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A NEW NUMERICAL ALGORITHM FOR TWO-PHASE FLOWS DRIFT-FLUX MODEL WITH STAGGERED GRID IN POROUS MEDIA

ANOUAR MEKKAS¹, ANNE CHARMEAU² AND SAMI KOURAICHI³

Abstract. FLICA4 is a 3D compressible code dedicated to reactor core analysis. It solves a compressible drift-flux model for two-phase flows in a porous medium [2]. To define convective fluxes, FLICA4 uses a specific finite volume numerical method based on an extension of the Roe's approximate Riemann collocated solver [3]. Nevertheless, analysis of this method shows that at low Mach number, it is necessary to apply modifications to the 2D or 3D geometries on a cartesian mesh otherwise this method does not converge to the right solution when the mach number goes to zero [4]. For this reason, we apply a so-called "pressure correction". Although this correction is necessary to reach the required precision, it may produces some checkerboard oscillations in space in the situations we are interested in, especially in the 1D case. Since these checkerboard oscillations are sometimes critical and may lead to unstable solutions in some cases, we investigate another numerical algorithm to solve this compressible drift-flux model in the low Mach regim. The aim of this work is to propose a new compressible scheme accurate and robust at low Mach number on staggered grid since checkerboard oscillations cannot exist on this type of discretisation [8]. The accuracy and robustness of this new scheme are verified in low Mach regime with test cases describing a simplified nuclear core "Boiling channel". The behavior of this scheme is also tested in the compressible regime with or without shock waves.

Résumé. FLICA4 est un logiciel de simulation 3D dédié à l'analyse des écoulements dans les coeurs de réacteurs nucléaires et qui résout un modèle compressible diphasique à 4 équations à l'échelle poreuse [2]. Le schéma numérique du code FLICA4 est basé sur une technique de volumes finis où les flux numériques convectifs sont calculés à l'aide d'un solveur colocalisé appelé Roe [3]. L'analyse de cette méthode numérique montre qu'à bas nombre de Mach, il est nécessaire d'introduire des modifications spécifiques aux géométries 2D ou 3D sur un maillage cartésien sans quoi la solution ne converge pas vers la bonne solution lorsque le nombre de Mach tend vers zéro [4]. C'est la raison pour laquelle une correction dite "correction de pression" est appliquée. Cette "correction de pression" nécessaire à la précision du schéma numérique à bas nombre de Mach pour des configurations 2D ou 3D sur un maillage cartésien introduit presque systématiquement des oscillations en espace de type mode en échiquier dans les configurations étudiées ici, surtout en 1D. Comme ces oscillations spatiales peuvent être très fortes dans certains cas et éventuellement conduire à une divergence de certains calculs. Nous étudions un nouvel algorithme numérique pour résoudre le modèle compressible diphasique à 4 équations. Le but de ce travail est de proposer un nouveau schéma numérique précis et robuste à bas nombre de Mach sur grilles décalées car les oscillations spatiales de type mode en échiquier sont inexistantes avec ce type de discrétisation [8]. Ce nouveau schéma numérique est vérifié en régime bas Mach avec des cas-tests décrivant un coeur nucléaire simplifié "canal bouillant". Le comportement de ce schéma est également testé en régime compressible avec ou sans ondes de choc.

INTRODUCTION

FLICA4 is a 3D compressible code dedicated to reactor core analysis. This code solves for a compressible drift-flux model for two-phase flows in a porous medium [2]. To derive convective fluxes, FLICA4 uses a specific finite volume numerical method based on an extension of the Roe's approximate Riemann

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colocated solver [3]. Nevertheless, an analysis of this type of method shows that at low Mach number, it is necessary to apply modifications to the 2D or 3D geometries on a cartesian mesh otherwise this method does not converge to the right solution when the mach number goes to zero [3]. For this reason, we apply a so-called “pressure correction“. Although this correction is necessary to reach the required precision, it may produces some checkerboard oscillations in space, especially in the 1D case.

Since these checkerboard oscillations are sometimes critical and may lead to unstable solutions in some cases, we also investigate another numerical algorithm to solve this compressible drift-flux model in the low Mach regim. The key point is to developpe a compressible solver on staggered grid since checkerboard oscillations cannot exist on this type of discretisation [8]. The aim of this work is to present such a compressible scheme and to verify it in the low Mach regime with test cases describing a simplified nuclear core. Then, the behavior of this scheme is tested in the compressible regime with or without shock waves.

The compressible solver on staggered grid that we develop follows the finite volume approach for all 4 balance equations. The time discretization of the equations is based on a semi-implicit scheme. Since the equations are not linear, the solution at each time step is obtained by a Newton-Raphson iterative method. This method gives a linear system of equations for the increments of the principal variables. The chosen solution algorithm [6] consists at first in eliminating the velocity increments as functions of the pressure increments by rewriting the momentum equations. Substituting the velocity increments into the non-linear system gives a system involving only the pressure increments. The successive elimination of the scalar variables other than the pressure variable gives a linear system on the pressure. The resolution of this linear system allows to determine the velocity and the other variables. Preliminary numerical experiments are presented and compared with analytic solutions [7, 12].

§4.1 shows that the current numerical scheme computes solutions very close to the analytical solutions in the scope of low Mach number flows (see figures 4, 5 and 6). The numerical method uses non-conservative formulation of the four equations. Therefore, difficulties to get precise shock wave solutions were expected. Figures 7 and 9 indeed show a lack of precision of the new numerical scheme to capture shock waves although it is stable. Nevertheless, the scheme captures compressible regular solutions with accuracy (see figure 8). As a consequence, our scheme is robust and is enough accurate to capture at the same time subsonic compressible solutions and low Mach solutions: this property is the main requirement for our applications.

1. POROUS 4 EQUATIONS MODEL

FLICA4 is a four equation code. The equations are mixture mass balance, phasic mass balance, mixture momentum balance and mixture energy balance. The 4 equations are averaged in space, time and phase over control volumes. A drift-flux model is used to account for the slip between vapor and liquid phases. The fluid is compressible and the two-phases are assumed to be at the same pressure. One of the phases is assumed to at saturation temperature. The equations written in the non-conservative are given by:

$$(\mathcal{M}) \begin{cases} \phi \frac{\partial \rho}{\partial t} + \nabla \cdot (\phi \rho \vec{V}) = 0, \\ \phi \frac{\partial (\rho C)}{\partial t} + \nabla \cdot (\phi \rho C \vec{V}) + \nabla \cdot (\phi \rho C (1 - C) \vec{V}_r) = \nabla \cdot (\phi K_{cv} \nabla C) + \phi \Gamma_v, \\ \phi \rho \left(\frac{\partial \vec{V}}{\partial t} + \vec{V} \cdot \nabla \vec{V} \right) + \nabla \cdot (\phi \rho C (1 - C) \vec{V}_r \otimes \vec{V}_r) + \phi \nabla P = \nabla \cdot \vec{\tau} + \phi \tau_f + \phi \rho \vec{g}, \\ \phi \frac{\partial (\rho e)}{\partial t} + \nabla \cdot (\phi \rho e \vec{V}) + P \nabla \cdot (\phi \vec{V}) + \nabla \cdot (\phi \rho C (1 - C) (H_v - H_l) \vec{V}_r) = \phi Q + \nabla \cdot \vec{q}. \end{cases} \quad (1)$$

Above, the blue terms are given by the user, the red terms are computed with physical modeling and the green terms are defined by the equation of state

$$\rho = \mathcal{F}(P, h). \quad (2)$$

The nomenclature is given as follows : t is the time, ϕ is the porosity, ρ is the mixture density, h is the mixture specific enthalpy, $\vec{V}$ is the mixture velocity, $\vec{V}_r$ is the relative velocity between the two phases, C is the vapor mass concentration, P is the mixture pressure, e is the mixture internal energy, H_v is the steam total enthalpy, H_l is the liquid total enthalpy, $\vec{g}$ is the gravity force, Q is the power density, $\vec{\tau}$ is the stress tensor, τ_f is the friction forces and q is the heat flux. Contribution of the diffusive terms $\nabla \cdot (\phi K_{cv} \nabla C)$, $\nabla \cdot \vec{\tau}$ and $\nabla \cdot q$ are neglected.

2. FULL TIME AND SPACE DISCRETIZATION

For space discretization, a staggered grid (see figure 1) is used where scalar variables (pressure, density, enthalpy, *etc*) are computed at center of the control volumes. Velocity or momentum variables are computed on volume faces. It differs from a collocated grid, where all the variables are computed at the same position.

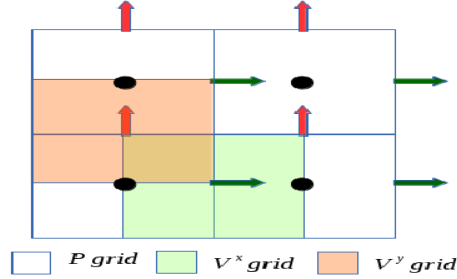


FIGURE 1. Staggered grid in 2-dimensions

Using a staggered grid is a simple way to avoid odd-even decoupling between pressure and velocity. Odd-even decoupling is a discretization error that can occur on collocated grids and which leads to checkerboard patterns in the solutions [15].

2.1. Discretization of the mixture mass equation

The **time discretization** of the mixture mass equation is based on a semi-implicit scheme. More precisely, the mass fluxes are approximated on the interface using a donor semi-implicit scheme where the velocity is implicit while the scalar variables are explicit. The **space discretization** in the three directions of the mass fluxes in the mixture mass equation is done by approximating the density on the cell faces by using a donor formulation.

More precisely, the finite volumes discretization of the mixture mass equation involves its integration in time between t_n and t_{n+1} and in space on an elementary control volume M_c^K (see figure 2):

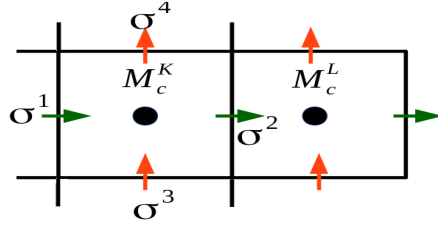
$$\int_{M_c^K} \int_{t_n}^{t_{n+1}} \left[\phi \frac{\partial \rho}{\partial t} + \nabla \cdot (\phi \rho \vec{V}) \right] d\Omega dt = 0. \quad (3)$$

By using the divergence theorem, equation (3) becomes:

$$\int_{M_c^K} \int_{t_n}^{t_{n+1}} \phi \frac{\partial \rho}{\partial t} d\Omega dt + \int_{\partial M_c^K} \int_{t_n}^{t_{n+1}} \phi \rho \vec{V} \cdot \vec{n} dS dt = 0 \quad (4)$$

or in discrete form:

$$\frac{\rho_{M_c^K}^{n+1} - \rho_{M_c^K}^n}{\Delta t} + \frac{1}{(\phi \nabla)_{M_c^K}} \sum_{\sigma \in \varepsilon_K} \mathcal{F}_\sigma^{n+1} = 0 \quad (5)$$

FIGURE 2. Control volume M_c^K in 2-dimensions

In (5), ε_K is the set of faces of M_c^K , $\mathbb{V}_{M_c^K}$ is the volume of M_c^K and $\mathcal{F}_\sigma^{n+1}$ is the approximation of the flux on the interface σ at time t_{n+1} .

To establish the discrete mixture mass equation, all we need now is to approximate the flux $\mathcal{F}_\sigma^{n+1}$ on the faces of a given cell M_c^K . To ensure the stability of the numerical scheme, we use a donor formulation of the convection term:

$$\mathcal{F}_\sigma^{n+1} = \phi_\sigma \mathbb{S}_\sigma \rho_\sigma^n \vec{V}_\sigma^{n+1} \cdot \vec{n}_\sigma. \quad (6)$$

In (6), $\mathbb{S}_\sigma$ is the crossing surface of σ , $\vec{n}_\sigma$ is the outward unitary normal of the face between the M_c^K and M_c^L cells and ρ_σ^n represents the upwind mixture density on the interface σ between a given cell M_c^K and a neighboring cell M_c^L :

$$\rho_\sigma^n = \begin{cases} \rho_{M_c^K}^n & \text{if } \vec{V}_\sigma^{n+1} \cdot \vec{n}_\sigma > 0, \\ \rho_{M_c^L}^n & \text{otherwise.} \end{cases}$$

As a result, the discrete form of the mixture mass equation (5) can be written as:

$$F^1(\rho_{M_c^K}^{n+1}, \vec{V}_{\sigma \in \varepsilon_K}^{n+1}) = 0. \quad (7)$$

Taking into account the state equation (2), equation (7) becomes:

$$F^1(P_{M_c^K}^{n+1}, h_{M_c^K}^{n+1}, \vec{V}_{\sigma \in \varepsilon_K}^{n+1}) = 0. \quad (8)$$

2.2. Discretization of the mixture internal energy balance equation

The **spatial and temporal discretization** of the mixture internal energy balance equation is done by using the approach used for the mixture mass equation.

The finite volumes discretization of the mixture internal energy equation involves its integration in time between t_n and t_{n+1} and in space on an elementary control volume M_c^K (see figure 2):

$$\int_{M_c^K} \int_{t_n}^{t_{n+1}} \left\{ \phi \frac{\partial \rho e}{\partial t} + \nabla \cdot (\phi \rho e \vec{V}) + P \nabla \cdot (\phi \vec{V}) + \nabla \cdot [(\phi \rho C(1-C)(H_v - H_l) \vec{V}_r)] - \phi Q \right\} d\Omega dt = 0. \quad (9)$$

The discrete form of (9) is:

$$\frac{(\rho e)_{M_c^K}^{n+1} - (\rho e)_{M_c^K}^n}{\Delta t} + \frac{1}{(\phi \mathbb{V})_{M_c^K}} \sum_{\sigma \in \varepsilon_K} [\mathcal{F}_\sigma^{n+1} + P_{M_c^K}^{n+1} \mathcal{G}_\sigma^{n+1} + \mathcal{H}_\sigma^{n+1}] - Q_{M_c^K}^n = 0 \quad (10)$$

where $\mathcal{F}_\sigma^{n+1}$, $\mathcal{G}_\sigma^{n+1}$ and $\mathcal{H}_\sigma^{n+1}$ are the approximations of the fluxes on the interface σ at time t_{n+1} :

$$\begin{cases} \mathcal{F}_\sigma^{n+1} &= \phi_\sigma \mathbb{S}_\sigma (\rho e)_\sigma^n \vec{V}_\sigma^{n+1} \cdot \vec{n}_\sigma, \\ \mathcal{G}_\sigma^{n+1} &= \phi_\sigma \mathbb{S}_\sigma \vec{V}_\sigma^{n+1} \cdot \vec{n}_\sigma, \\ \mathcal{H}_\sigma^{n+1} &= \phi_\sigma \mathbb{S}_\sigma [\rho_r C_r (1 - C_r) (H_v - H_l)]_\sigma^n (\vec{V}_r)_\sigma^{n+1} \cdot \vec{n}_\sigma. \end{cases}$$

- $(\rho e)_\sigma^n$ and $[\rho_r C_r(1 - C_r)(H_v - H_l)]_\sigma^n$ are defined only at the cells center. On the faces, they are approximated using the following donor formulation:

$$(\rho e)_\sigma^n = \begin{cases} (\rho e)_{M_c^K}^n & \text{if } \vec{V}_\sigma^{n+1} \cdot \vec{n}_\sigma > 0, \\ (\rho e)_{M_c^L}^n & \text{otherwise.} \end{cases}$$

$$[\rho_r C_r(1 - C_r)(H_v - H_l)]_\sigma^n = \begin{cases} [\rho C(1 - C)(H_v - H_l)]_{M_c^K}^n & \text{if } (\vec{V}_r)_\sigma^{n+1} \cdot \vec{n}_\sigma > 0, \\ [\rho C(1 - C)(H_v - H_l)]_{M_c^L}^n & \text{otherwise.} \end{cases}$$

- $(\vec{V}_r)_\sigma^{n+1}$ is the relative velocity which is given by using the Ishii model [9,10]:

$$(\vec{V}_r)_\sigma^{n+1} = \frac{(C_0 - 1)\vec{V}_\sigma^{n+1} + \vec{V}_{v,lim}}{1 - C_\sigma^n + C_0(C_\sigma^n - \alpha_\sigma^n)} \quad (11)$$

C_0 is a parameter that adjusts the mixture velocity and $\vec{V}_{v,lim}$ is the vapor velocity limit. The concentration C_σ^n and the void fraction α_σ^n on the interface σ are approximated by also using a donor formulation.

Hence, the discrete form of the mixture internal energy equation (10) can be written as:

$$F^2(\rho_{M_c^K}^{n+1}, e_{M_c^K}^{n+1}, \vec{V}_{\sigma \in \epsilon_K}^{n+1}, (\vec{V}_r)_{\sigma \in \epsilon_K}^{n+1}) = 0. \quad (12)$$

Taking into account the state equation (2) and the relation (11), equation (12) becomes:

$$F^2(P_{M_c^K}^{n+1}, h_{M_c^K}^{n+1}, \vec{V}_{\sigma \in \epsilon_K}^{n+1}) = 0. \quad (13)$$

2.3. Discretization of the vapor mass equation

The **spatial and temporal discretization** of the vapor mass balance equation is done by using the approach used for the mixture mass equation.

We integrate the vapor mass equation between the time instants t_n and t_{n+1} on the cell M_c^K (see figure 2):

$$\int_{M_c^K} \int_{t_n}^{t_{n+1}} \left\{ \phi \frac{\partial \rho C}{\partial t} + \nabla \cdot (\phi \rho C \vec{V}) + \nabla \cdot [\phi \rho C(1 - C) \vec{V}_r] - \phi \Gamma_v \right\} d\Omega dt = 0. \quad (14)$$

The discrete form of (14) is:

$$\frac{(\rho C)_{M_c^K}^{n+1} - (\rho C)_{M_c^K}^n}{\Delta t} + \frac{1}{(\phi \mathbb{V})_{M_c^K}} \sum_{\sigma \in \epsilon_K} [\mathcal{F}_\sigma^{n+1} + \mathcal{G}_\sigma^{n+1}] - (\Gamma_v)_{M_c^K}^{n+1} = 0 \quad (15)$$

where $\mathcal{F}_\sigma^{n+1}$ and $\mathcal{G}_\sigma^{n+1}$ are the approximations of the fluxes on the interface σ at time t_{n+1} :

$$\begin{cases} \mathcal{F}_\sigma^{n+1} &= \phi_\sigma \mathbb{S}_\sigma (\rho C)_\sigma^n \vec{V}_\sigma^{n+1} \cdot \vec{n}_\sigma, \\ \mathcal{G}_\sigma^{n+1} &= \phi_\sigma \mathbb{S}_\sigma [\rho_r C_r(1 - C_r)]_\sigma^n (\vec{V}_r)_\sigma^{n+1} \cdot \vec{n}_\sigma. \end{cases}$$

- $(\rho C)_\sigma^n$ and $[\rho_r C_r(1 - C_r)]_\sigma^n$ are defined only at the cells center. On the faces, they are approximated using the following donor formulation:

$$(\rho C)_\sigma^n = \begin{cases} (\rho C)_{M_c^K}^n & \text{if } \vec{V}_\sigma^{n+1} \cdot \vec{n}_\sigma > 0, \\ (\rho C)_{M_c^L}^n & \text{otherwise,} \end{cases}$$

$$[(\rho_r C_r(1 - C_r))^D]_\sigma^n = \begin{cases} [\rho C(1 - C)]_{M_c^K}^n & \text{if } (\vec{V}_r)_\sigma^{n+1} \cdot \vec{n}_\sigma > 0, \\ [\rho C(1 - C)]_{M_c^L}^n & \text{otherwise.} \end{cases}$$

- $(\Gamma_v)_{M_c^K}^{n+1}$ is calculated using a correlation [2].

As a result, the discrete form of the vapor mass equation (15) can be written as:

$$F^3(\rho_{M_c^K}^{n+1}, C_{M_c^K}^{n+1}, V_{\sigma \in \epsilon_K}^{n+1}, (\vec{V}_r)_{\sigma \in \epsilon_K}^{n+1}) = 0. \quad (16)$$

Taking into account the state equation (2) and the relation (11), the equation (16) becomes:

$$F^3(P_{M_c^K}^{n+1}, h_{M_c^K}^{n+1}, C_{M_c^K}^{n+1}, \vec{V}_{\sigma \in \epsilon_K}^{n+1}) = 0. \quad (17)$$

2.4. Discretization of the mixture momentum conservation equation

We solve the mixture momentum equation of (1) in the non-conservative form:

$$\phi \rho \left(\frac{\partial \vec{V}}{\partial t} + \vec{V} \cdot \nabla \vec{V} \right) + \nabla \cdot \left(\phi \rho C(1-C) \vec{V}_r \otimes \vec{V}_r \right) + \phi \nabla P = \phi \vec{\tau}_f + \phi \rho \vec{g}. \quad (18)$$

The equation (18) can be divided by the porosity which then remains only in the $\nabla \cdot \left(\phi \rho C(1-C) \vec{V}_r \otimes \vec{V}_r \right)$ term. In this article, we assume that the porosity is constant, the above equation (18) becomes:

$$\rho \frac{\partial \vec{V}}{\partial t} + \rho \vec{V} \nabla \vec{V} + \nabla \cdot \left(\rho C(1-C) \vec{V}_r \otimes \vec{V}_r \right) + \nabla P = \vec{\tau}_f + \rho \vec{g}. \quad (19)$$

Future work will be conducted to raise this hypothesis and discretize the term $\frac{1}{\phi} \nabla \cdot \left(\phi \rho C(1-C) \vec{V}_r \otimes \vec{V}_r \right)$.

Using the formula $\rho \vec{V} \cdot \nabla \vec{V} = \nabla \cdot \left(\rho \vec{V} \otimes \vec{V} \right) - \vec{V} \nabla \cdot \left(\rho \vec{V} \right)$, the mixture momentum equation (19) can be written as:

$$\rho \frac{\partial \vec{V}}{\partial t} + \nabla \cdot \left(\rho \vec{V} \otimes \vec{V} \right) - \vec{V} \nabla \cdot \left(\rho \vec{V} \right) + \nabla \cdot \left(\rho C(1-C) \vec{V}_r \otimes \vec{V}_r \right) + \nabla P = \vec{\tau}_f + \rho \vec{g} \quad (20)$$

In the sequel, we detail the spatial and temporal discretization of the equation (20) projected in the direction $\vec{e}_x$ (the discretization in the directions $\vec{e}_y$ and $\vec{e}_z$, is obtained by analogy).

The projection of equation (20) in the direction $\vec{e}_x$ gives:

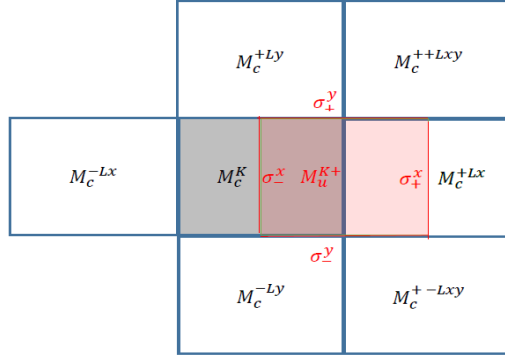
$$\rho \frac{\partial V^x}{\partial t} + \nabla \cdot (\rho V^x \vec{V}) - V^x \nabla \cdot (\rho \vec{V}) + \nabla \cdot \left[\rho C(1-C) V_r^x \vec{V}_r \right] + \frac{\partial P}{\partial x} = \tau_f^x + \rho g^x. \quad (21)$$

The finite volumes discretization involves the integration of equation (20) in time between t_n and t_{n+1} and in space on an elementary control volume M_u^{K+} (see figure 3):

$$\int_{M_u^{K+}} \int_{t_n}^{t_{n+1}} \left\{ \rho \frac{\partial V^x}{\partial t} + \nabla \cdot (\rho V^x \vec{V}) - V^x \nabla \cdot (\rho \vec{V}) + \nabla \cdot \left[\rho C(1-C) V_r^x \vec{V}_r \right] + \frac{\partial P}{\partial x} - \tau_f^x - \rho g^x \right\} d\Omega dt = 0.$$

The discrete form is:

$$\begin{aligned} \rho_{M_u^{K+}}^n \frac{(V^x)_{M_u^{K+}}^{n+1} - (V^x)_{M_u^{K+}}^n}{\Delta t} + \frac{1}{\mathbb{V}_{M_u^{K+}}} \sum_{\sigma \in \epsilon_M} [\mathcal{F}_\sigma^n - (V^x)_{M_u^{K+}}^n \mathcal{G}_\sigma^n + \mathcal{H}_\sigma^n] \\ + \left(\frac{\partial P}{\partial x} \right)_{M_u^{K+}}^{n+1} - (\tau_f^x)_{M_u^{K+}}^{n+1} - (\rho g^x)_{M_u^{K+}}^n = 0 \end{aligned} \quad (22)$$

FIGURE 3. control volume M_u^{K+} in 2-dimensions

ε_M is the set of faces of M_u^{K+} and $V_{M_u^{K+}}$ is the volume of M_u^{K+} . $\mathcal{F}_\sigma^n$, $\mathcal{G}_\sigma^n$ and $\mathcal{H}_\sigma^n$ are the approximations of the fluxes at the interface σ at time t_n :

$$\begin{cases} \mathcal{F}_\sigma^n &= \mathbb{S}_\sigma \rho_\sigma^n (V^x)_\sigma^n \vec{V}_\sigma^n \cdot \vec{n}_\sigma, \\ \mathcal{G}_\sigma^n &= \mathbb{S}_\sigma \rho_\sigma^n \vec{V}_\sigma^n \cdot \vec{n}_\sigma, \\ \mathcal{H}_\sigma^n &= \mathbb{S}_\sigma [\rho_r C_r (1 - C_r)]_\sigma^n (V_r^x)_\sigma^n (\vec{V}_r)_\sigma^n \cdot \vec{n}_\sigma. \end{cases}$$

We now detail each terms in 2D for simplification reasons.

- Approximation of pressure gradient $(\frac{\partial P}{\partial x})_{M_u^{K+}}^{n+1}$:

$$\left(\frac{\partial P}{\partial x}\right)_{M_u^{K+}}^{n+1} = \frac{P_{M_c^{+Lx}}^{n+1} - P_{M_c^K}^{n+1}}{\Delta x}$$

- Approximation of $\vec{V}_\sigma^n$ and $(V^x)_\sigma^n$ at the interfaces of M_u^{K+} :

Interface σ_x $\vec{V}_{\sigma_+^x}^n = \frac{\vec{V}_{M_u^{K+}}^n + \vec{V}_{M_u^{+Lx}}^n}{2}$ $\vec{V}_{\sigma_-^x}^n = \frac{\vec{V}_{M_u^{K+}}^n + \vec{V}_{M_u^{-Lx}}^n}{2}$ $(V^x)_{\sigma_+^x}^n = \begin{cases} (V^x)_{M_u^{K+}}^n & \text{if } \vec{V}_{\sigma_+^x}^n \cdot \vec{n}_{\sigma_+^x} > 0 \\ (V^x)_{M_u^{+Lx}}^n & \text{otherwise} \end{cases}$ $(V^x)_{\sigma_-^x}^n = \begin{cases} (V^x)_{M_u^{K+}}^n & \text{if } \vec{V}_{\sigma_-^x}^n \cdot \vec{n}_{\sigma_-^x} > 0 \\ (V^x)_{M_u^{K-}}^n & \text{otherwise} \end{cases}$	Interface σ_y $\vec{V}_{\sigma_+^y}^n = \frac{\vec{V}_{M_v^K}^n + \vec{V}_{M_v^{+Lx}}^n}{2}$ $\vec{V}_{\sigma_-^y}^n = \frac{\vec{V}_{M_v^{-Ly}}^n + \vec{V}_{M_v^{+-Lxy}}^n}{2}$ $(V^x)_{\sigma_+^y}^n = \begin{cases} (V^x)_{M_u^{K+}}^n & \text{if } \vec{V}_{\sigma_+^y}^n \cdot \vec{n}_{\sigma_+^y} > 0 \\ (V^x)_{M_u^{+Ly}}^n & \text{otherwise} \end{cases}$ $(V^x)_{\sigma_-^y}^n = \begin{cases} (V^x)_{M_u^{K+}}^n & \text{if } \vec{V}_{\sigma_-^y}^n \cdot \vec{n}_{\sigma_-^y} > 0 \\ (V^x)_{M_u^{-Ly}}^n & \text{otherwise} \end{cases}$
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- Approximation of relative velocity: $(\vec{V}_r)_\sigma^n$ and $(V_r^x)_\sigma^n$ at the interfaces of M_u^{K+} :
We use the Ishii model [9, 10]:

$$(\vec{V}_r)_\sigma^n = \frac{(C_0 - 1) \vec{V}_\sigma^n + \vec{V}_{v,lim}}{1 - C_\sigma^n + C_0(C_\sigma^n - \alpha_\sigma^n)}$$

$$\begin{aligned} (V_r^x)_{\sigma_+^x}^n &= \begin{cases} (V_r^x)_{M_u^{K+}}^n & \text{if } (\vec{V}_r)_{\sigma_+^x}^n \cdot \vec{n}_{\sigma_+^x} > 0, \\ (V_r^x)_{M_u^{+Lx}}^n & \text{otherwise,} \end{cases} & (V_r^x)_{\sigma_-^x}^n &= \begin{cases} (V_r^x)_{M_u^{K+}}^n & \text{if } (\vec{V}_r)_{\sigma_-^x}^n \cdot \vec{n}_{\sigma_-^x} > 0, \\ (V_r^x)_{M_u^{K-}}^n & \text{otherwise,} \end{cases} \\ (V_r^x)_{\sigma_+^y}^n &= \begin{cases} (V_r^x)_{M_u^{K+}}^n & \text{if } (\vec{V}_r)_{\sigma_+^y}^n \cdot \vec{n}_{\sigma_+^y} > 0, \\ (V_r^x)_{M_u^{+Ly}}^n & \text{otherwise,} \end{cases} & (V_r^x)_{\sigma_-^y}^n &= \begin{cases} (V_r^x)_{M_u^{K+}}^n & \text{if } (\vec{V}_r)_{\sigma_-^y}^n \cdot \vec{n}_{\sigma_-^y} > 0, \\ (V_r^x)_{M_u^{-Ly}}^n & \text{otherwise.} \end{cases} \end{aligned}$$

- Approximation of the scalar variables at the interfaces of M_u^{K+} :

$$\rho_{\sigma_-^x}^n = \rho_{M_c^K}^n, \quad \rho_{\sigma_+^x}^n = \rho_{M_c^{+Lx}}^n,$$

$$\rho_{\sigma_+^y}^n = \begin{cases} \frac{\rho_{M_c^K}^n + \rho_{M_c^{+Lx}}^n}{2} & \text{if } \vec{V}_{\sigma_+^y}^n \cdot \vec{n}_{\sigma_+^y} > 0, \\ \frac{\rho_{M_c^{+Ly}}^n + \rho_{M_c^{++Lxy}}^n}{2} & \text{otherwise,} \end{cases} \quad \rho_{\sigma_-^y}^n = \begin{cases} \frac{\rho_{M_c^K}^n + \rho_{M_c^{+Lx}}^n}{2} & \text{if } \vec{V}_{\sigma_-^y}^n \cdot \vec{n}_{\sigma_-^y} > 0, \\ \frac{\rho_{M_c^{-Ly}}^n + \rho_{M_c^{+-Lxy}}^n}{2} & \text{otherwise.} \end{cases}$$

We use the same method to determine $[\rho_r C_r (1 - C_r)]_{\sigma}^n$:

$$[\rho_r C_r (1 - C_r)]_{\sigma_-^x}^n = [\rho C (1 - C)]_{M_c^K}^n, \quad [\rho_r C_r (1 - C_r)]_{\sigma_+^x}^n = [\rho C (1 - C)]_{M_c^{+Lx}}^n,$$

$$[\rho_r C_r (1 - C_r)]_{\sigma_+^y}^n = \begin{cases} \frac{[\rho C (1 - C)]_{M_c^K}^n + [\rho C (1 - C)]_{M_c^{+Lx}}^n}{2} & \text{if } (\vec{V}_r)_{\sigma_+^y}^n \cdot \vec{n}_{\sigma_+^y} > 0, \\ \frac{[\rho C (1 - C)]_{M_c^{+Ly}}^n + [\rho C (1 - C)]_{M_c^{++Lxy}}^n}{2} & \text{otherwise,} \end{cases}$$

$$[\rho_r C_r (1 - C_r)]_{\sigma_-^y}^n = \begin{cases} \frac{[\rho C (1 - C)]_{M_c^K}^n + [\rho C (1 - C)]_{M_c^{+Lx}}^n}{2} & \text{if } (\vec{V}_r)_{\sigma_-^y}^n \cdot \vec{n}_{\sigma_-^y} > 0, \\ \frac{[\rho C (1 - C)]_{M_c^{-Ly}}^n + [\rho C (1 - C)]_{M_c^{+-Lxy}}^n}{2} & \text{otherwise.} \end{cases}$$

At the interfaces σ_+^z and σ_-^z , we easily get the same result as at the interfaces σ_+^y and σ_-^y if we replace y by z .

- Approximation of friction forces $(\tau_f^x)_{M_u^{K+}}^{n+1}$:

$$(\tau_f^x)_{M_u^{K+}}^{n+1} = (\tau_{fw}^x)_{M_u^{K+}}^{n+1} + (\tau_{fs}^x)_{M_u^{K+}}^{n+1}$$

where τ_{fw}^x is the wall friction and τ_{fs}^x is the singular friction. We obtain:

$$(\tau_w^x)_{M_u^{K+}}^{n+1} = \frac{-f_w^x}{2(D_h^x)_{M_u^{K+}}} \rho_{M_u^{K+}}^n (V^x)_{M_u^{K+}}^{n+1} |(V^x)_{M_u^{K+}}^{n+1}|,$$

$$(\tau_s^x)_{M_u^{K+}}^{n+1} = \frac{-K^x}{2} \rho_{M_u^{K+}}^n (V^x)_{M_u^{K+}}^{n+1} |(V^x)_{M_u^{K+}}^{n+1}|$$

where K^x and f_w^x are the friction coefficients.

Finally, the discretization of the mixture momentum equation in the direction e_x^r (22) can be written as:

$$F^4(P_{\mathcal{M}_c^K}^{n+1}, P_{\mathcal{M}_c^{+Lx}}^{n+1}, (V^x)_{\mathcal{M}_c^K}^{n+1}) = 0. \quad (23)$$

By analogy, we obtain the discretization in the directions e_y^r and e_z^r :

$$F^5(P_{\mathcal{M}_c^K}^{n+1}, P_{\mathcal{M}_c^{+Ly}}^{n+1}, (V^y)_{\mathcal{M}_c^K}^{n+1}) = 0, \quad (24)$$

$$F^6(P_{\mathcal{M}_c^K}^{n+1}, P_{\mathcal{M}_c^{+Lz}}^{n+1}, (V^z)_{\mathcal{M}_c^K}^{n+1}) = 0. \quad (25)$$

3. SOLUTION ALGORITHM

3.1. Construction of the linear system to solve

Let (S) denote the non-linear system we ought to solve at each physical time step:

$$(S) \begin{cases} F^1(P, h, \vec{V}) = 0, \\ F^2(P, h, C, \vec{V}) = 0, \\ F^3(P, h, \vec{V}) = 0, \\ F^4(P, \vec{V}) = 0, \\ F^5(P, \vec{V}) = 0, \\ F^6(P, \vec{V}) = 0. \end{cases} \quad (26)$$

System (S) is solved by using a Newton-Raphson iterative method which consists in solving a linearisation of (S) at each iteration. More precisely, at each iteration k of the Newton-Raphson algorithm, we solve the linear system:

$$\mathcal{J}(\mathcal{U}^k) \Delta \mathcal{U}^{k+1} = \mathcal{S}(\mathcal{U}^n, \mathcal{U}^k) \quad (27)$$

where $\mathcal{U} = (P, h, C, V^x, V^y, V^z)^t$ is unknown vector and $\Delta \mathcal{U}^{k+1} = \mathcal{U}^{k+1} - \mathcal{U}^k$ is increment of $\mathcal{U}$, and where k is the number of the iteration, the matrix $\mathcal{J}$ is the Jacobian matrix of the system (S) and the vector $\mathcal{S}$ is the right-hand-side vector containing the residuals of equations (26) evaluated at the previous iteration. The solution $\mathcal{U}^{n+1}$ is $\mathcal{U}^k$ when $k \rightarrow +\infty$.

To solve the non-linear system (26), we compare two different methods:

- the “Full Jacobian” method (see §3.2),
- the “Pressure-based Solver” method (see §3.3).

These methods are used by the CATHARE code to solve the six equations model [6]. The Full Jacobian method is used to deal with the 1D problems since the size of the matrix allows it. However, in the 2D and 3D problems CATHARE code uses the pressure-based method.

3.2. The “Full Jacobian” method

This method involves the inversion of the matrix in (26) when its size is reasonable. Actually in this case this method is very useful since it is simple to implement and because it allows the possibility of “impliciting” all the variables in the discretization step which leads to a better resolution.

Despite the efficiency of the full Jacobian method to treat the “small sized” problems, its use is bounded by a limit on the jacobian matrix size. Beyond this limit, the pressure-based method becomes more efficient.

3.3. The “pressure-based solver” method

The “semi-implicit” scheme we used to discretize the four equations (1) allows to simplify significantly the terms of the matrix that occur in the momentum equations F^4 , F^5 and F^6 . This will enable the expression of the velocity increments as functions of the pressure increments (see section 3.3.1) and then to eliminate them. In section §3.3.2 we will see how to eliminate all the scalar variables (but the pressure increments) and then to obtain a linear equation where only the pressure increments should occur.

3.3.1. Elimination of the velocity increments

The purpose of this step is to write the velocity increments as a function of the pressure increments. To do so we consider only the momentum equations which corresponds to this “partial” linear system:

$$\begin{pmatrix} \frac{\partial F^4}{\partial P} & \frac{\partial F^4}{\partial h} & \frac{\partial F^4}{\partial C} & \frac{\partial F^4}{\partial V^x} & \frac{\partial F^4}{\partial V^y} & \frac{\partial F^4}{\partial V^z} \\ \frac{\partial F^5}{\partial P} & \frac{\partial F^5}{\partial h} & \frac{\partial F^5}{\partial C} & \frac{\partial F^5}{\partial V^x} & \frac{\partial F^5}{\partial V^y} & \frac{\partial F^5}{\partial V^z} \\ \frac{\partial F^6}{\partial P} & \frac{\partial F^6}{\partial h} & \frac{\partial F^6}{\partial C} & \frac{\partial F^6}{\partial V^x} & \frac{\partial F^6}{\partial V^y} & \frac{\partial F^6}{\partial V^z} \end{pmatrix} \begin{pmatrix} \Delta \mathcal{U}_1 \\ \Delta \mathcal{U}_2 \\ \Delta \mathcal{U}_3 \\ \Delta \mathcal{U}_4 \\ \Delta \mathcal{U}_5 \\ \Delta \mathcal{U}_6 \end{pmatrix} = \begin{pmatrix} S^4 \\ S^5 \\ S^6 \end{pmatrix} \quad (28)$$

According to (23),(24) and (25), the functions F^4 , F^5 and F^6 do not depend on mixture enthalpy h and mass vapor concentration C at time step t^{n+1} . Thus, their derivatives with respect to these variables are equals to zero. In the same way:

- the derivatives of F^4 with respect to V^y and V^z are equal to zero,
- the derivatives of F^5 with respect to V^x and V^z are equal to zero,
- the derivatives of F^6 with respect to V^x and V^y are equal to zero.

Thus, system (28) becomes:

$$\begin{pmatrix} \frac{\partial F^4}{\partial P} & 0 & 0 & \frac{\partial F^4}{\partial V^x} & 0 & 0 \\ \frac{\partial F^5}{\partial P} & 0 & 0 & 0 & \frac{\partial F^5}{\partial V^y} & 0 \\ \frac{\partial F^6}{\partial P} & 0 & 0 & 0 & 0 & \frac{\partial F^6}{\partial V^z} \end{pmatrix} \begin{pmatrix} \Delta \mathcal{U}_1 \\ \Delta \mathcal{U}_2 \\ \Delta \mathcal{U}_3 \\ \Delta \mathcal{U}_4 \\ \Delta \mathcal{U}_5 \\ \Delta \mathcal{U}_6 \end{pmatrix} = \begin{pmatrix} S^4 \\ S^5 \\ S^6 \end{pmatrix} \quad (29)$$

Moreover, by developing equation (29) in the cells M_u^{K+} , M_v^{K+} and M_w^{K+} , we obtain the following equations system:

$$\left\{ \begin{array}{l} (\Delta V^x)_{M_u^{K+}} = \frac{1}{\frac{\partial F^4}{\partial P} \frac{M_u^{K+}}{M_u^{K+}}} [S^4_{M_u^{K+}} - \frac{\partial F^4}{\partial P_{M_c^K}} (\Delta P)_{M_c^K} - \frac{\partial F^4}{\partial P_{M_c^{+Lx}}} (\Delta P)_{M_c^{+Lx}}], \\ (\Delta V^y)_{M_v^{K+}} = \frac{1}{\frac{\partial F^5}{\partial P} \frac{M_v^{K+}}{M_v^{K+}}} [S^5_{M_v^{K+}} - \frac{\partial F^5}{\partial P_{M_c^K}} (\Delta P)_{M_c^K} - \frac{\partial F^5}{\partial P_{M_c^{+Ly}}} (\Delta P)_{M_c^{+Ly}}], \\ (\Delta V^z)_{M_w^{K+}} = \frac{1}{\frac{\partial F^6}{\partial P} \frac{M_w^{K+}}{M_w^{K+}}} [S^6_{M_w^{K+}} - \frac{\partial F^6}{\partial P_{M_c^K}} (\Delta P)_{M_c^K} - \frac{\partial F^6}{\partial P_{M_c^{+Lz}}} (\Delta P)_{M_c^{+Lz}}]. \end{array} \right. \quad (30)$$

By analogy, we determine the velocity increments $(\Delta V^x)_{M_u^{K-}}$, $(\Delta V^y)_{M_v^{K-}}$ and $(\Delta V^z)_{M_w^{K-}}$ as functions of the pressure increments.

This step enabled the writing of the velocity increments $\Delta \mathcal{U}_4$, $\Delta \mathcal{U}_5$ and $\Delta \mathcal{U}_6$ at each face of the mesh as functions of the pressure increments. This will be useful in the next step (see §3.3.2) to establish a linear pressure equation (such as only pressure increments are unknown).

3.3.2. Triangulation

In this step we aim to eliminate the scalar variables increments. To do so, we use the three scalar variables equations (mixture mass, mass vapor concentration and mixture energy), which corresponds to the following system:

$$\begin{pmatrix} \frac{\partial F^1}{\partial P} & \frac{\partial F^1}{\partial h} & \frac{\partial F^1}{\partial C} & \frac{\partial F^1}{\partial V^x} & \frac{\partial F^1}{\partial V^y} & \frac{\partial F^1}{\partial V^z} \\ \frac{\partial F^2}{\partial P} & \frac{\partial F^2}{\partial h} & \frac{\partial F^2}{\partial C} & \frac{\partial F^2}{\partial V^x} & \frac{\partial F^2}{\partial V^y} & \frac{\partial F^2}{\partial V^z} \\ \frac{\partial F^3}{\partial P} & \frac{\partial F^3}{\partial h} & \frac{\partial F^3}{\partial C} & \frac{\partial F^3}{\partial V^x} & \frac{\partial F^3}{\partial V^y} & \frac{\partial F^3}{\partial V^z} \end{pmatrix} \begin{pmatrix} \Delta \mathcal{U}_1 \\ \Delta \mathcal{U}_2 \\ \Delta \mathcal{U}_3 \\ \Delta \mathcal{U}_4 \\ \Delta \mathcal{U}_5 \\ \Delta \mathcal{U}_6 \end{pmatrix} = \begin{pmatrix} S^1 \\ S^2 \\ S^3 \end{pmatrix} \quad (31)$$

As we did previously, some simplifications take place (thanks to (8) and (13)) since F^1 and F^2 do not depend on C at t_{n+1} . Thus, system (31) becomes:

$$\begin{pmatrix} \frac{\partial F^1}{\partial P} & \frac{\partial F^1}{\partial h} & 0 & \frac{\partial F^1}{\partial V^x} & \frac{\partial F^1}{\partial V^y} & \frac{\partial F^1}{\partial V^z} \\ \frac{\partial F^2}{\partial P} & \frac{\partial F^2}{\partial h} & 0 & \frac{\partial F^2}{\partial V^x} & \frac{\partial F^2}{\partial V^y} & \frac{\partial F^2}{\partial V^z} \\ \frac{\partial F^3}{\partial P} & \frac{\partial F^3}{\partial h} & \frac{\partial F^3}{\partial C} & \frac{\partial F^3}{\partial V^x} & \frac{\partial F^3}{\partial V^y} & \frac{\partial F^3}{\partial V^z} \end{pmatrix} \begin{pmatrix} \Delta \mathcal{U}_1 \\ \Delta \mathcal{U}_2 \\ \Delta \mathcal{U}_3 \\ \Delta \mathcal{U}_4 \\ \Delta \mathcal{U}_5 \\ \Delta \mathcal{U}_6 \end{pmatrix} = \begin{pmatrix} S^1 \\ S^2 \\ S^3 \end{pmatrix} \quad (32)$$

At this stage applying the operation $(L^1) \leftarrow (L^1) \times \frac{\partial F^2}{\partial h} - (L^2) \times \frac{\partial F^1}{\partial h}$ on the system (32) results in:

$$\begin{pmatrix} J^{1,1} & 0 & 0 & J^{1,4} & J^{1,5} & J^{1,6} \\ \frac{\partial F^2}{\partial P} & \frac{\partial F^2}{\partial h} & 0 & \frac{\partial F^2}{\partial V^x} & \frac{\partial F^2}{\partial V^y} & \frac{\partial F^2}{\partial V^z} \\ \frac{\partial F^3}{\partial P} & \frac{\partial F^3}{\partial h} & \frac{\partial F^3}{\partial C} & \frac{\partial F^3}{\partial V^x} & \frac{\partial F^3}{\partial V^y} & \frac{\partial F^3}{\partial V^z} \end{pmatrix} \begin{pmatrix} \Delta \mathcal{U}_1 \\ \Delta \mathcal{U}_2 \\ \Delta \mathcal{U}_3 \\ \Delta \mathcal{U}_4 \\ \Delta \mathcal{U}_5 \\ \Delta \mathcal{U}_6 \end{pmatrix} = \begin{pmatrix} D^1 \\ S^2 \\ S^3 \end{pmatrix} \quad (33)$$

where:

$$D_{M_c^K}^1 = S_{M_c^K}^1 \frac{\partial F_{M_c^K}^2}{\partial h_{M_c^K}} - S_{M_c^K}^2 \frac{\partial F_{M_c^K}^1}{\partial h_{M_c^K}}$$

$$\begin{aligned}
J_{M_u^{K+}}^{1,4} &= \left(\frac{\partial F_{M_c^K}^2}{\partial h_{M_c^K}} \frac{\partial F_{M_u^{K+}}^1}{\partial V_{M_u^{K+}}^x} \right) - \left(\frac{\partial F_{M_c^K}^1}{\partial h_{M_c^K}} \frac{\partial F_{M_u^{K+}}^2}{\partial V_{M_u^{K+}}^x} \right) & J_{M_w^{K+}}^{1,6} &= \left(\frac{\partial F_{M_c^K}^2}{\partial h_{M_c^K}} \frac{\partial F_{M_w^{K+}}^1}{\partial V_{M_w^{K+}}^z} \right) - \left(\frac{\partial F_{M_c^K}^1}{\partial h_{M_c^K}} \frac{\partial F_{M_w^{K+}}^2}{\partial V_{M_w^{K+}}^z} \right) \\
J_{M_v^{K+}}^{1,5} &= \left(\frac{\partial F_{M_c^K}^2}{\partial h_{M_c^K}} \frac{\partial F_{M_v^{K+}}^1}{\partial V_{M_v^{K+}}^y} \right) - \left(\frac{\partial F_{M_c^K}^1}{\partial h_{M_c^K}} \frac{\partial F_{M_v^{K+}}^2}{\partial V_{M_v^{K+}}^y} \right) & J_{M_c^K}^{1,1} &= \left(\frac{\partial F_{M_c^K}^2}{\partial h_{M_c^K}} \frac{\partial F_{M_c^K}^1}{\partial P_{M_c^K}} \right) - \left(\frac{\partial F_{M_c^K}^1}{\partial h_{M_c^K}} \frac{\partial F_{M_c^K}^2}{\partial P_{M_c^K}} \right)
\end{aligned}$$

By analogy, we determine the $J_{M_u^{K-}}^{1,4}$, $J_{M_v^{K-}}^{1,5}$ and $J_{M_w^{K-}}^{1,6}$ terms.

By developing, the first row of system (33) in a cell M_c^K , we get the following equation:

$$\begin{aligned}
& (J^{1,1})_{M_c^K} (\Delta P)_{M_c^K} + (J^{1,4})_{M_u^{K+}} (\Delta V^x)_{M_u^{K+}} + (J^{1,4})_{M_u^{K-}} (\Delta V^x)_{M_u^{K-}} \\
& + (J^{1,5})_{M_v^{K+}} (\Delta V^y)_{M_v^{K+}} + (J^{1,5})_{M_v^{K-}} (\Delta V^y)_{M_v^{K-}} \\
& + (J^{1,6})_{M_w^{K+}} (\Delta V^z)_{M_w^{K+}} + (J^{1,6})_{M_w^{K-}} (\Delta V^z)_{M_w^{K-}} = D_{M_c^K}^1
\end{aligned} \tag{34}$$

It is at this stage that we use of the velocity increments calculated in the last step with (30). Putting (30) in (34), we obtain:

$$\begin{aligned}
& \mathbb{A}(\Delta P)_{M_c^K} + \mathbb{B}(\Delta P)_{M_c^{+Lx}} + \mathbb{C}(\Delta P)_{M_c^{-Ly}} \\
& + \mathbb{D}(\Delta P)_{M_c^{+Ly}} + \mathbb{E}(\Delta P)_{M_c^{-Lz}} \\
& + \mathbb{F}(\Delta P)_{M_c^{+Lz}} + \mathbb{G}(\Delta P)_{M_c^{-Lz}} = \mathbb{S}
\end{aligned} \tag{35}$$

where:

$$\begin{aligned}
\mathbb{A} &= (J^{1,1})_{M_c^K} - (J^{1,4})_{M_u^{K+}} \frac{\frac{\partial F_{M_u^{K+}}^4}{\partial P_{M_c^K}}}{\frac{\partial F_{M_u^{K+}}^4}{\partial V_{M_u^{K+}}^x}} - (J^{1,4})_{M_u^{K-}} \frac{\frac{\partial F_{M_u^{K-}}^4}{\partial P_{M_c^K}}}{\frac{\partial F_{M_u^{K-}}^4}{\partial V_{M_u^{K-}}^x}} - (J^{1,5})_{M_v^{K+}} \frac{\frac{\partial F_{M_v^{K+}}^5}{\partial P_{M_c^K}}}{\frac{\partial F_{M_v^{K+}}^5}{\partial V_{M_v^{K+}}^y}} - (J^{1,5})_{M_v^{K-}} \frac{\frac{\partial F_{M_v^{K-}}^5}{\partial P_{M_c^K}}}{\frac{\partial F_{M_v^{K-}}^5}{\partial V_{M_v^{K-}}^y}} \\
& - (J^{1,6})_{M_w^{K+}} \frac{\frac{\partial F_{M_w^{K+}}^6}{\partial P_{M_c^K}}}{\frac{\partial F_{M_w^{K+}}^6}{\partial V_{M_w^{K+}}^z}} - (J^{1,6})_{M_w^{K-}} \frac{\frac{\partial F_{M_w^{K-}}^6}{\partial P_{M_c^K}}}{\frac{\partial F_{M_w^{K-}}^6}{\partial V_{M_w^{K-}}^z}}, \\
\mathbb{B} &= -(J^{1,4})_{M_u^{K+}} \frac{\frac{\partial F_{M_u^{K+}}^4}{\partial P_{M_c^{+Lx}}}}{\frac{\partial F_{M_u^{K+}}^4}{\partial V_{M_u^{K+}}^x}}, & \mathbb{D} &= -(J^{1,5})_{M_v^{K+}} \frac{\frac{\partial F_{M_v^{K+}}^5}{\partial P_{M_c^{+Ly}}}}{\frac{\partial F_{M_v^{K+}}^5}{\partial V_{M_v^{K+}}^y}}, & \mathbb{F} &= -(J^{1,6})_{M_w^{K+}} \frac{\frac{\partial F_{M_w^{K+}}^6}{\partial P_{M_c^{+Lz}}}}{\frac{\partial F_{M_w^{K+}}^6}{\partial V_{M_w^{K+}}^z}}, \\
\mathbb{C} &= -(J^{1,4})_{M_u^{K-}} \frac{\frac{\partial F_{M_u^{K-}}^4}{\partial P_{M_c^{-Ly}}}}{\frac{\partial F_{M_u^{K-}}^4}{\partial V_{M_u^{K-}}^x}}, & \mathbb{E} &= -(J^{1,5})_{M_v^{K-}} \frac{\frac{\partial F_{M_v^{K-}}^5}{\partial P_{M_c^{-Lz}}}}{\frac{\partial F_{M_v^{K-}}^5}{\partial V_{M_v^{K-}}^y}}, & \mathbb{G} &= -(J^{1,6})_{M_w^{K-}} \frac{\frac{\partial F_{M_w^{K-}}^6}{\partial P_{M_c^{-Lz}}}}{\frac{\partial F_{M_w^{K-}}^6}{\partial V_{M_w^{K-}}^z}}, \\
\mathbb{S} &= D_{M_c^K}^1 - \left[\frac{(J^{1,4})_{M_u^{K+}} S_{M_u^{K+}}^4}{\frac{\partial F_{M_u^{K+}}^4}{\partial V_{M_u^{K+}}^x}} + \frac{(J^{1,4})_{M_u^{K-}} S_{M_u^{K-}}^4}{\frac{\partial F_{M_u^{K-}}^4}{\partial V_{M_u^{K-}}^x}} + \frac{(J^{1,5})_{M_v^{K+}} S_{M_v^{K+}}^5}{\frac{\partial F_{M_v^{K+}}^5}{\partial V_{M_v^{K+}}^y}} + \frac{(J^{1,5})_{M_v^{K-}} S_{M_v^{K-}}^5}{\frac{\partial F_{M_v^{K-}}^5}{\partial V_{M_v^{K-}}^y}} \right. \\
& \quad \left. + \frac{(J^{1,6})_{M_w^{K+}} S_{M_w^{K+}}^6}{\frac{\partial F_{M_w^{K+}}^6}{\partial V_{M_w^{K+}}^z}} + \frac{(J^{1,6})_{M_w^{K-}} S_{M_w^{K-}}^6}{\frac{\partial F_{M_w^{K-}}^6}{\partial V_{M_w^{K-}}^z}} \right].
\end{aligned}$$

The resolution of the pressure equation (35) gives the pressure increments $\Delta\mathcal{U}_1$. Then, velocity increments $\Delta\mathcal{U}_4$, $\Delta\mathcal{U}_5$ and $\Delta\mathcal{U}_6$ is computed by using (30).

3.3.3. Enthalpy and concentration Increments

To compute the enthalpy increments, all we need is to develop the second row of system (33):

$$\begin{aligned} \frac{\partial F_{M_c^K}^2}{\partial P_{M_c^K}}(\Delta P)_{M_c^K} + \frac{\partial F_{M_c^K}^2}{\partial h_{M_c^K}}(\Delta h)_{M_c^K} + \frac{\partial F_{M_c^K}^2}{\partial (V^x)_{M_u^{K+}}}(\Delta V^x)_{M_u^{K+}} + \frac{\partial F_{M_c^K}^2}{\partial (V^x)_{M_u^{K-}}}(\Delta V^x)_{M_u^{K-}} \\ + \frac{\partial F_{M_c^K}^2}{\partial (V^y)_{M_v^{K+}}}(\Delta V^y)_{M_v^{K+}} + \frac{\partial F_{M_c^K}^2}{\partial (V^y)_{M_v^{K-}}}(\Delta V^y)_{M_v^{K-}} \\ + \frac{\partial F_{M_c^K}^2}{\partial (V^z)_{M_w^{K+}}}(\Delta V^z)_{M_w^{K+}} + \frac{\partial F_{M_c^K}^2}{\partial (V^z)_{M_w^{K-}}}(\Delta V^z)_{M_w^{K-}} = S_{M_c^K}^2. \end{aligned} \quad (36)$$

In equation (36), the pressure increments and the velocity increments are known (see §3.3.2). Then only the enthalpy increments are unknown. They are computed as follows:

$$\begin{aligned} (\Delta h)_{M_c^K} = \frac{1}{\frac{\partial F_{M_c^K}^2}{\partial h_{M_c^K}}} \left[S_{M_c^K}^2 - \frac{\partial F_{M_c^K}^2}{\partial P_{M_c^K}}(\Delta P)_{M_c^K} - \frac{\partial F_{M_c^K}^2}{\partial (V^x)_{M_u^{K+}}}(\Delta V^x)_{M_u^{K+}} - \frac{\partial F_{M_c^K}^2}{\partial (V^x)_{M_u^{K-}}}(\Delta V^x)_{M_u^{K-}} \right. \\ \left. - \frac{\partial F_{M_c^K}^2}{\partial (V^y)_{M_v^{K+}}}(\Delta V^y)_{M_v^{K+}} - \frac{\partial F_{M_c^K}^2}{\partial (V^y)_{M_v^{K-}}}(\Delta V^y)_{M_v^{K-}} \right. \\ \left. - \frac{\partial F_{M_c^K}^2}{\partial (V^z)_{M_w^{K+}}}(\Delta V^z)_{M_w^{K+}} - \frac{\partial F_{M_c^K}^2}{\partial (V^z)_{M_w^{K-}}}(\Delta V^z)_{M_w^{K-}} \right]. \end{aligned}$$

The same method applies for the concentration increments that can be computed using the third row of system (33):

$$\begin{aligned} (\Delta C)_{M_c^K} = \frac{1}{\frac{\partial F_{M_c^K}^3}{\partial C_{M_c^K}}} \left[S_{M_c^K}^3 - \frac{\partial F_{M_c^K}^3}{\partial P_{M_c^K}}(\Delta P)_{M_c^K} - \frac{\partial F_{M_c^K}^3}{\partial h_{M_c^K}}(\Delta h)_{M_c^K} - \frac{\partial F_{M_c^K}^3}{\partial (V^x)_{M_u^{K+}}}(\Delta V^x)_{M_u^{K+}} - \frac{\partial F_{M_c^K}^3}{\partial (V^x)_{M_u^{K-}}}(\Delta V^x)_{M_u^{K-}} \right. \\ \left. - \frac{\partial F_{M_c^K}^3}{\partial (V^y)_{M_v^{K+}}}(\Delta V^y)_{M_v^{K+}} - \frac{\partial F_{M_c^K}^3}{\partial (V^y)_{M_v^{K-}}}(\Delta V^y)_{M_v^{K-}} \right. \\ \left. - \frac{\partial F_{M_c^K}^3}{\partial (V^z)_{M_w^{K+}}}(\Delta V^z)_{M_w^{K+}} - \frac{\partial F_{M_c^K}^3}{\partial (V^z)_{M_w^{K-}}}(\Delta V^z)_{M_w^{K-}} \right]. \end{aligned} \quad (37)$$

4. NUMERICAL TESTS

4.1. Low Mach regime

In this section, we check the efficiency of the numerical method described in Sections 2 and 3 by carrying out various 1D tests. For all these tests, we used the stiffened gas law for the equation of state law [5].

4.1.1. Channel with varying porosity

Test description: Stationary liquid flow in a 1D channel with varying porosity. The channel is 4.2 m long. The porosity in the middle of the channel (1.4 m $\times$ 2.8 m) is set to 0.5 and to 1 elsewhere. The pressure at the outlet of the channel is fixed at 155 bar and the liquid velocity at the inlet of the channel is 1 m s⁻¹. The friction wall is set to zero. The gravity is neglected. Here, the objective is to test the ability of the spatial discretization to conserve momentum in case of a 1D varying porosity.

Results: Figure 4 presents the velocity and the pressure profiles along the z -axis.

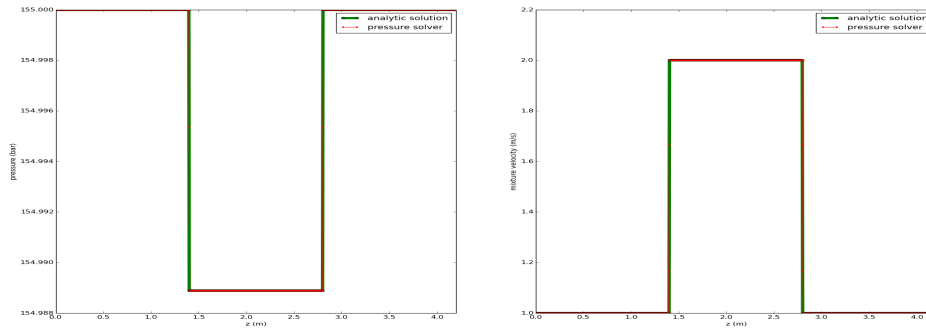


FIGURE 4. Channel with varying porosity: Pressure-based solver (red), analytic solution (green)

4.1.2. Channel with singular charge loss

Test description: Stationary liquid flow in a 1D channel with charge loss. The channel is 4.2 m long. The singular charge loss and models friction effects due to the presence of an element (like a mixing grid) at the middle of the core 2.1 m. The pressure at the outlet of the channel is fixed at 155 bar and the liquid velocity at the inlet of the channel is 1 m s⁻¹. The friction wall is set to zero. The gravity is neglected. We take $K = 100$ as the charge loss coefficient.

Results: Figure 5 shows that the pressure decreases after the flow passed through the mixing grid.

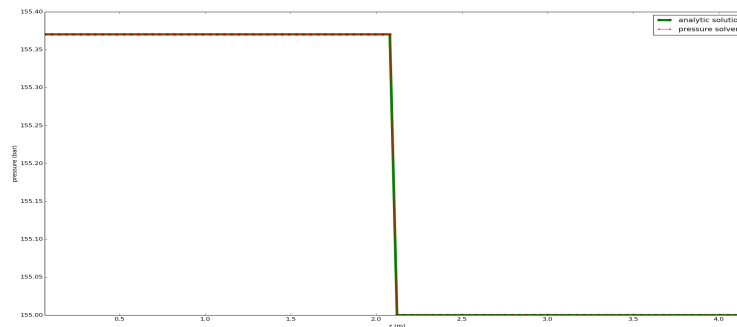


FIGURE 5. Channel with singular charge loss: Pressure-based solver (red), analytic solution (green)

4.1.3. Boiling channel

Test description: The physical quantities that we use in these tests match the functioning of the PWR (Pressurized Water Reactors). We consider a 4.2 m long channel heated by a uniform thermal flux $Q = 1. \text{E}8 \text{ W m}^{-3}$ on which we impose the following conditions: inlet concentration $C = 0$, inlet enthalpies $h_l = 1300 \text{ kJ kg}^{-1}$ and $h_v = 2600 \text{ kJ kg}^{-1}$, inlet velocities $u_l = u_v = 1 \text{ m s}^{-1}$ and outlet pressure $P_s = 155 \text{ bar}$. The friction wall is set to zero. The gravity is taken into account.

Results: In the figure 6, we compare the results of homogeneous ($\vec{V}_r = 0$) model (1) obtained with our pressure solver to an analytical solution obtained with the low Mach mixture model proposed in [5].

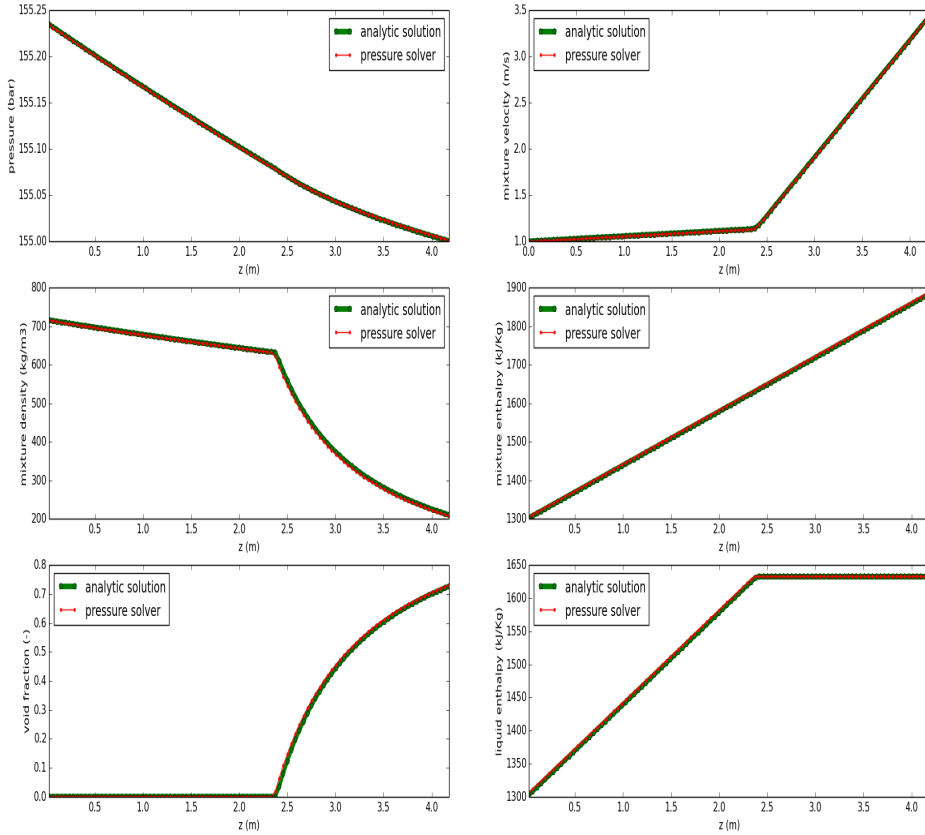


FIGURE 6. Boiling channel: Pressure-based solver (red), analytic solution (green)

4.2. Compressible regime

To test our Pressure-based Solver in the compressible regime, we study test cases described in [12] and presented in Table 1. All tests are performed with an ideal gas $\rho = \frac{\gamma}{\gamma-1} \frac{P}{h}$, with a constant $\gamma = 1.4$. All chosen data consist of two constant states separated by a discontinuity at $x = x_0$. The position of the discontinuity is stated in the legend. The spatial domain is $0 \leq x \leq 1$ and the numerical solution is computed with 100 and 5000 cells.

Test	ρ_L ($kg.m^{-3}$)	V_L ($m.s^{-1}$)	P_L (Pa)	ρ_R ($kg.m^{-3}$)	V_R ($m.s^{-1}$)	P_R (Pa)
Test 1	1	0.75	1	0.125	0	0.1
Test 2	1	-2	0.4	1	2	0.4
Test 3	1	0.	1000	1.	0	0.01

TABLE 1. Data for three Riemann problem tests for testing the Pressure-based Riemann solver.

For test 1, the Sod's Shock Tube problem [12] is modified slightly. The solution of the problem has a right shock wave, a right travelling contact wave and a left sonic rarefaction wave. The purpose of this test is to assess the entropy satisfaction property of the numerical methods. The results for this test are shown in Figure 7 against the exact results. We can see that the Pressure-based Solver struggles slightly with the internal energy, but otherwise performs very close to the exact Riemann solver with particularly accurate result around the sonic point unlike Roe scheme [12].

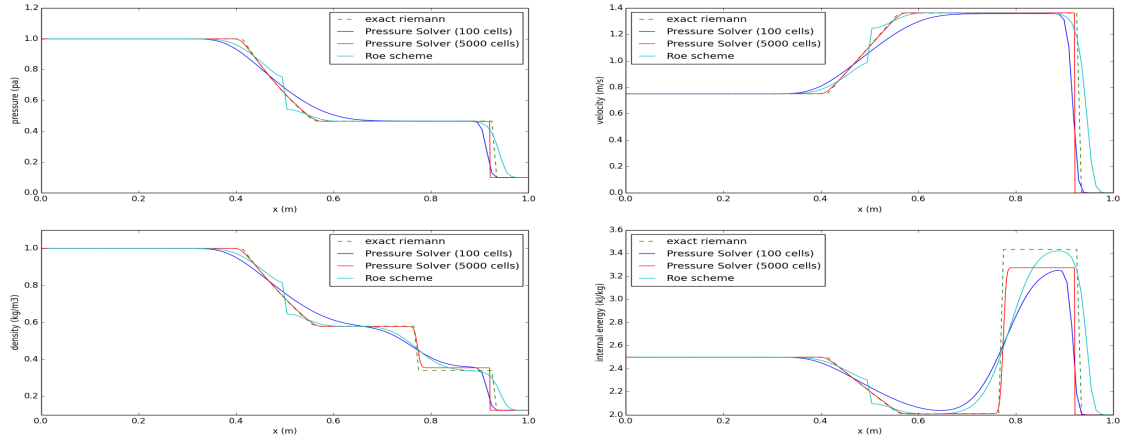


FIGURE 7. Pressure-based Riemann solver applied to test 1 of Table 1: Pressure-based solver (red and blue lines), Roe solver (sky blue line) and exact (dash) solutions compared at time 0.2

Test 2 consists of two symmetric rarefaction waves and a trivial contact wave, with the star region between the non-linear waves close to vacuum. This problem is a good assessment of the performance of numerical methods for low-density flows. The results for this test are shown in Figure 8 against the exact results and we can see that the accuracy of the numerical results is nearly from those of the exact Riemann solver unlike Roe scheme which fails near low-density flows [13].

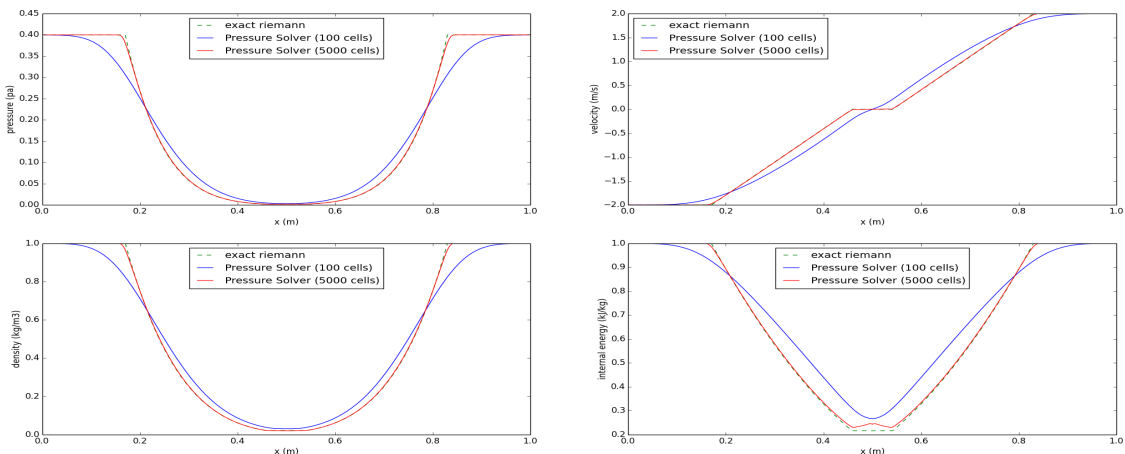


FIGURE 8. Pressure-based Riemann solver applied to test 2 of Table 1: Numerical (red and blue lines) and exact (dash) solutions compared at time 0.12

The robustness and accuracy of the Pressure-based solver is tested with Test 3. The solution of Test 3 consists of a strong shock wave, a contact surface and a left rarefaction wave. We can see from Figures 9 (100 cells) that the Pressure-based solver struggles slightly with the density, but otherwise performs very close to the exact solution. We can also see that the results obtained with the Pressure-based and Roe solvers are near. However, when the mesh is refined (1000 cells), we see that the Pressure-based solver do not converge to the exact solution.

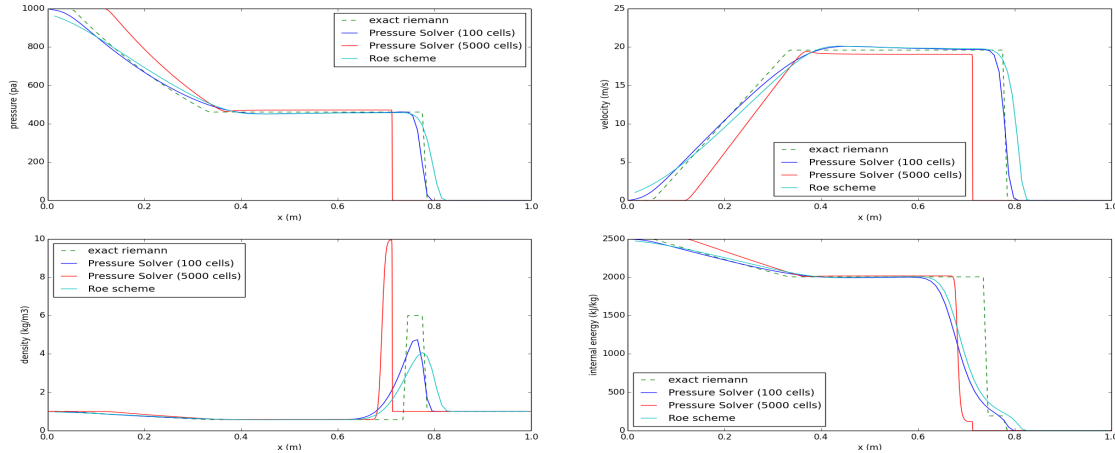


FIGURE 9. Pressure-based Riemann solver applied to test 3 of Table 1: Pressure-based solver (red and blue lines), Roe solver (sky blue line) and exact (dash) solutions compared at time 0.012

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