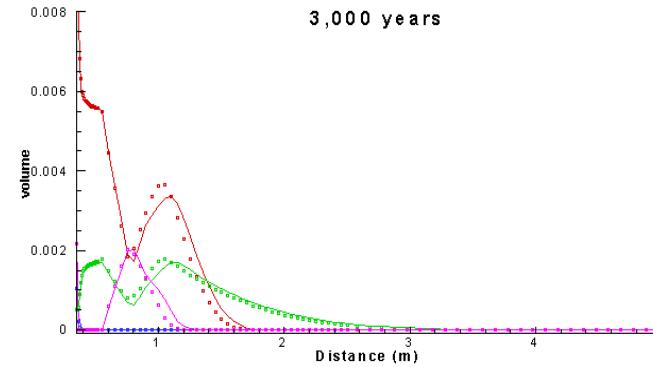
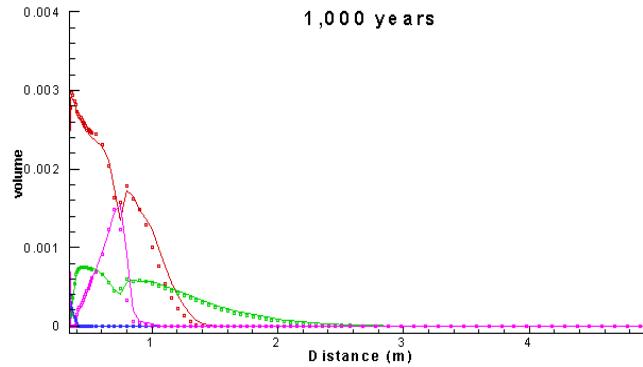


in the glass zone

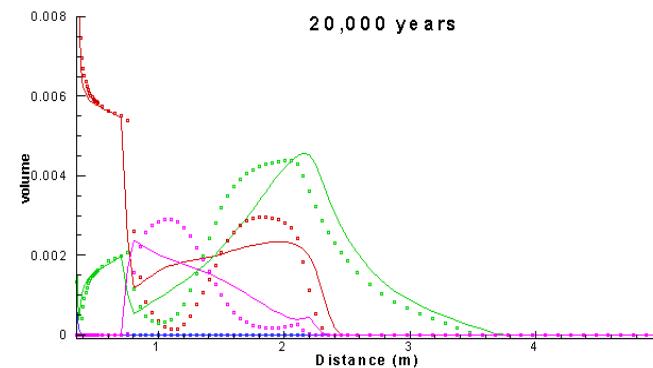
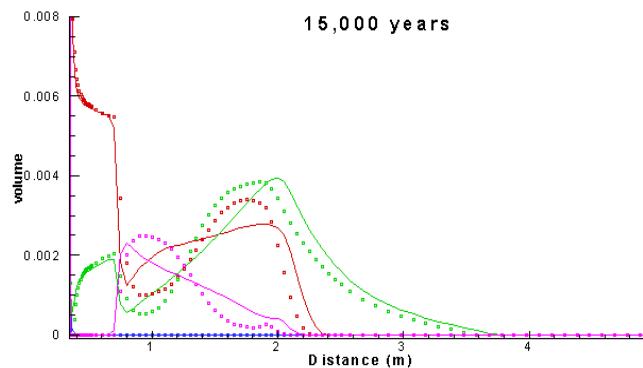
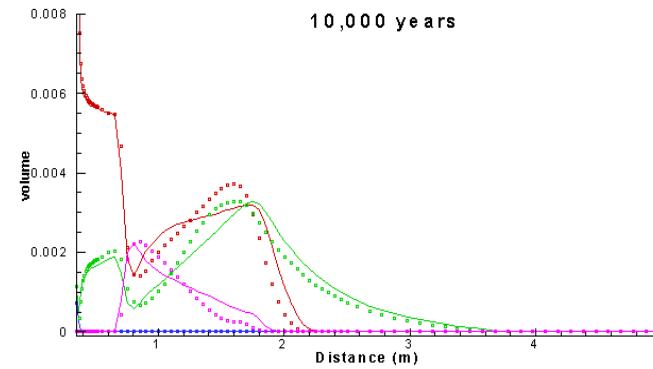
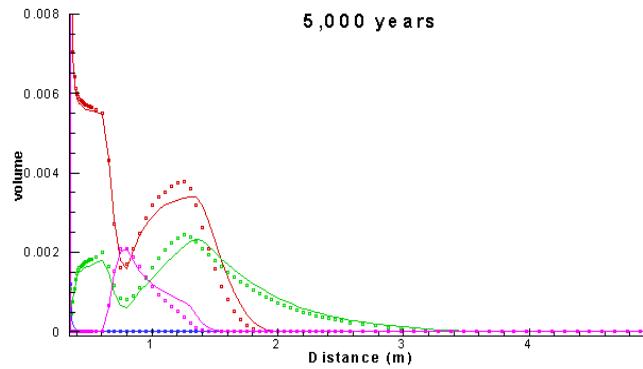


- Calcite - crunchflow
- Chalcedony - crunchflow
- Daphnite\_14A - crunchflow
- Fe-Saponite-Na - crunchflow
- Fe-MontmorilloniteNa - crunchflow
- G reenalite - crunchflow
- Illite-F ell - crunchflow
- Magnetite,beta - crunchflow
- Pyrrhotite-alpha - crunchflow
- Daphnite 14 A - MIN 3P
- G reenalite - MIN 3P
- Fe-Saponite-Na - MIN 3P
- Pyrrhotite-alpha - MIN 3P
- Magnetite,beta - MIN 3P
- Chalcedony - MIN 3P
- Fe-MontmorilloniteNa - MIN 3P
- Calcite - MIN 3P
- Illite-F ell - MIN 3P

# RESULTS IN THE BASE CASE (4)



**in the clay zone**



- Daphnite\_14 Å - crunchflow
- Fe-Saponite-Na - crunchflow
- Greenalite - crunchflow
- Pyrrhotite-alpha - crunchflow
- Daphnite 14 Å - MIN 3P
- Greenalite - MIN 3P
- Fe-Saponite-Na - MIN 3P
- Pyrrhotite-alpha - MIN 3P