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DE LA RECHERCHE À L'INDUSTRIE





CORROSION BEHAVIOUR OF 9-12%CR AND 17-22%CR STEELS IN S-CO₂



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JC RUIZ, P. VENDITTI

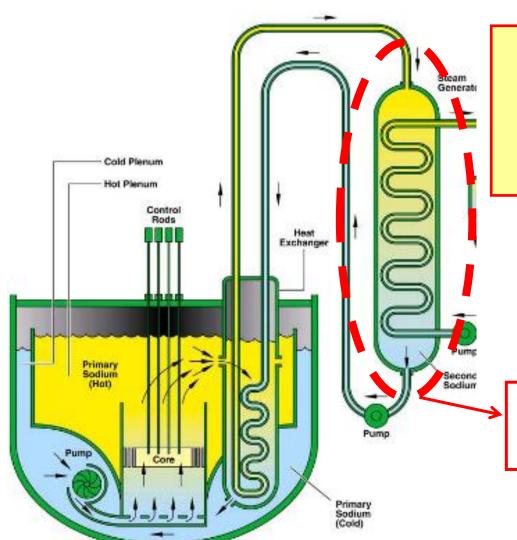
CEA/DEN/ DTCD/SPDE/LPSD (MARCOULE)



www.cea.fr



CONTEXT: S-CO₂ BRAYTON CYCLE COUPLED TO SFR



Advantages of S-CO₂ Brayton cycle:

- Avoids the Sodium-Water reaction
- •Increases the compactness of the cycle
 - •Increases the cycle efficiency

International collaboration on S-CO₂ cycle coupled to Sodium Fast Reactor: France, USA, South Korea, Japan

T: 400 - 550 °C

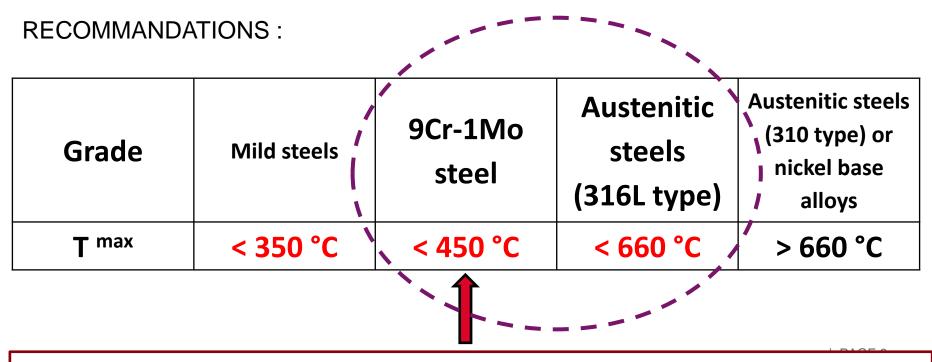
P: 80 - 250 bar



CORROSION IN CO₂?

FEEDBACKS FROM FORMER CO₂-COOLED NUCLEAR REACTORS (60-80'S)

 $CO_2 + 1\%$ vol CO + up to a few hundreds of vpm H_2O , H_2 , CH_4 Pressure = 3 - 4 MPa



T max: strongly dependent on gas composition, steel composition, surface finish, ...

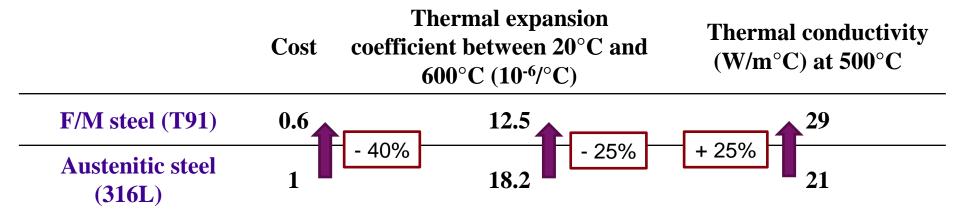
[D.R. Holmes, R.B. Hill, and L.M. Wyatt, Corrosion of steels in CO₂, British Nuclear Energy Society, Reading University (1974)]



MATERIALS FOR APPLICATIONS UP TO 550 °C

9-12%Cr Ferritic/Martensitic steels

17-22%Cr Austenitic steels



- 9-12% Cr Ferritic/Martensitic steels : Physical Properties and Cost +
 - □ 17-22% Cr Austenitic steels : Intrinsic Corrosion Behaviour 🕂



CEA - JAEA COLLABORATION (2008-2014)



Objectives: Technical exchanges for comprehensive understanding of corrosion mechanisms in S-CO₂

In both labs:

- more than 350 corroded samples
- 11 steel grades (F/M and austenitic steels)
- 5 temperatures from 400 °C to 600 °C
- 4 CO₂ pressures : from 0.1 MPa to 25 MPa
- Up to 8000 h of exposure time
- Use of various experimental facilities (loop, autoclave, onethrough furnace): study of their impact ...



S

STUDIED MATERIALS

l ste
∀
ustenitic steels

Weigth %	%Cr	%Ni	%C	%Si	Other	Feedback
T91 (CEA)	9	0.2	0.1	0.3	Mo : 1%	SG in Fossil Power Plants
VM12 (CEA)	11	0.4	0.1	0.3	W : 2% Co : 2%	New generation of 9-12Cr steel
P122 (JAEA)	11	0.4	0.1	0.3	W : 2% Cu : 1%	New generation of 9-12Cr steel
316L (CEA)	17	11	0.02	0.6	Mo : 2%	« classic » austenitic steel
316FR (JAEA)	17	11	0.01	0.6	Mo : 2% N : 0.1%	« nuclear » grade austenitic steel
253MA (CEA)	21	11	0.1	1.6	Ce: 0.04%	Steel optimized for HT corrosion



CORROSION FACILITIES

High pressure S-CO₂



Atmospheric pressure CO₂





Metallic coupons (25*15*1 mm)

« Industrial » CO₂ purity in JAEA and CEA tests (99,995%):

- $H_2O < 200 \text{ vpm}$
- $O_2 < 50 \text{ vpm}$

CORROSION OF 9-12CR F/M STEELS

TODAY: WHAT WE THINK TO KNOW WITH A GOOD CONFIDENCE

F. ROUILLARD AND T. FURUKAWA, CORROSION SCIENCE JAN 2016

- ☐ The « short-term » corrosion kinetics of usual 9-12%Cr steels
 - ✓ Oxidation rate = f(T, P)
 - ✓ Carburisation rate = f(T, P)



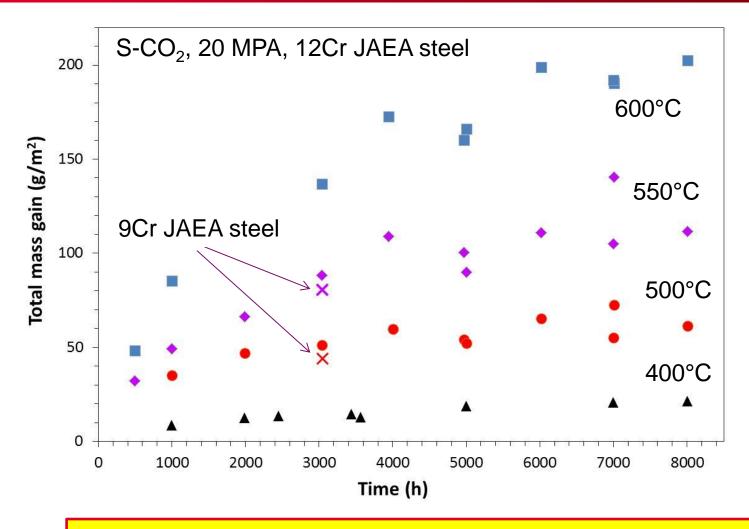
Proposed corrosion model: « Available Space Model »

- ✓ Influence of surface finish
- ✓ Influence of O₂ impurities in CO₂

PhD thesis of S. Bouhieda (2009-2012)



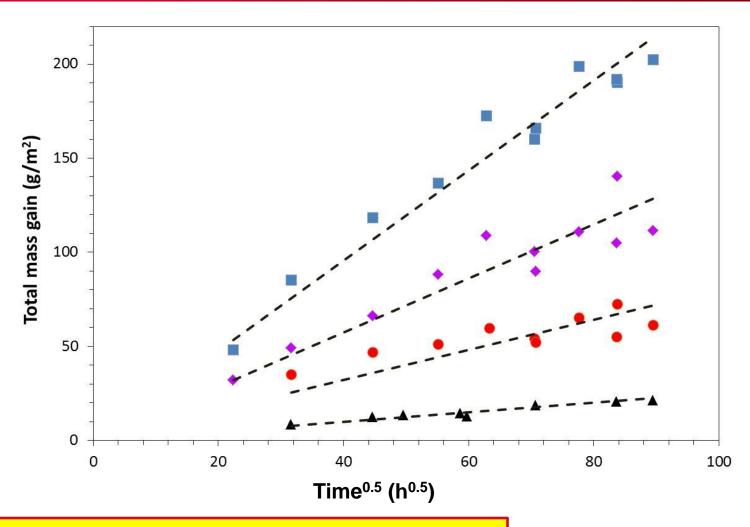
CORROSION KINETICS OF 9-12CR JAEA STEELS



Same corrosion kinetics for 9 and 12Cr steel (JAEA)



CORROSION KINETICS OF 9-12CR JAEA STEELS

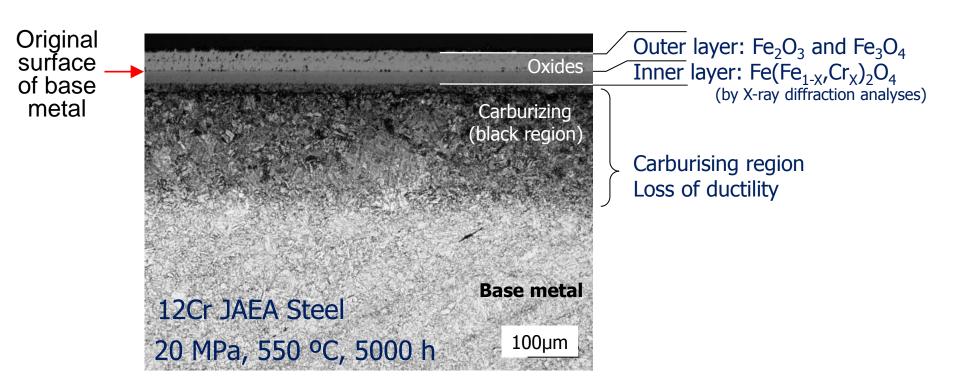


- □ Parabolic kinetics
- What does happen to the samples?



CORRODED SURFACE UNDER CO₂

Mass gain = Oxidation AND Carburisation



What are the proportion of the mass gain induced by:

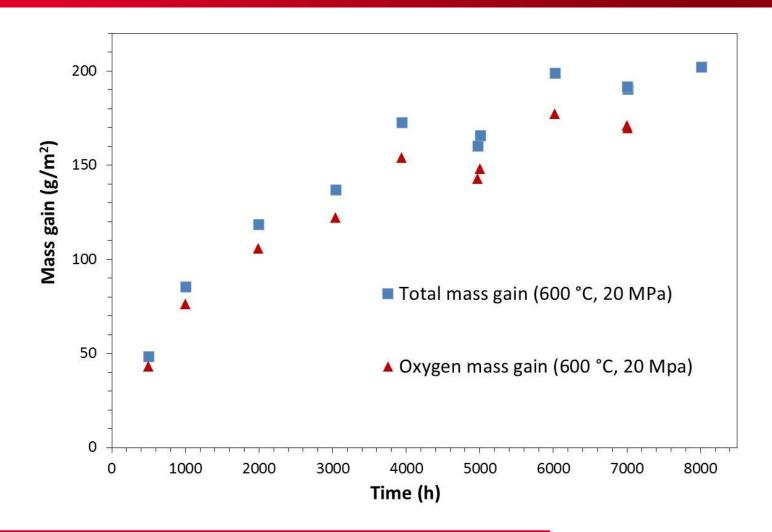
- Oxidation : Mechanism ? Driving Force ?
- Carbon transfer : Mechanism Driving Force ?



Oxidation mechanism of 9-12Cr steels in CO₂



OXIDATION KINETICS

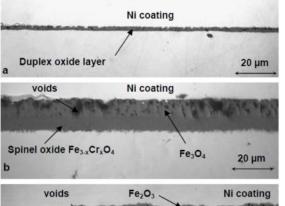


Parabolic oxidation rate = diffusion controlled



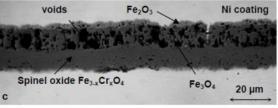
OXIDE FEATURES

9Cr CEA steel in CO₂, 550 °C, 0.1 MPa

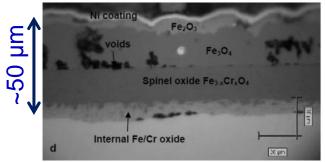


110 h

1 h



322 h



1000 h

- •**Duplex** oxide layer : Fe oxides (Fe₃O₄ + Fe₂O₃) and Fe/Cr oxide (Fe_{2.3}Cr_{0.7}O₄)
- •The oxide/oxide interface = **original** metallic surface (gold markers)
- •[Cr]_{spinel}(mol/cm³) ~ [Cr]_{substrate}(mol/cm³)

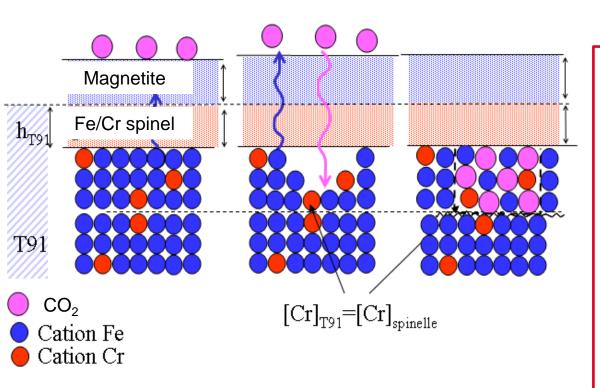
 Chromium does not diffuse and is oxidized in the substrate.
- •<u>Carbon</u> enrichment at the O/M interface (GDOES analysis)
- •Fe_{2.3}Cr_{0.7}O₄ grows at the metal/oxide interface and Fe₃O₄ at the oxide/gas interface (Taylor et al. OxMet. 1980 : Tracers experiment).
- Parabolic growth rate

Oxidation model?

OXIDATION

F. ROUILLARD ET AL. OXIDATION OF METALS 77 N°1-2 (2012)

« Available Space Model » or « void-induced oxide growth »



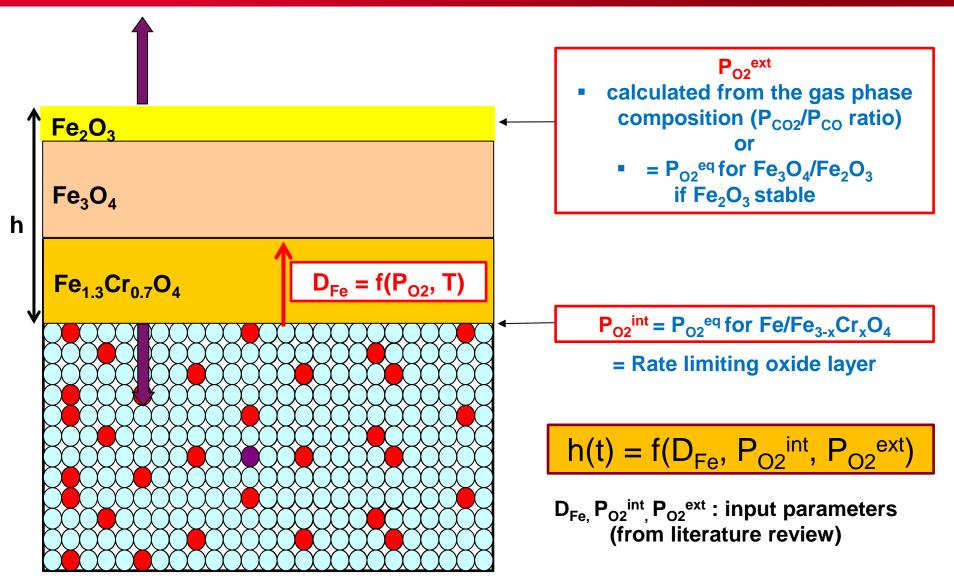
- Outwards diffusion of Fe cations
- ✓ Injection of vacancies at the O/M interface
- ✓ Formation of voids
- 2. CO₂ diffusion to the O/M interface

through high diffusion paths (nanochannels) in the oxide layer *Atkinson et al. Rev. Mod. Phys. 57 (1985)*

3. Filling of the voids by new oxide formation

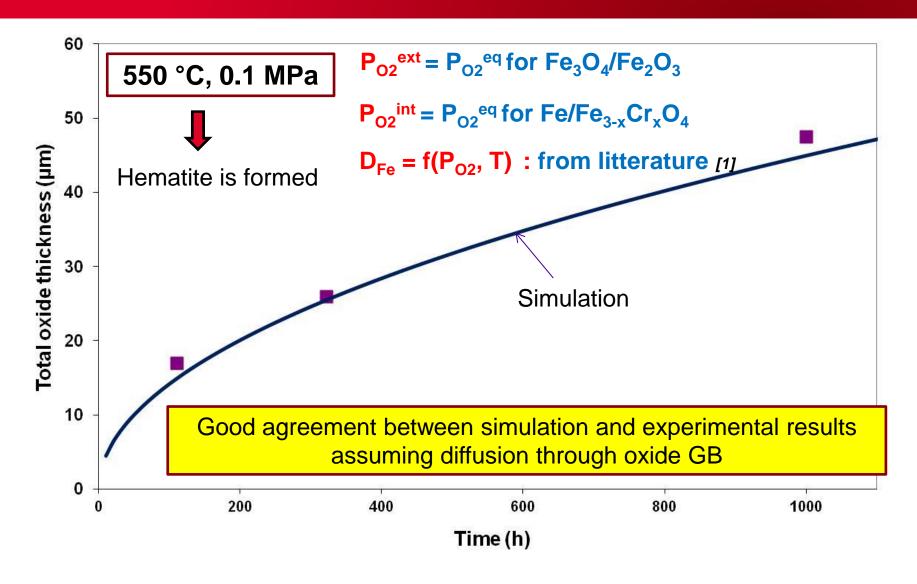


OXIDE KINETICS MODELING AND SIMULATION



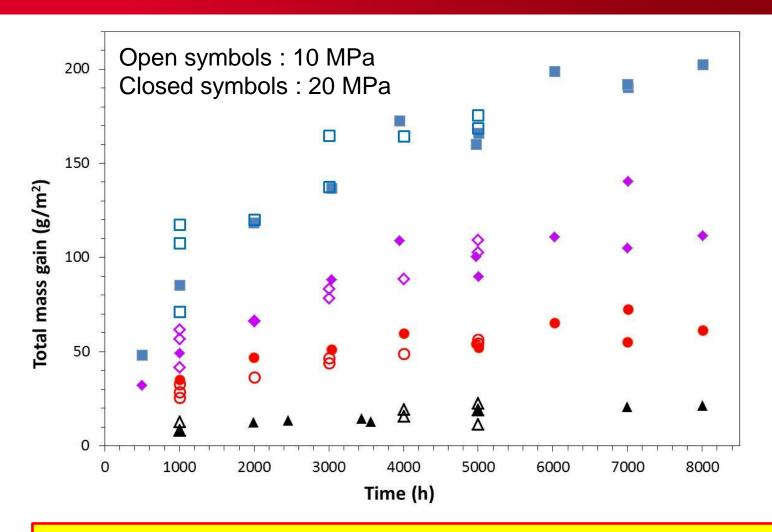


OXIDE GROWTH MODELING AND SIMULATION





EFFECT OF P_{CO2} ON OXIDATION

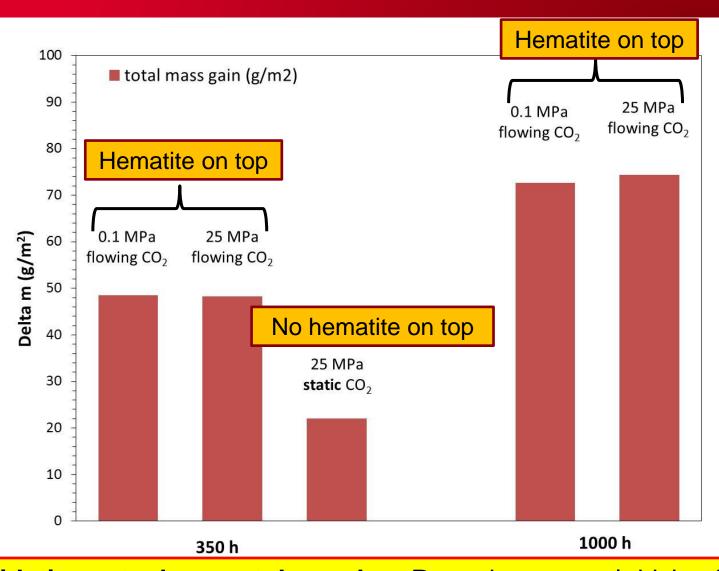


No detectable effect of P_{CO2} between 10 and 20 MPa

With higher P_{CO2} difference : 0.1 MPa and 25 MPa ?

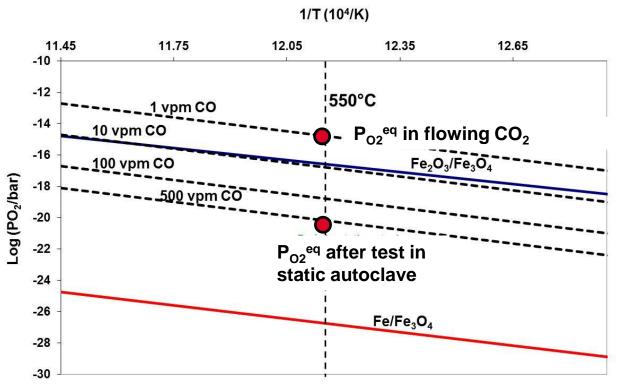


EFFECT OF P_{CO2} ON OXIDATION



The oxidation rate does not depend on P_{CO2} : the external driving force for oxide growth P_{O2}^{ext} is « buffered » by the presence of hematite

FORMATION OF FE₂O₃ ?



The formation of Fe_2O_3 is controlled by the P_{CO2}/P_{CO} ratio in the gas phase :

$$CO_2(g) = CO(g) + 0.5O_2(g)$$

$$P_{o_2}^{ext} = \left(\frac{K * P_{CO_2}}{P_{CO}}\right)^2$$

CO(g) in the gas phase is mainly formed from oxidation of the metallic substrate :

$$xM + yCO_2(g) = M_xO_y + yCO(g)$$

As a consequence, the driving force for oxidation $P_{\text{CO2}}/P_{\text{CO}}$ is driven by any CO accumulation encoutered along the flow :

- Depends on the hydrodynamics encoutered in the channel or the tube
- Oxidation kinetics in static autoclave < Oxidation kinetics in tube furnace with gas flow</p>



Carburisation mechanism of 9-12Cr steels in CO₂

QUESTIONS?

What is the carburisation kinetics? Is there any effect of P_{CO2} ?

Could we model the carburisation propagation into the steel?

Why does the steel carburise?

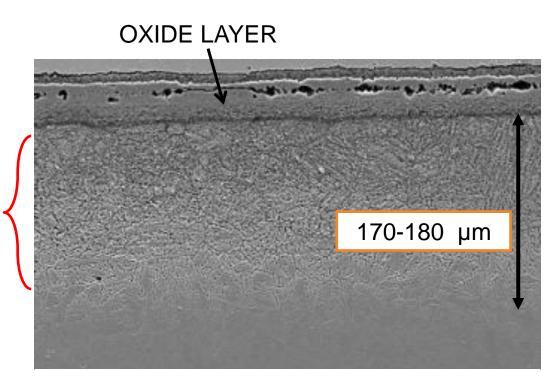
What are the driving force and the mechanism for carbon transfer?



CARBURISATION MICROSTRUCTURE

CARBURISED ZONE:

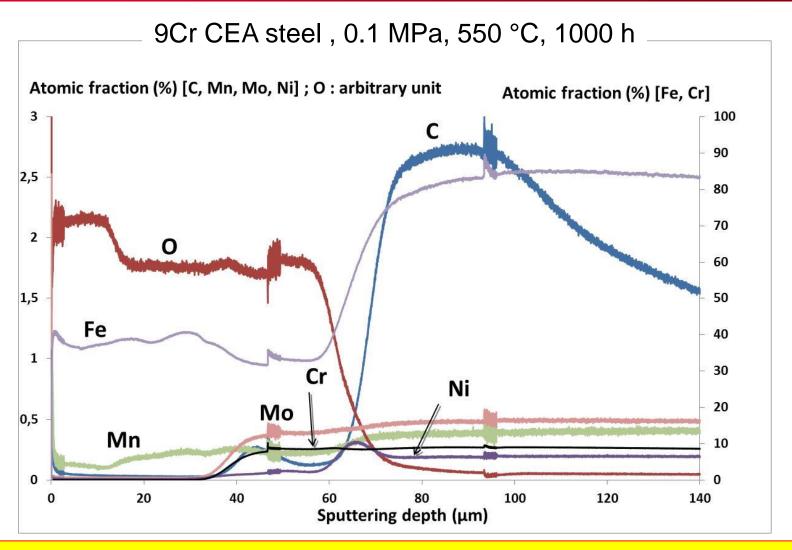
On martensitic laths and old primary austenitic GB



9Cr CEA steel, 0.1 MPa, 550 °C, 1000 h



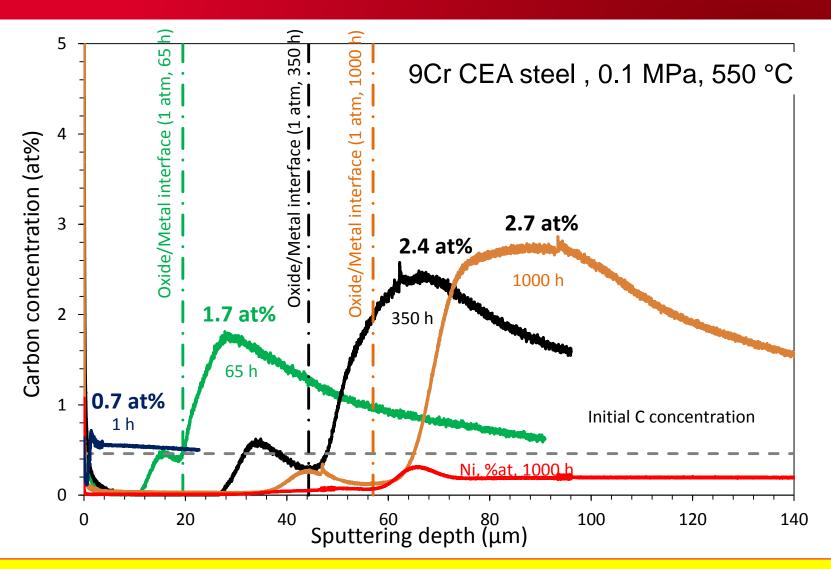
CARBON PROFILE BY GDOES



□ Strong carbon enrichment below the O/M interface
 □ No carbon in magnetite. Only small content in the spinel oxide layer



NON STEADY STATE CARBURISATION



%C at the O/M interface increases with time = Non steady state carburisation



CARBURISATION PROPAGATION INTO THE SUBSTRATE

- □ Carburisation depth kinetics = Parabolic ...
- ... even if increase of %C at the oxide/metal interface with time?
- ☐ The carburisation depth kinetics is:
 - lower than expected by simple C diffusion in ferrite
 - higher than expected by C diffusion in ferrite and reaction with all Cr atoms to form carbides (according to Wagner theory)



Similar results than observed by Young et al.

Non-steady state carburisation of martensitic 9 – 12%Cr steels in CO₂ rich gases at 550 °C, Young et al. Corrosion Science 88 (2014)



YOUNG'S CARBURISATION MODEL ASSUMPTIONS

□ Normal diffusion of solute carbon within the metal phase,
coupled with rapid carbide precipitation and equilibrium
partitioning of carbon between the metal and precipitate
phases (Thermodynamic calculations)

☐ Slow rate of carbon transfer:

$$v_c = \alpha (C^{eq} - C^s)$$

With C^{eq} the concentration of carbon in equilibrium with <u>the</u> <u>carbon activity of the gas phase</u>

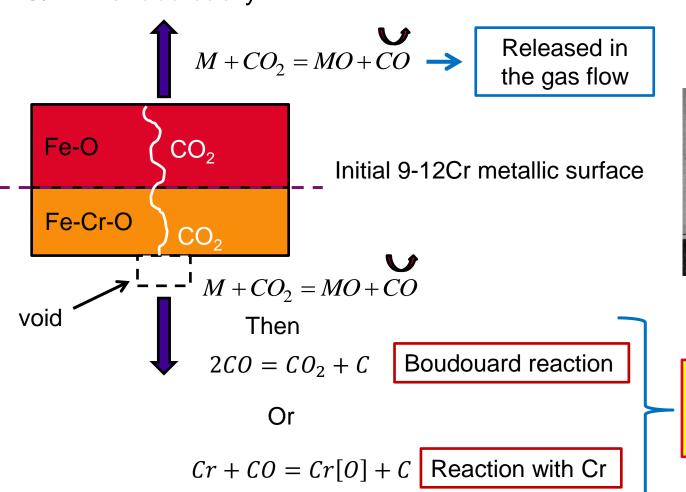


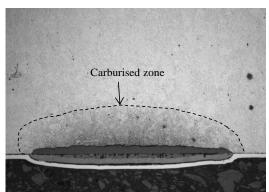
There are still questions about the carbon transfer mechanism and its rate expression



CARBON TRANSFER

We believed that the carbon transfer is <u>intrinsically</u> induced by the way the steel oxidizes = the « Available Space Model » allows carbon reaching the O/M interface easily

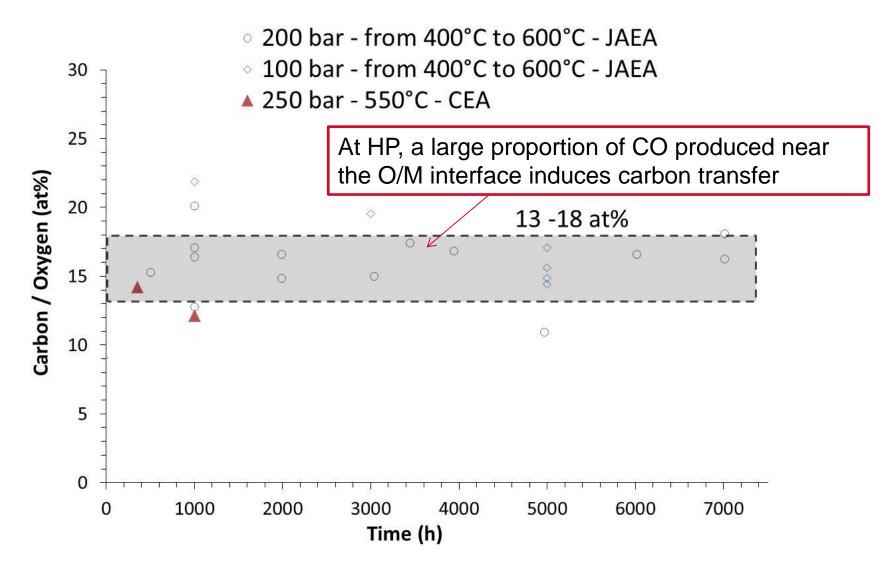




If all CO molecules carburise then %C/%O = 20 at%



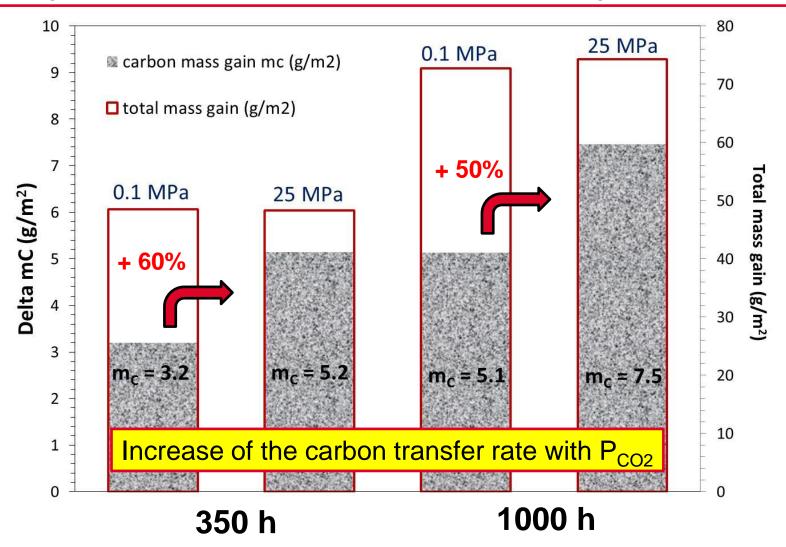
CARBON TRANSFER





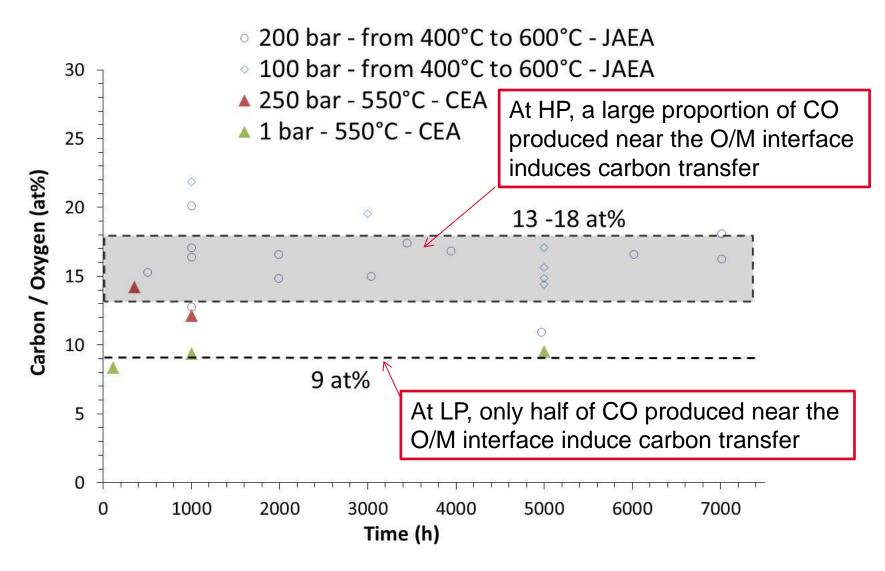
INFLUENCE OF P_{CO2} **ON CARBON TRANSFER**

☐ No « detectable » influence of P_{CO2} between 10 and 20 MPa but higher carbon transfer rate detectable when increasing from 0.1 to 25 MPa

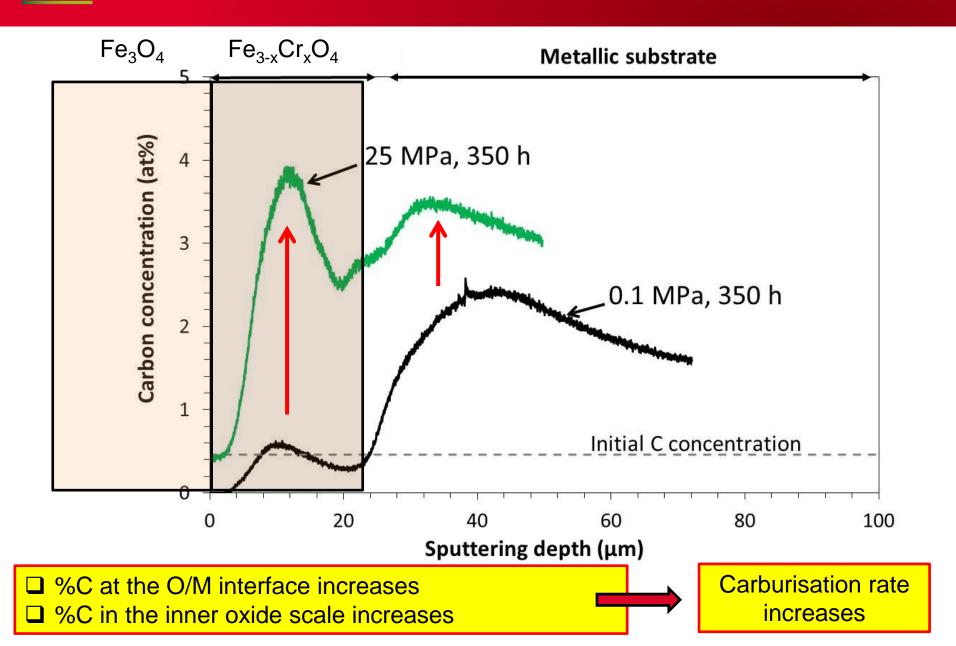




INFLUENCE OF P_{CO2} ON CARBON TRANSFER



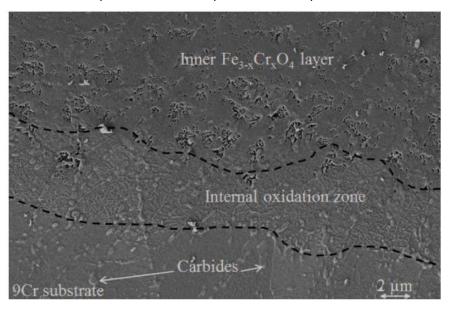
INFLUENCE OF P_{CO2} ON CARBON TRANSFER



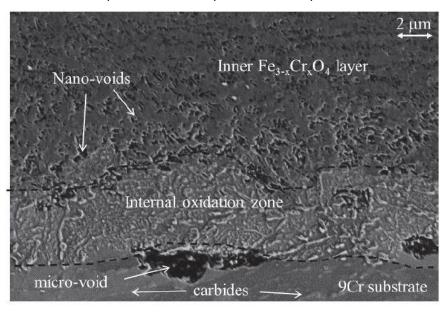


INFLUENCE OF CARBURISATION ON THE INNER OXIDE MICROSTRUCTURE

T91, **0.1 MPa**, 550 °C, 350 h



T91, **25 MPa**, 550 °C, 350 h



At high P_{CO2}:

- ☐ Carbide density is higher below the inner spinel oxide scale
- ☐ The void density in the inner spinel oxide scale is higher



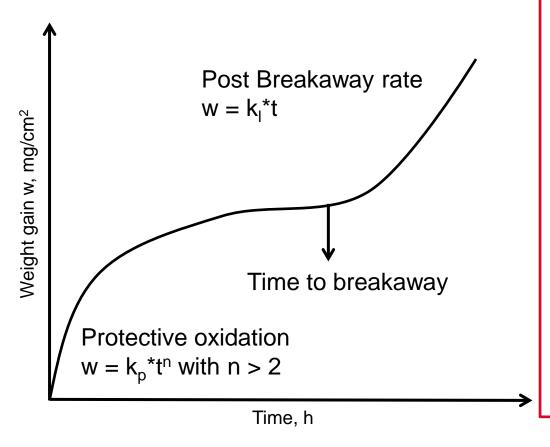
Voids are formed around former carbide precipitates while oxide grows inwards?



Inner oxide porosity may depend on carbide density



CAN « BREAKAWAY » OXIDATION BE POSSIBLE ON USUAL 9-12%CR STEELS ?



Feedbacks from CO₂-cooled nuclear reactors*:

- Known for mild steels in S-CO₂ at T > 350 °C
- But already observed on 9Cr steel in CO₂ – 40 bar at 550°C (first in 1971)
- Favored at HP CO₂ with high water vapour content (>0.1%) and low Si content

*D.R. Holmes, R.B. Hill, and L.M. Wyatt, Corrosion of steels in CO₂, British Nuclear Energy Society, Reading University (1974)

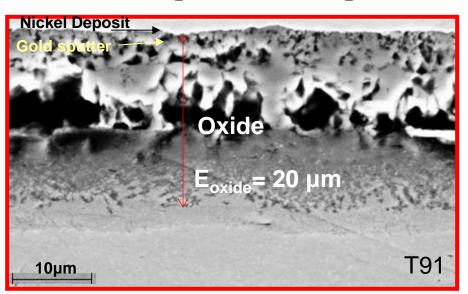
What is the exact mechanism?
Influenced by the carburisation state of the substrate?

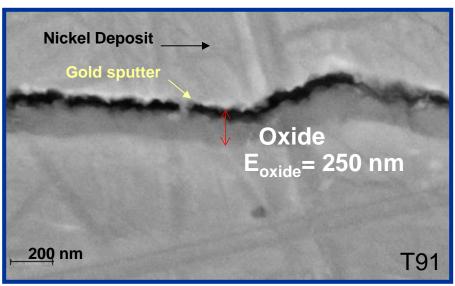


INFLUENCE OF CO2 PURITY ON THE SURFACE OXIDE COMPOSITION

« Industrial » CO_2 purity (with $O_2 \sim 100 \mu bar)$

High CO_2 purity (with $O_2 \sim 1 \mu bar$)





Fast growing iron rich duplex oxide scale

Slow growing chromium rich oxide scale

%Cr oxide ~ 9 at%

%Cr oxide ~ 20 at%

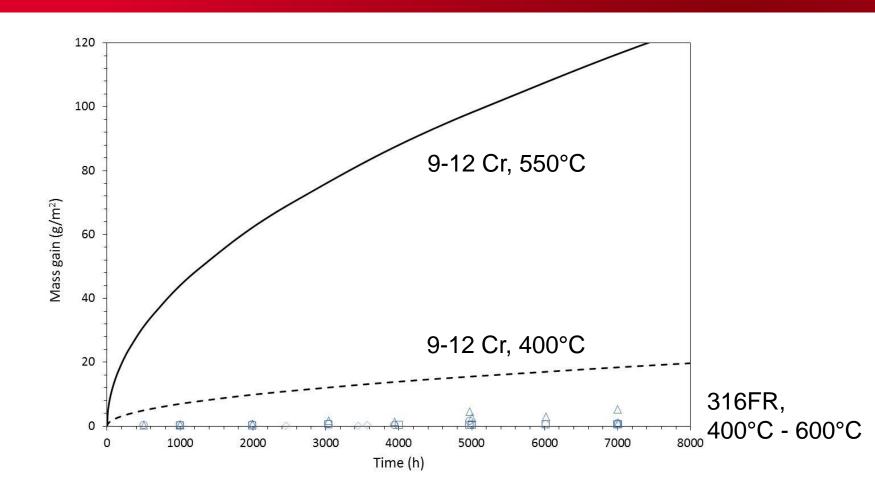
Still protective after 5000 h

Conclusions of PhD thesis (S. Bouhieda 2012):

- O₂ impurities (µbar) react first during the thermal ramp
- Its level in CO₂ impacts on the surface oxide composition (Cr enrichment)
- The surface finish (mainly roughness?) impacts on the critical O₂ partial pressure

CORROSION MECHANISM OF 17-21CR AUSTENITIC STEELS

MASS GAIN KINETICS OF 316 AUSTENITIC STEEL

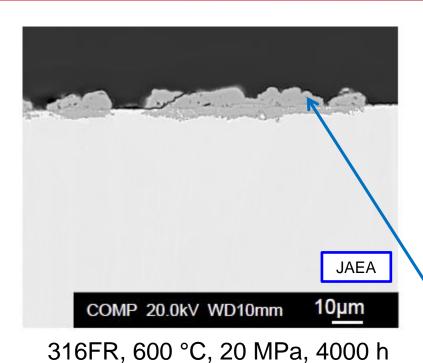


- ☐ Very low mass gain : mass gain (316FR) < 100*mass gain (9-12Cr)
- No detectable effect of total pressure
- ☐ Larger mass gain is detectable after 5000 h at T = 600°C



OXIDE SCALE





316L – 0.1 MPa – 550°C – 1000 h

CEA

< 200 nm

Formation of thin « protective » Cr rich oxide scale and thick nodules of duplex oxide scale (as on 9-12Cr steel but higher %Cr)

The « short-term » resistance of Cr rich austenitic steels is evaluated by its ability to form thin Cr rich oxide scale

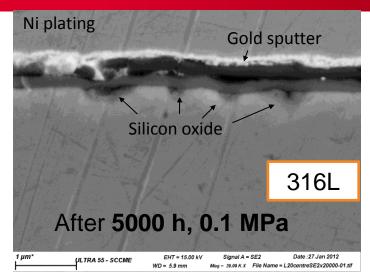
8 µm thick

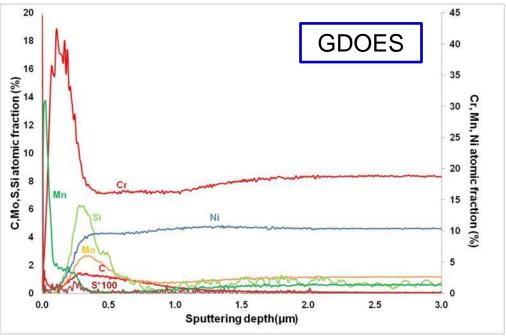
CEA



DETAILS ON THE THIN CR RICH OXIDE SCALE







✓ Oxide layer :

- •Cr rich oxide layer
- ■Mn enrichment in the external part (30 at%) and internal part (4 at%)
- ■Si oxide at the O/M interface (discontinuous)

✓ Substrate:

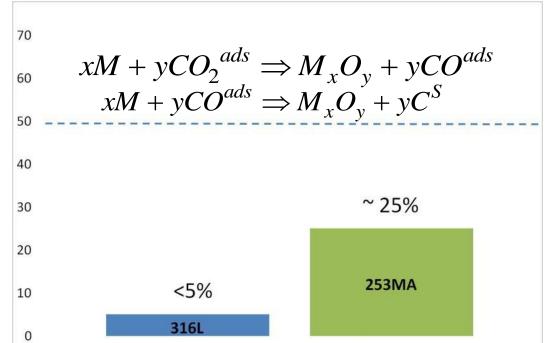
■C enrichment below the oxide layer and diffusion profile

INFLUENCE OF STEEL GRADE ON CARBON TRANSFER

At%	%Cr	%Ni	Other
316L	19%	10%	/
253MA	22%	10%	Si : 3%, Ce

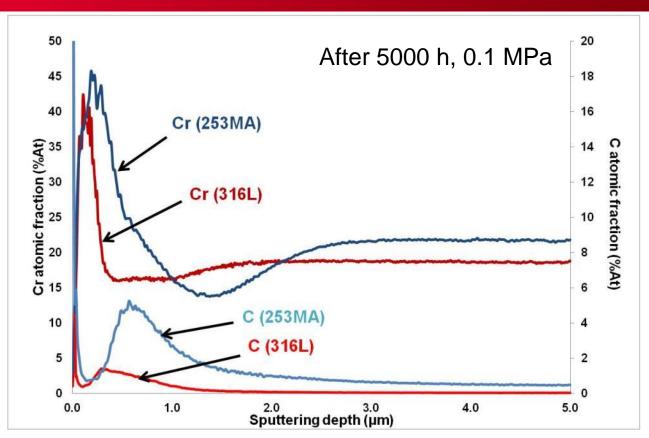
C content / O content ratio for two grades at any time





50%

COO INFLUENCE OF STEEL GRADE ON CARBON TRANSFER

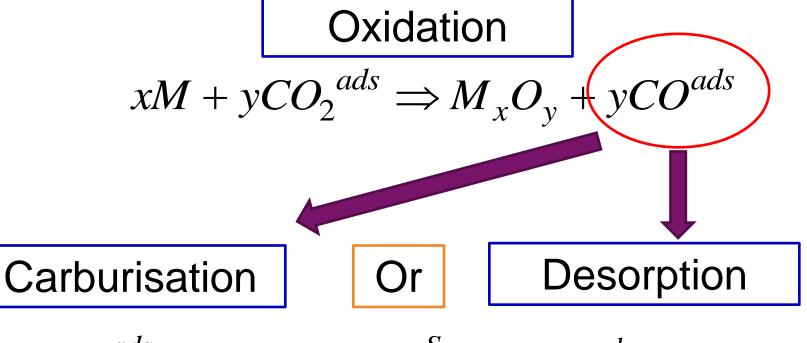


ThermoCalc

At%	Max %at C at the O/M interface	Volume fraction f _v of M ₂₃ C ₆
316L	1.3%	5%
253MA	5%	21% PAGE



CARBURIZATION PROCESS?



$$xM + yCO^{ads} \Rightarrow M_xO_y + yC^S$$
 $CO^{ads} \Rightarrow CO(g)$

Carburisation degree of austenitic steels:

Depends on the catalytic properties of the surface for CO dissociation ?

- ✓ increases with Cr content [Anghel et al. Applied Surface Science 233 (2004)]
- ✓ with other elements?





SUMMARY



9Cr F/M Steels

- **≻Thick duplex oxide scale**
 - [Fe-oxides + Fe/Cr oxide]
- Fast parabolic growth rate Driving force = P_{O2}^{eq} Fe₃O₄/Fe₂O₃
- Strong Carburisation rate
 [via Boudouard reaction ?]

 Carbon transfer rate increases with P_{CO2}

Is Breakaway Oxidation possible ??
One should look for it ...

17-25Cr Austenitic Steels

- ➤Thin oxide scale
 - [Cr rich oxide]
- ➤ Slow growth rate [exact mechanism to be determined]
- **≻Low Carburisation rate**

[via CO dissociation ?]
Increases with %at Cr?
Impact on long-term exposure ?



Formation of oxide nodules on the lowest Cr rich austenitic steels (17Cr) which grow faster

THANK YOU FOR YOUR ATTENTION