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Modelling of a Venturi using CATHARE-3 two-phase flow thermalhydraulic code for sodium flow cavitation studies

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Abstract. For reactor design and safety purposes, the French Alternative Energies and Atomic Energy Commission (CEA) is currently working on Sodium Fast Reactor (SFR) thermal-hydraulics. A SFR is a system composed of three circuits (primary and secondary: liquid sodium and tertiary: nitrogen gas or water) and designed to both produce electricity and optimize nuclear fuel cycle. In such SFR systems, primary pumps are associated as a parallel circuit. Then, throughout primary pump seizure transients, cavitation may occur in non-affected pumps because of the induced hydraulic resistance drop. Studying sodium flow cavitation occurring in simple geometries such as a Venturi (converging/diverging tube) is the first step to better understand the phenomenon and its sensitivities. The long term aim is to validate the flashing model used for sodium applications in the CATHARE-3 code in order to be confident when simulating more complex geometries. In this article, a Venturi test section experimented in the CANADER facility at CEA Cadarache in the 1980s and its modelling will be presented. Cavitation is obtained by flow rate variation at fixed tank pressure and circuit temperature conditions. Several computations are made in order to study the sensitivity of results to numerical and physical parameters. A set of parameters supposed to constitute the most representative case is defined and comparison of the predicted Thoma number against the experimental one is made. Detailed results of quantities of interest as profiles along the test section and evolutions during the transient are also presented.

1. Introduction

1.1. Context of sodium flow cavitation studies

The cavitation phenomenon happens in liquids when the local static pressure drops below the vapor pressure. Cavitation has been widely studied using water as working fluid. Liquid metal cavitation is less known because experiments are much more expensive and difficult to operate. First interest on sodium cavitation came out in the 1950s in the United States with the aircraft nuclear powerplant project [1]. In France, sodium cavitation started to be studied in the 1970s in the frame of Sodium-cooled Fast neutron breeder Reactors (SFR). At CEA Cadarache in particular, Courbiere et al [2] [3] [4] [5] [6] [7] [8] worked on the CANADER sodium cavitation tunnel. Various types of test section geometries were tested in this facility: diaphragm, Venturi, hydrofoil or cylinder types. More recently (2008-2011) but still linked to SFR thermal-hydraulic studies, Japan has made a research effort on sodium cavitation with the work of Ardiansyah et al

on a Venturi [9] [10] [11] [12] [13]. Today, France is still working on SFR thermal-hydraulics with the design of ASTRID 4th reactor generation demonstrator [14]. High flow rates involved in such reactors can lead to cavitation occurrence in pumps or orifices in incidental or accidental operating conditions. For this reason, several experimental tests on the Venturi test section geometry of CANADER were modelled with the two-phase flow thermal-hydraulic code CATHARE-3. It is the reference thermalhydraulic system code for french SFR safety studies. Comparison of computation results and experimental data of these cavitation inception tests is presented in this paper.

1.2. Objectives of the study and method

Objectives of this study are the following:

- learn on sodium flow cavitation phenomenon (identify main parameters affecting sodium cavitation)
- learn on sodium flow cavitation modelling
- extend CATHARE-3 flashing model validation for sodium applications

To reach these goals, the Venturi test section experimented in the CANADER loop will be modelled with CATHARE-3 and validation will be made on the Thoma number corresponding to cavitation inception obtained for several pressure and temperature conditions.

2. Description of the experimental setup

2.1. The CANADER facility

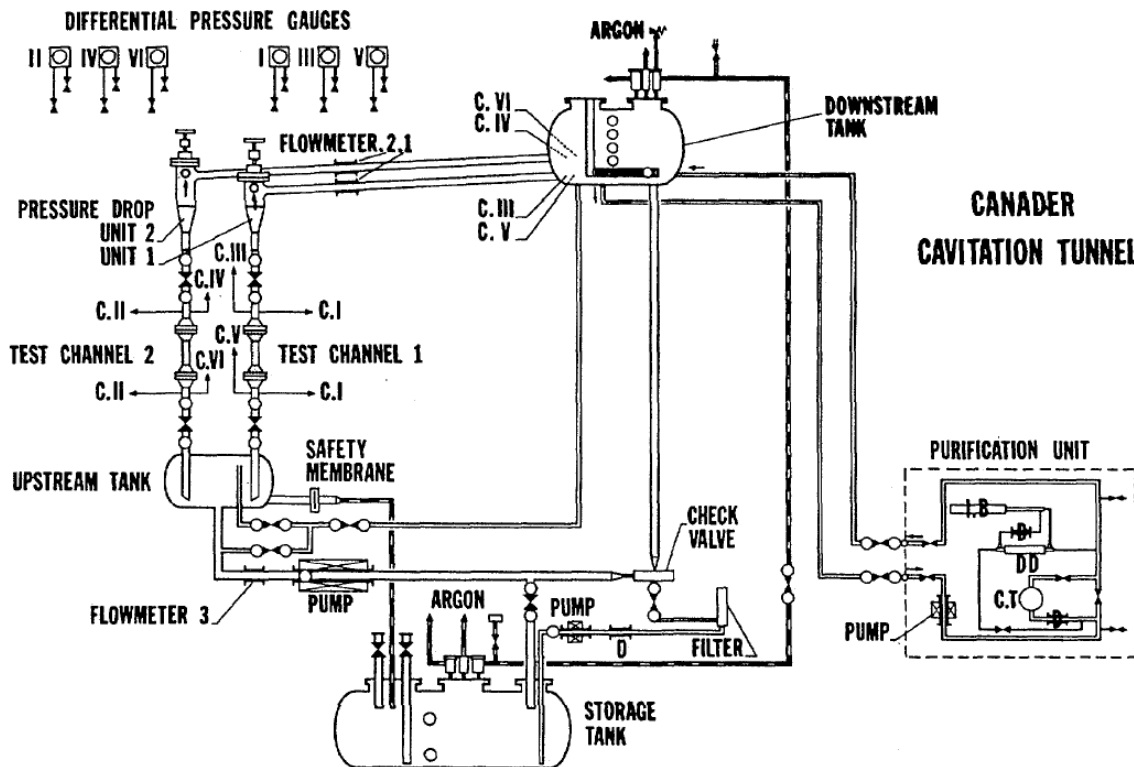


Figure 1. CANADER

CANADER is a sodium loop whose scheme is shown on figure 1. It has the following boundary operating conditions:

- Temperature: 200 °C to 600 °C
- Flow rate: 1 to 7 l/s
- Downstream vessel argon pressure: 1.15 to 5 absolute bars

Flow rate is controlled with an electromagnetic pump and the maximal pressure generated at pump outlet is 8 absolute bars. Minimum downstream vessel argon pressure is 1.15 absolute bars (a bit greater than atmospheric pressure) to limit oxygen entry in the circuit.

Temperature	Pressures
545 °C	1.15; 2; 3; 4; 5
450 °C	1.15; 2; 3; 4; 5
350 °C	1.15; 2; 3; 4; 5
250 °C	1.15; 2; 3; 4; 5

Table 1. Sodium test matrix

The experimental test matrix of temperature and pressure conditions tested on the Venturi geometry of CANADER is presented in table 1.

2.2. The Venturi test section geometry
The test section is composed of:

- a profiled converging tube with a ratio of 27 between inlet tube section and orifice section
- a cylindric orifice
- a conic diverging tube characterized by a half-angle of 7 °

2.3. Obtaining cavitation in both facilities

In CANADER facility, cavitation is obtained following this method:

- fluid temperature is stabilized in the whole circuit
- gas pressure in downstream vessel is kept constant
- cavitation phenomena is obtained only by acting on flow rate. Starting from a non-cavitating state, flow rate is gradually increased until the onset of cavitation.

The Thoma parameter is used to characterize the onset of cavitation:

$$\sigma = \frac{P_{us} - P_{sat}}{1/2\rho V^2} \quad (1)$$

P_{us} is the absolute static pressure measured upstream from the orifice

P_{sat} is the saturation pressure

ρ is the density of the liquid

V is the average velocity through the orifice

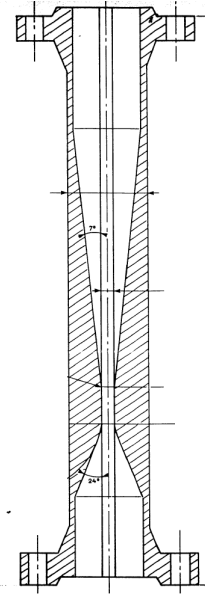


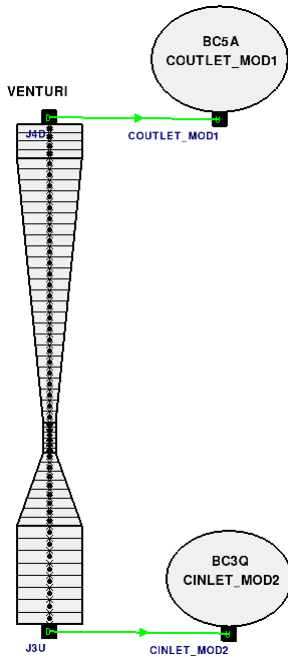
Figure 2. Venturi

3. Modelling

3.1. Description of the CATHARE-3 thermal-hydraulic code

CATHARE-3 is a french two-phase flow modular system code. It is owned and developed since 1979 by CEA and its partners EDF, Framatome and IRSN. See [15] for more details on the code development and validation strategy. One-dimensional (1D), three-dimensional (3D) or point (0D) hydraulic elements can be associated together to represent a whole facility. Thermal and hydraulic submodules (as warming walls, valves, pumps, turbines...etc) can be added to main hydraulic elements to respectively take into account thermal transfer, flow limitation, pressure

rise or pressure drop. Six local and instantaneous balance equations (mass, momentum and enthalpy for each phase) make possible liquid and gas representation for transient calculations. By this way, mechanical and thermal disequilibrium between phases can be represented [16]. Phase averages make necessary the use of physical closure laws in the balance equations system. One closure law concerns the flashing model, which is presented by Bestion in [17]. Cavitation and flashing correspond to the same phenomenon which is a phase change from liquid to vapor when pressure drops locally or in the whole system.



The flashing model contains two parts:

- a part existing with or without presence of non-condensable (NC) gas and depending on the liquid phase Reynolds and the difference between the liquid temperature T_l and the saturation temperature $T_{sat}(P)$.
- a part existing only in the presence of NC gas which tends to facilitate the vapor creation in this case.

3.2. Venturi modelled with CATHARE-3

The converging/diverging tube is modelled using a 1D hydraulic element. The choice of a 1D mesh implies one direction allowed for liquid and gas velocities but two possible ways (positive or negative). Several meshings have been tested in this study (see paragraph 4.3.1). The meshing presented on figure 3 is composed of 50 meshes.

Figure 3. Venturi modelled with CATHARE-3

Two boundary conditions (BC) are defined:

- an inlet BC (down) which imposes fluid velocity and temperature (for both liquid and gas even if gas phase is residual) and void fraction as functions of time.
- an outlet BC (up) which imposes static pressure as a function of time.

4. Validation against experimental data

4.1. Available experimental data: Thoma number as a function of Reynolds

Liquid sodium is an opaque fluid and as a result cavitation cannot be observed with the naked eye. Acoustic methods are used to detect cavitation inception either for small test sections or for a whole SFR. First cavitation detection acoustic method was used in 1957 by Robertson et al [18]. The sigma definition used below corresponds to cavitation inception and the first change of slope in acoustic characteristics [7]. The $\sigma-Re$ graph on figure 4 was obtained by Courbiere et al in the 1980s by experimenting the Venturi test section in the CANADER loop and in another loop called CALYPSO. Indeed, all test section geometries were also tested with water as working fluid in the CALYPSO loop [3]. In the present paper only sodium tests will be compared to computations. Sodium-water similarity will be studied in the next future.

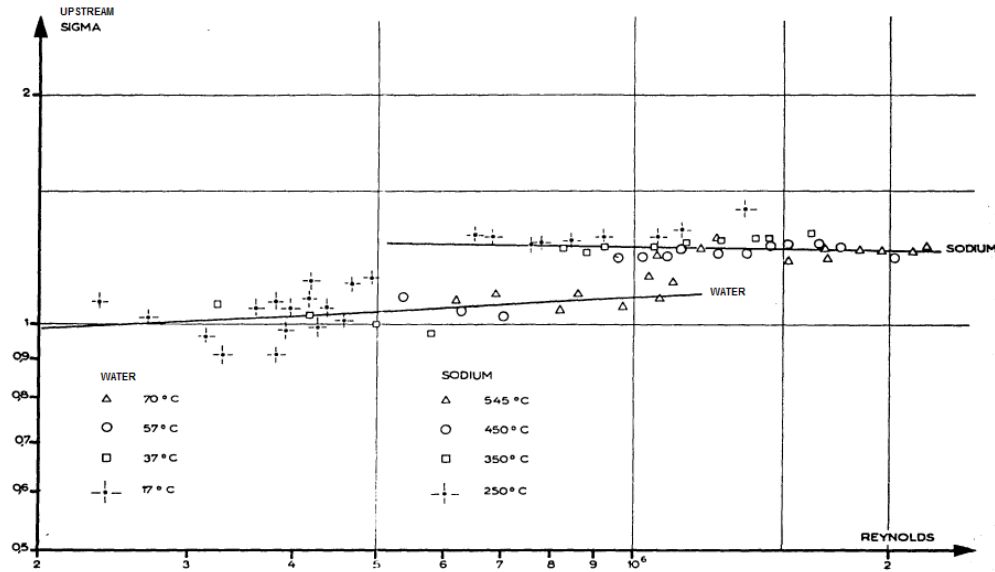


Figure 4. Thoma number as a function of Reynolds

The aim of the study is to obtain the $\sigma-Re$ graph presented above by CATHARE-3 calculations.

4.2. CATHARE-3 transient defined to obtain the $\sigma-Re$ graph

For each pressure-temperature (P-T) couple of conditions, a CATHARE-3 computation is run. As explained in the paragraph 3.2, temperature is imposed as an inlet BC and pressure is imposed as an outlet BC. Both are kept constant during the calculation. Fluid velocity (directly linked to flow rate) is imposed at the inlet BC and gradually increased to obtain cavitation.

The onset of cavitation is detected with a condition on the void fraction reaching a threshold noted α_{thr} at the end of the Venturi throat. When this condition is verified, fluid velocity is kept constant at its last value corresponding to cavitation inception.

Some physical parameters have to be defined to run calculations:

- α_{thr} is the void fraction threshold used to detect cavitation inception.
- **ALIQ** is the void fraction imposed at inlet BC.
- **XARGON** is the fraction of argon NC gas if defined in the computation.
- **model** is the flashing model type used in the computation.
- **rugosity** is the pipe rugosity used in the computation.

Numerical parameters also have to be defined:

- **Nmesh** is the number of meshes used to model the Venturi test section. All meshes along the Venturi have the same length noted dz .
- **DTMAX** is the maximal allowed duration of a time step during the calculation (in seconds).

In the following paragraph, sensitivity studies will be made by varying these parameters. First, numerical parameters will be tested and a reference set of numerical parameters will be chosen according to mesh and time convergences. Second, physical parameters will be tested and according to physical considerations, a case as representative of the real experiment as possible will be defined.

4.3. Numerical sensitivities

The order of magnitude of meshes used in CATHARE-3 calculations varies in general from 10cm to 1mm. Here, mesh lengths from 2.4cm (25 meshes) to 0.6mm (1000 meshes) will be tested in order to evaluate mesh convergence of calculations.

A standard value of **DTMAX** used in CATHARE-3 calculations is 1s. Two other values will be tested here: 0.1s and 0.01s in order to evaluate time convergence of calculations.

Finally, the effect of the definition of a NC gas even at a residual value will be studied to ensure that there is no influence on results in this case. Only NC gas rates greater than the residual value must have an effect.

The numerical sensitivity tests matrix is the following:

Case name	α_{thr}	ALIQ	XARGON	Nmesh	DTMAX	model	rugosity
m25dt1	10^{-2}	10^{-5}	0.	25	1.	rev1	standard
m50dt1	10^{-2}	10^{-5}	0.	50	1.	rev1	standard
m100dt1	10^{-2}	10^{-5}	0.	100	1.	rev1	standard
m150dt1	10^{-2}	10^{-5}	0.	150	1.	rev1	standard
m200dt1	10^{-2}	10^{-5}	0.	200	1.	rev1	standard
m250dt1	10^{-2}	10^{-5}	0.	250	1.	rev1	standard
m300dt1	10^{-2}	10^{-5}	0.	300	1.	rev1	standard
m500dt1	10^{-2}	10^{-5}	0.	500	1.	rev1	standard
m1000dt1	10^{-2}	10^{-5}	0.	1000	1.	rev1	standard
m200dt0.1	10^{-2}	10^{-5}	0.	200	0.1	rev1	standard
m200dt0.01	10^{-2}	10^{-5}	0.	200	0.01	rev1	standard

Table 2. Numerical sensitivities tests matrix

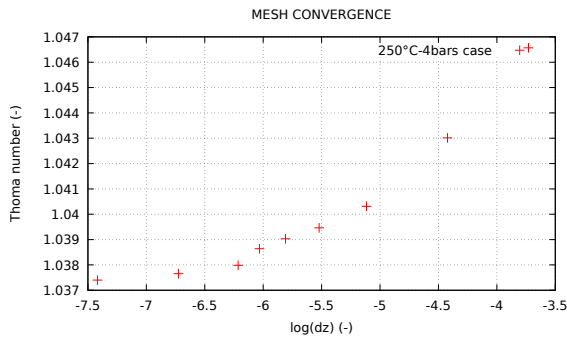


Figure 5. $\sigma-Re$ mesh convergence

4.3.1. Mesh convergence To test the mesh convergence, computations using 25, 50, 100, 150, 200, 250, 300, 500 and 1000 meshes are run with other parameters kept constant. Results are available on figure 5 representing the calculated Thoma number for one computation (250°-4bars case) as a function of the mesh length logarithm.

Results are slightly sensitive to the defined mesh. A convergence is obtained by refining the meshing what is satisfactory.

The case using 200 meshes seems to be the good compromise between convergence and CPU time. For this reason, it will be applied for all other following computations.

4.3.2. Time convergence To test the time convergence, computations using a DTMAX value of 1., 0.1 and 0.01 seconds are run for the 200-mesh case. Time convergence is satisfactory according to the results obtained on the global $\sigma-Re$ graph on figure 6.

A maximal time step duration of 1s seems to be sufficient but more accuracy can be obtained with 0.1s with still reasonable CPU time. For all the following computations, a DTMAX value of 0.1s will be imposed.

4.4. Physical sensitivities

The effect of varying physical parameters is analyzed here. Concerning the NC gas presence, from Courbiere [7] it can be considered that the minimal and maximal realistic NC rates respectively are $5 \cdot 10^{-6}$ and $3 \cdot 10^{-4} \text{ cm}^3 \text{ Ar/cm}^3 \text{ Na}$.

In this study, this volumetric concentration is assumed to correspond to the ALIQ void fraction defined as *gas volume/total volume*. Indeed, the argon volume is negligible compared to the sodium volume. The minimal value of NC gas presence that can be modelled is the residual one (10^{-5}) which has no effect by definition. Above this residual value, an effect of NC gas presence is expected.

Case name	α_{thr}	ALIQ	XARGON	Nmesh	DTMAX	model	rugosity
m200dt0.1	10^{-2}	10^{-5}	0.	200	0.1	rev1	standard
m200dt0.1mod	10^{-2}	10^{-5}	0.	200	0.1	rev3	standard
m200dt0.1rug45	10^{-2}	10^{-5}	0.	200	0.1	rev1	$45 \cdot 10^{-6}$
m200dt0.1rug152	10^{-2}	10^{-5}	0.	200	0.1	rev1	$152 \cdot 10^{-6}$
m200dt0.1thr	10^{-4}	10^{-5}	0.	200	0.1	rev1	standard
m200dt0.1aliq	10^{-2}	$3 \cdot 10^{-4}$	0.	200	0.1	rev1	standard
m200dt0.1aliqNC	10^{-2}	$3 \cdot 10^{-4}$	0.999999	200	0.1	rev1	standard
m200dt0.1aliqNCval	10^{-2}	$3 \cdot 10^{-4}$	0.99999	200	0.1	rev1	standard

Table 3. Physical sensitivities tests matrix

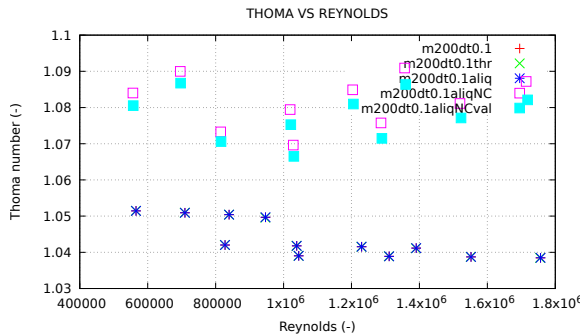


Figure 7. σ - Re physical sensitivities

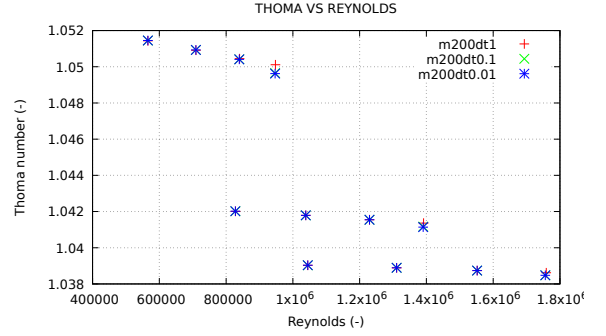


Figure 6. σ - Re time convergence

4.4.1. Sensitivity to the threshold value A sensitivity to the threshold value ($\alpha_{thr} = 10^{-2}$ or 10^{-4}) has been conducted. Results are not sensitive as shown on figure 7, then, the value of $\alpha_{thr} = 10^{-2}$ is kept in the following.

4.4.2. Sensitivity to the void fraction without NC gas A sensitivity to the void fraction value imposed at inlet BC without presence of NC gas (ALIQ = 10^{-5} or $3 \cdot 10^{-4}$ with XARGON=0. in both cases) has been conducted. Results are not sensitive to this parameter without NC gas presence as shown on 7.

4.4.3. *Sensitivity to the presence of NC gas* A sensitivity to the presence of NC gas imposed at inlet BC (XARGON=0. or XARGON=0.999999 with ALIQ = 3.10^{-4} in both cases) has been conducted. Results are really sensitive to the NC gas presence as shown on figure 7. NC gas presence is a important parameter to take into account in sodium cavitation studies, what was also identified by Courbiere [7].

4.4.4. *Sensitivity to the argon rate value* The argon rate value XARGON cannot be set exactly to 1. (100% of gas phase) because residual water vapor phase always exists in CATHARE-3 two-phase computations for numerical reasons. The effect of defining a XARGON value to 0.999999 or 0.99999 is investigated here. Results presented on figure 7 show a little dependence on the value of XARGON. In the following, the value of 0.999999 will be kept.

4.4.5. *Sensitivity to the flashing model* The default flashing model used in all calculations of this study is the one developed for water applications [17]. But, in the frame of SFR thermalhydraulics studies, the CATHARE development team at CEA proposed to modify two constants of the initial flashing model in order to better represent sodium flow conditions. In this paragraph, results on the prediction of the Thoma number using the modified sodium flashing model will be compared to those using the initial flashing model.

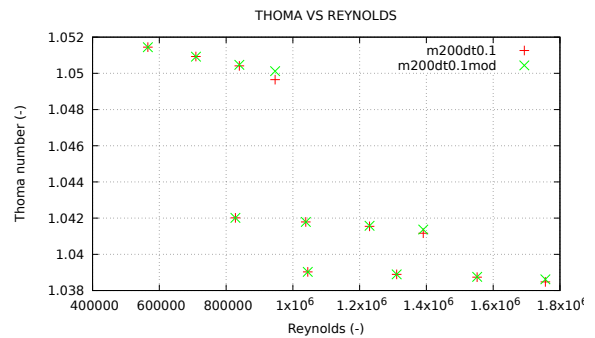


Figure 8. $\sigma-Re$ model sensitivity

In this cavitation inception study, the modification of the two constants in the flashing model seems not to have a significant influence on results. Currently, there is a lack of data allowing to validate correctly flashing models for sodium applications. Depressurization validation cases need to be experimented and modelled.

4.4.6. *Sensitivity to the rugosity* Pipe rugosity impacts the pressure drop along the test channel. For this reason, a sensitivity to the rugosity is conducted here. Results using the CATHARE-3 'RUGO' option with two absolute rugosities of $45.10^{-6}m$ (stainless steel) and $152.10^{-6}m$ (galvanized steel) [19] are compared to results using the classical CATHARE-3 model that corresponds approximately to an absolute rugosity of $1.5.10^{-6}m$ in this range of Reynolds number.

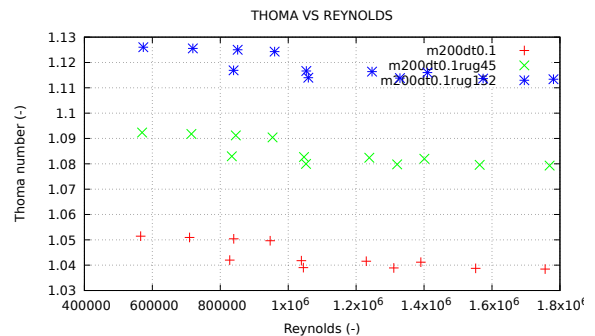


Figure 9. $\sigma-Re$ rugosity sensitivity

RUGO is an option of CATHARE-3 developed mainly for high Reynolds applications in the frame of ASTRID gas power conversion system studies [20]. Results presented on figure 9 show a great sensitivity to the pipe rugosity. In the following, the value of $45.10^{-6}m$ will be kept as it is the most plausible rugosity of the test channel.

4.5. Detailed results of the most representative case

Considering the sensitivity studies conducted and physical considerations mentioned previously, the following representative case is defined:

Case name	α_{thr}	ALIQ	XARGON	Nmesh	DTMAX	model	rugosity
representative	10^{-2}	3.10^{-4}	0.999999	200	0.1	rev1	45.10^{-6}

Table 4. The most representative case defined

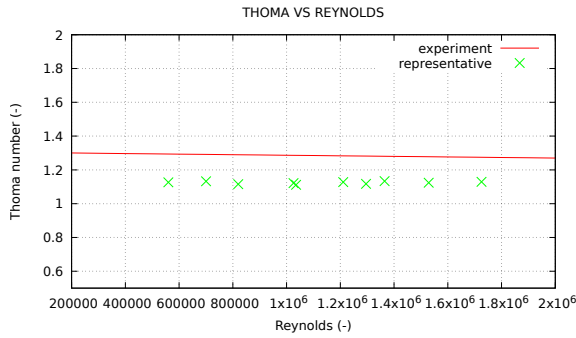


Figure 10. $\sigma-Re$ validation

Comparison of computation results of the most representative case to experimental data is made here. Scale boundaries of initial experimental graph are defined but scaling is linear instead of 2-logarithmic. Difference between the two scalings is small in this case. The experimental line represented in the experimental graph has been reproduced on figure 10. Globally, results are underestimated of approximately 13% compared to experimental data. However, the qualitative trend of the $\sigma-Re$ curve is respected.

Additionally to the global $\sigma-Re$ curve, detailed profiles and evolutions of main physical quantities are presented in the following. Evolutions of the inlet BC velocity and the void fraction at the end of the Venturi throat are available on figure 11 and 12 for each P-T couple of conditions. Pressure and void fraction profiles obtained at the end of the transient are presented on figure 13 and 14.

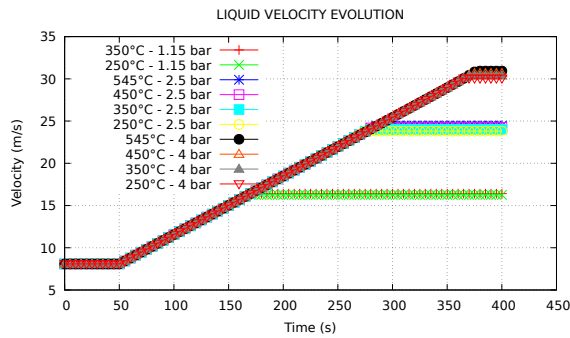


Figure 11. Velocity evolutions

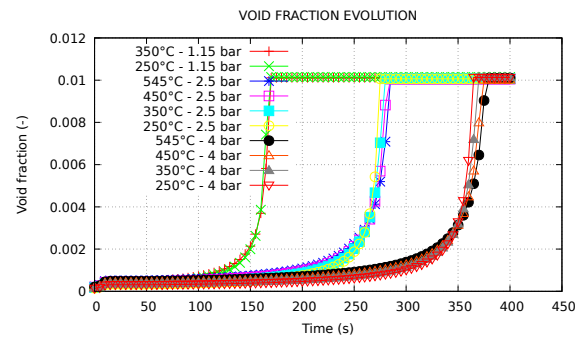


Figure 12. Void fraction evolutions

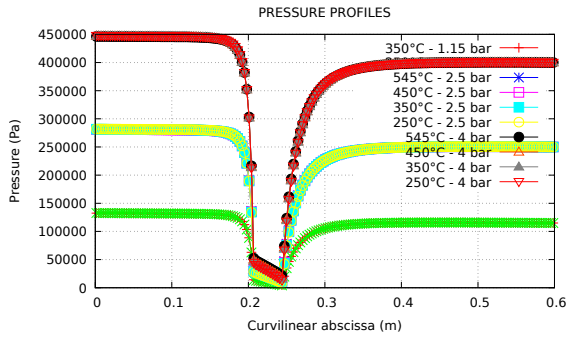


Figure 13. Pressure profiles

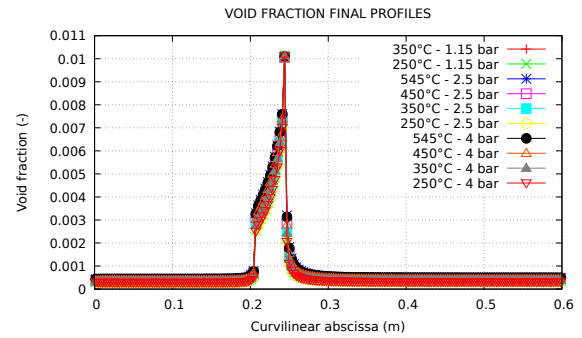


Figure 14. Void fraction profiles

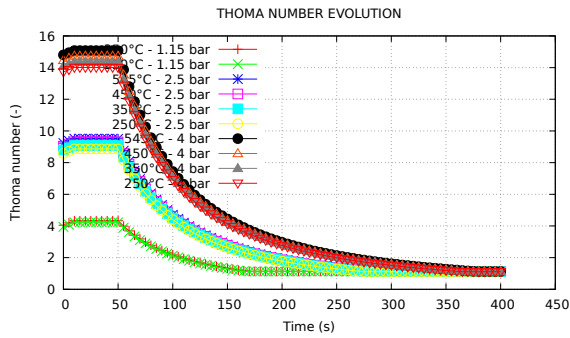


Figure 15. Thoma number evolutions

Finally, evolutions of the Thoma number for each P-T couple of conditions as a function of time are presented on figure 15. What can be concluded from all these detailed results is that temperature seems to have a small effect on cavitation inception flow rate instead of pressure that have an important effect.

Conclusions and perspectives

The objective of the present study is to learn about sodium cavitation phenomenon. Indeed, water cavitation occurring in Venturis has been well studied but experiment sodium loops is much more difficult and expensive what explains the lack of available experimental data on the subject.

The CANADER facility operated in the 1980s at CEA Cadarache has been presented in this paper and the tests experimented on the Venturi geometry have been modelled using the CATHARE-3 two-phase flow thermalhydraulic code.

Numerical and physical sensitivity tests have been respectively conducted to better control the obtained results and evaluate the effect of parameters on the predicted Thoma number. The Thoma number corresponding to cavitation inception and its dependence on the Reynolds number has ben studied. Profiles along the test section and evolutions during the transient of quantities of interest have been presented.

The perspective of this work is mainly the study of water-sodium similarity by simulating the CALYPSO tests on the same Venturi test section geometry. That will be done in the next future.

Nomenclature

Acronyms

Symbol	Description
<i>ASTRID</i>	Advanced Sodium Technological Reactor for Industrial Demonstration
<i>BC</i>	Boundary Condition
<i>CATHARE</i>	Code for Analysis of THERmalhydraulics during an Accident of Reactor and safety Evaluation
<i>CEA</i>	French Alternative Energies and Atomic Energy Commission
<i>CPU</i>	Central Processing Unit
<i>EDF</i>	Electricité De France
<i>IRSN</i>	Institut de Radioprotection et de Sûreté Nucléaire
<i>NC</i>	Non-Condensable
<i>SFR</i>	Sodium Fast Reactor
<i>xD</i>	x-dimensional

Subscripts

<i>l</i>	liquid
<i>sat</i>	saturation
<i>thr</i>	threshold
<i>us</i>	upstream

Latin letters

<i>dz</i>	Mesh length
<i>P</i>	Pressure
<i>Re</i>	Reynolds number
<i>T</i>	Temperature
<i>V</i>	Fluid velocity

Greek letters

α	void fraction
ρ	density
σ	Thoma number

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